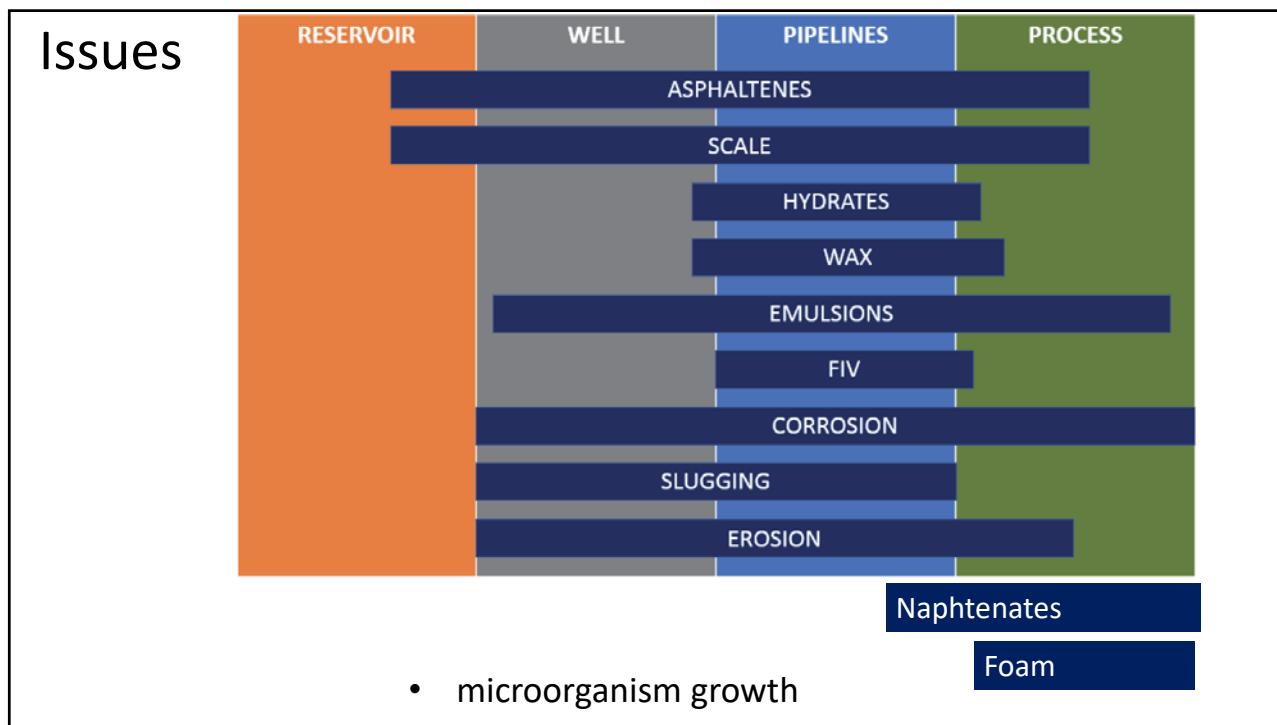


Notes for Youtube video nr. 18

# Flow assurance considerations in hydrocarbon field development and planning

Prof. Milan Stanko (NTNU)

1

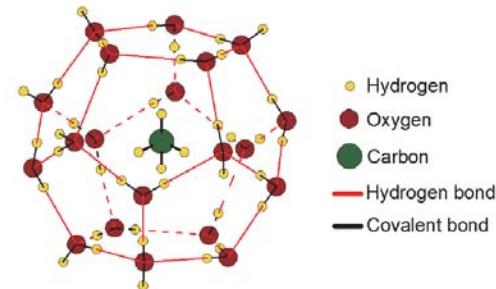


2

# Hydrates



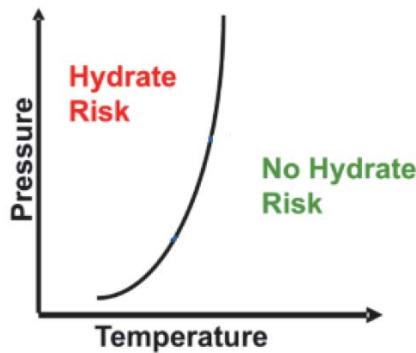
<https://www.youtube.com/watch?v=Oz4NLXfdqpA>



3

## Hydrates - conditions

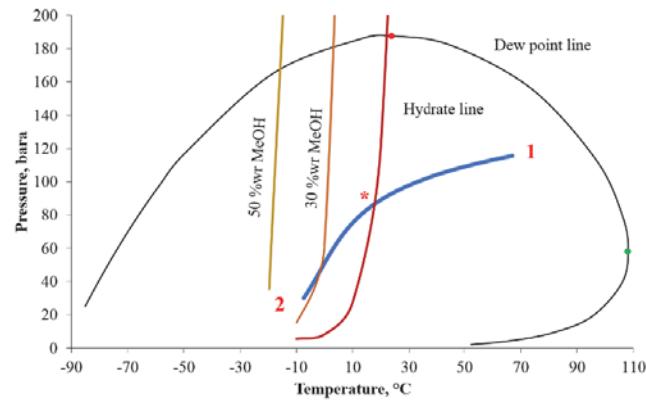
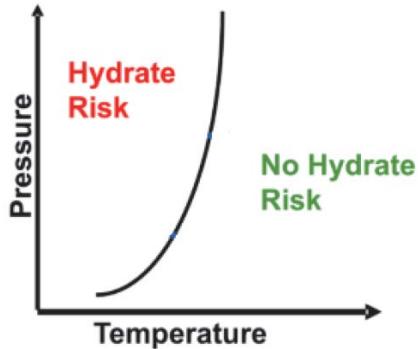
- Free water (in liquid phase)
- Small hydrocarbon molecules
- Particular range of pressure and temperature.



4

## Hydrates - conditions

- Free water (in liquid phase)
- Small hydrocarbon molecules
- Particular range of pressure and temperature.

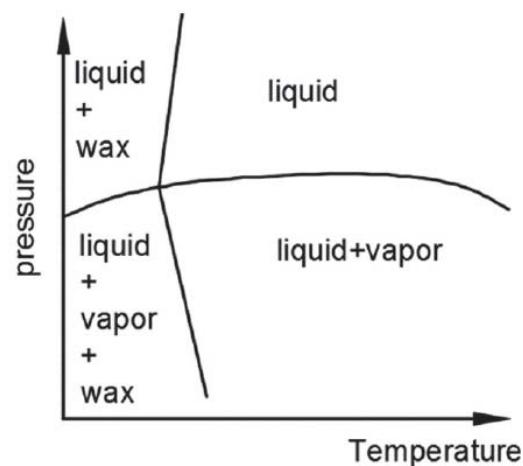


5

## Wax



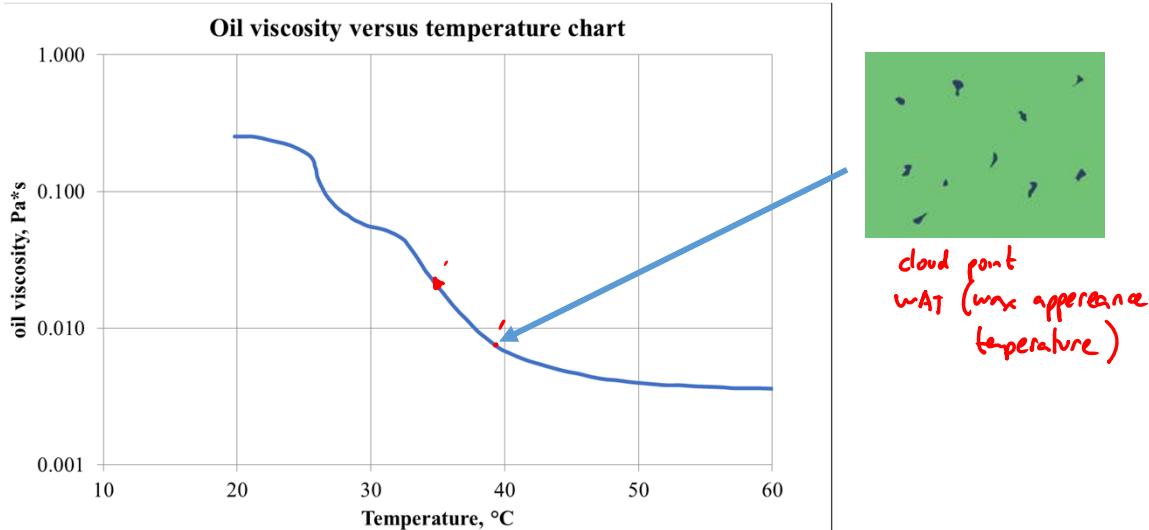
TAKEN FROM EQUINOR



Paraffins (C18 - C36)

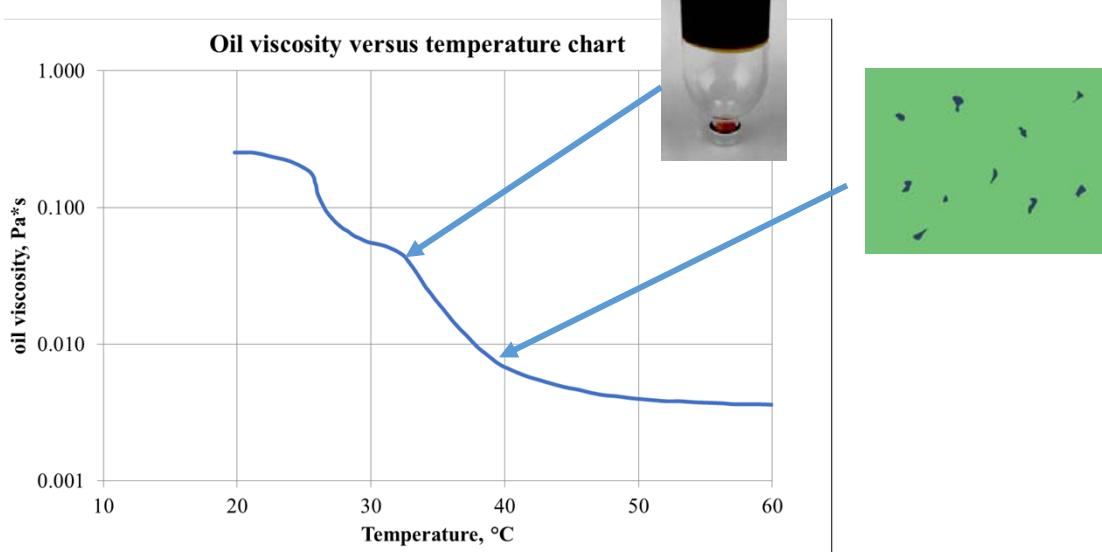
6

# Wax



7

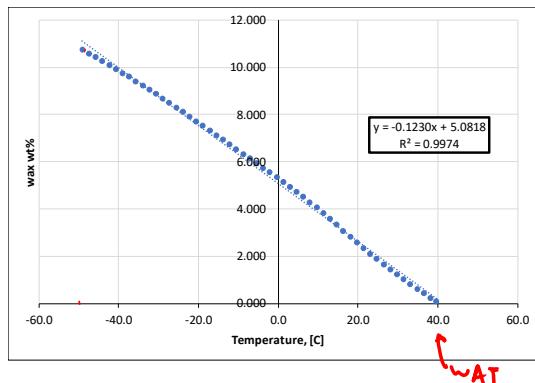
# Wax



8

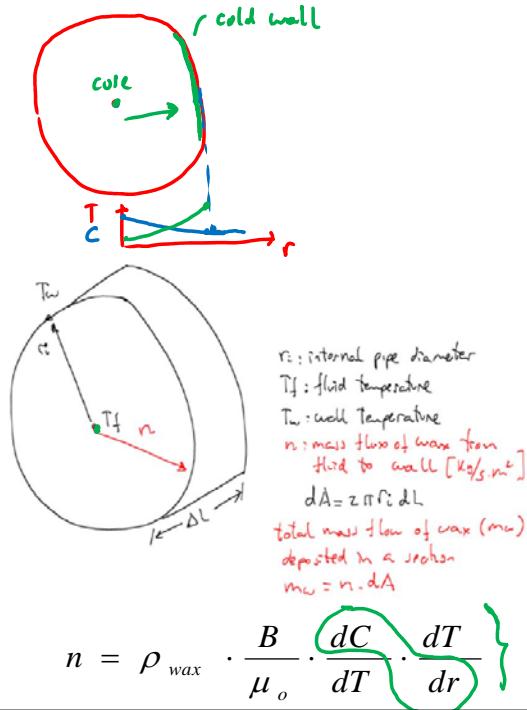
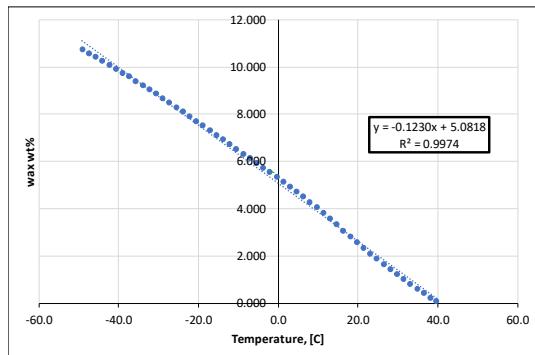
## Wax

weight of wax particles, 100  
total weight



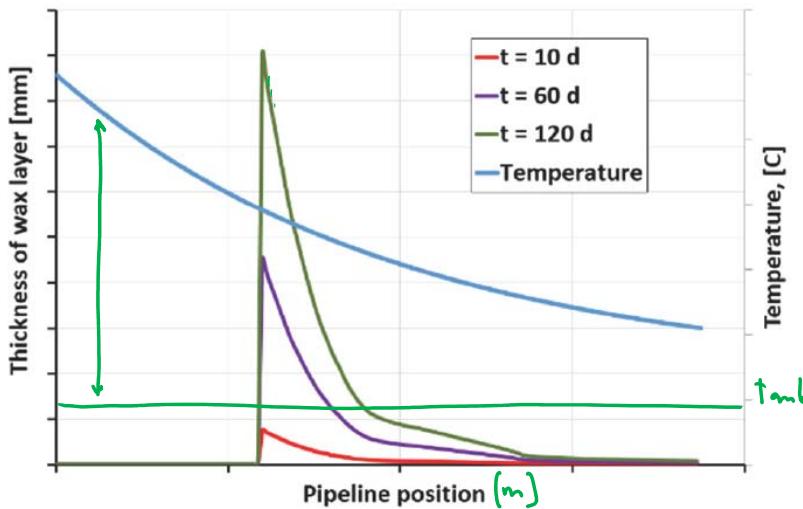
9

## Wax



10

## Wax

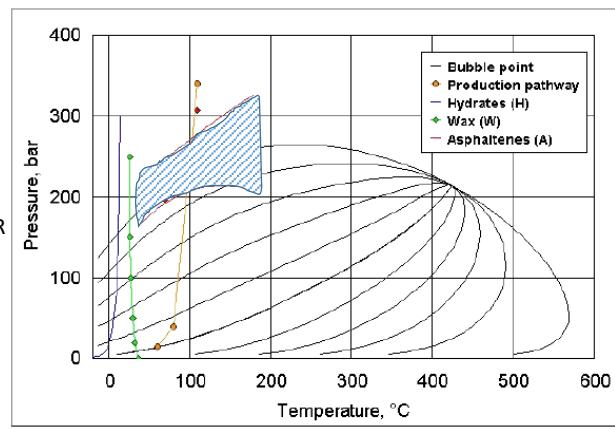
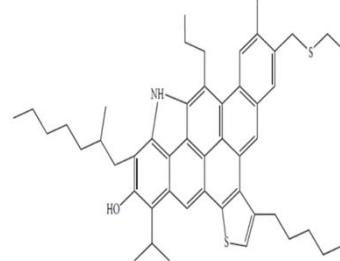


11

## Asphaltenes



TAKEN FROM EQUINOR  
(KALLEVIK)



12

## Scale



Choke on FCM 1000 18142 S/N 101

Ion	Formasjonsvann [mg/l]	Seawater [mg/l]
Na	14 800	10 680
K	520	396
Mg	13	1 279
Ca	378	409
Ba	410	8
Sr	228	0
Fe	58	0
Cl	23 600	19 220
SO <sub>4</sub>	0	2 689

+

$$Ba^{2+} + SO_4^{2-} = BaSO_4(s)$$

$$Ca^{2+} + CO_3^{2-} = CaCO_3(s)$$

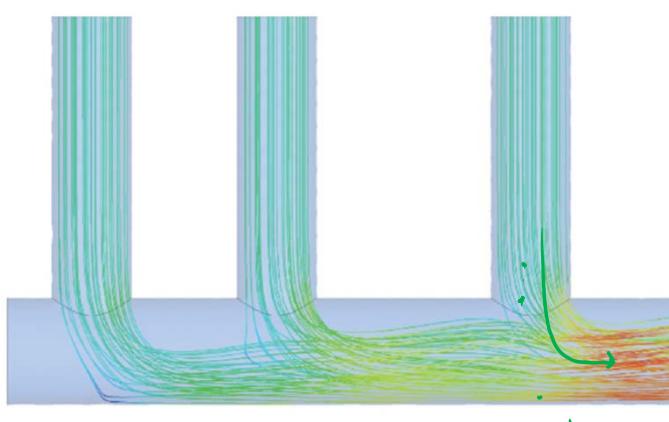
$p \downarrow$   $\rightarrow$   $T \uparrow$

**BaSO<sub>4</sub>    CaCO<sub>3</sub>    NaCl**

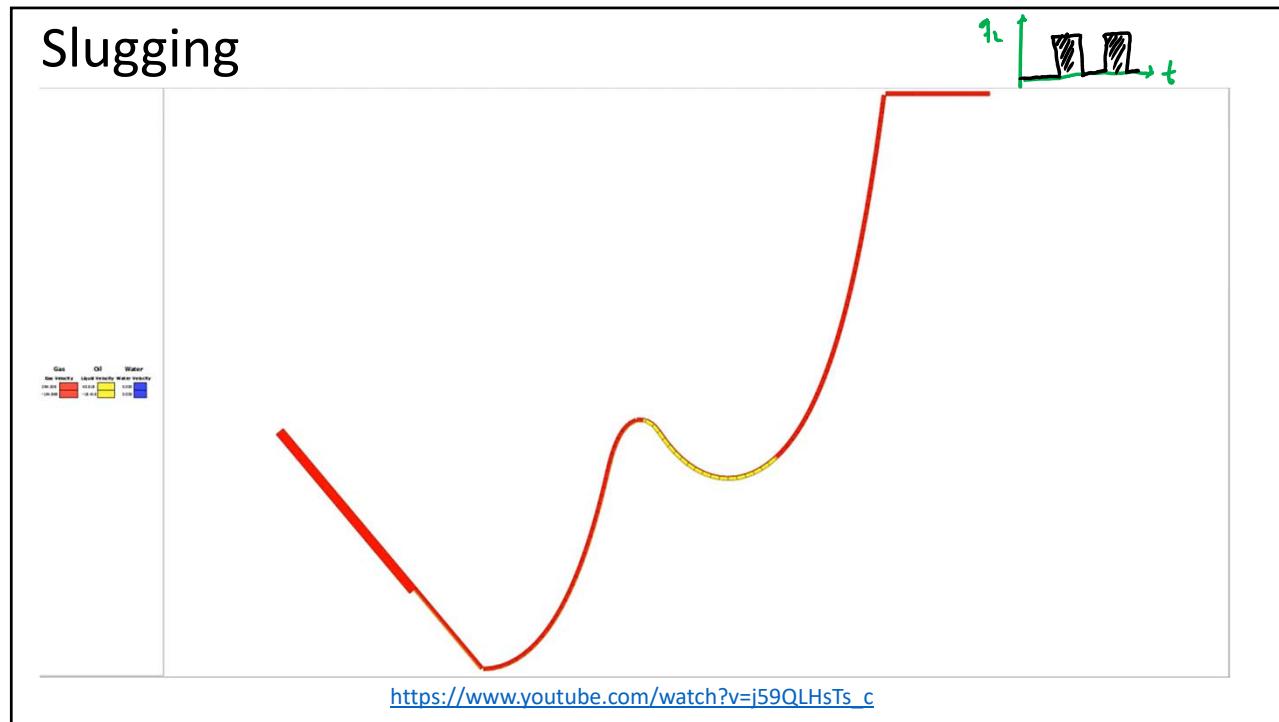
TAKEN FROM EQUINOR (SANDENGEN)

13

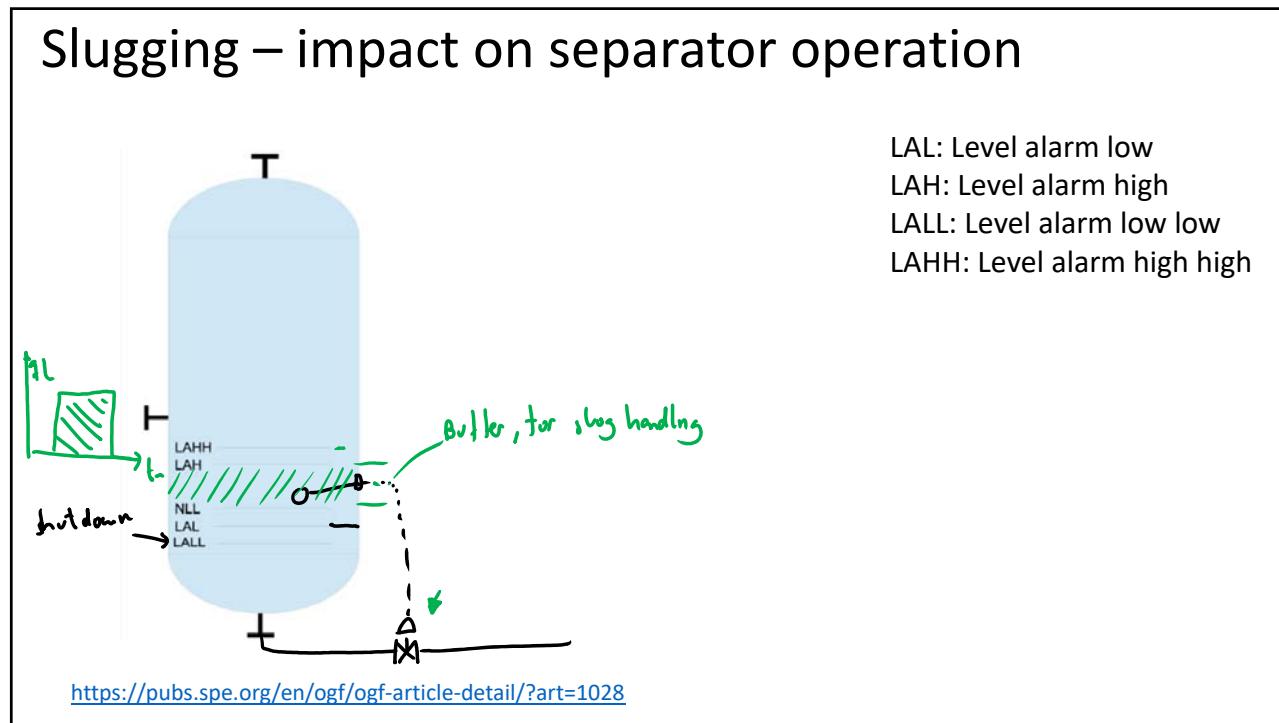
## Erosion

14

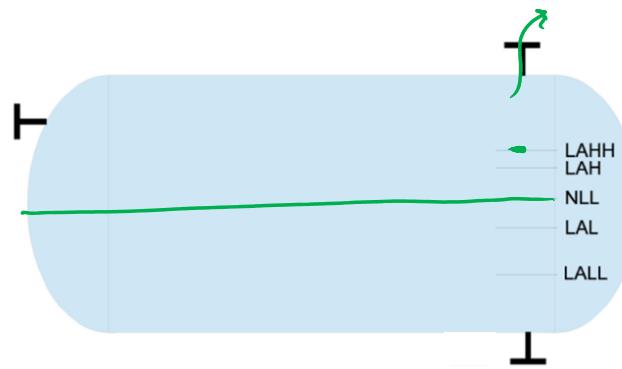


15



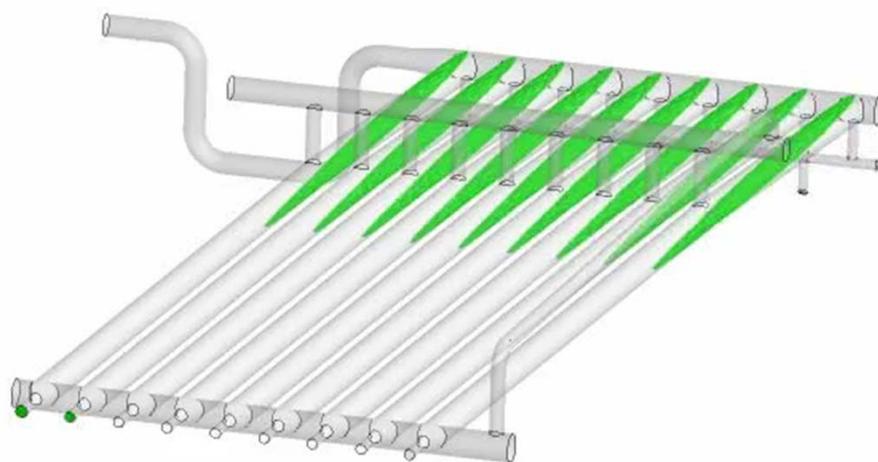
16

## Slugging – impact on separator operation



17

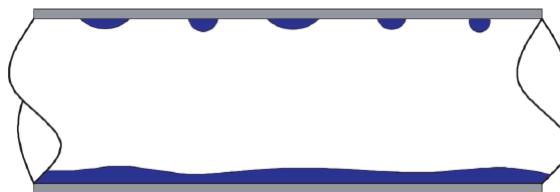
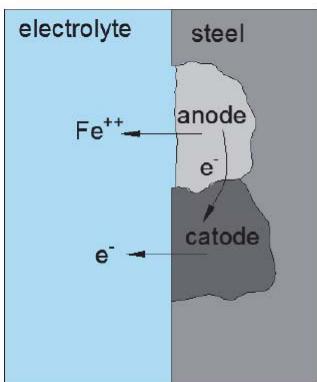
## Slugging – slugcatcher handling slugs



<https://www.youtube.com/watch?v=LKLW5284adI>

18

## Corrosion



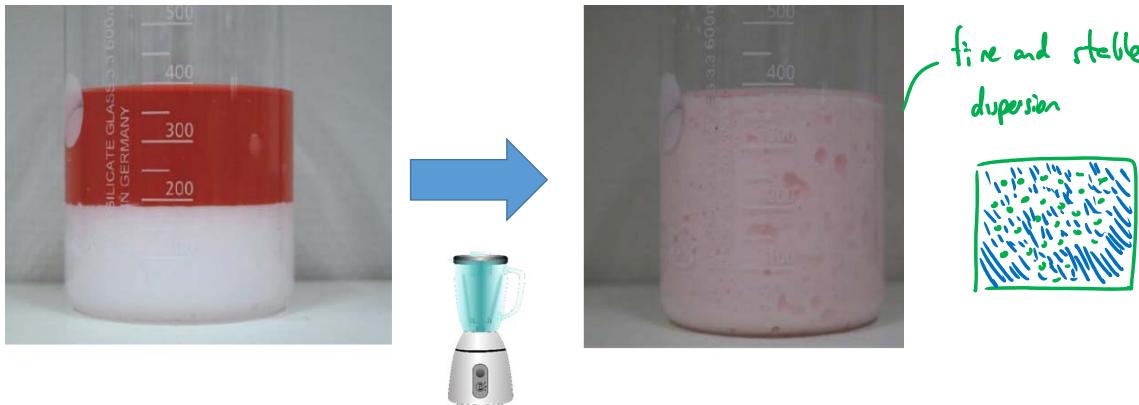
19

## Oil-water emulsions



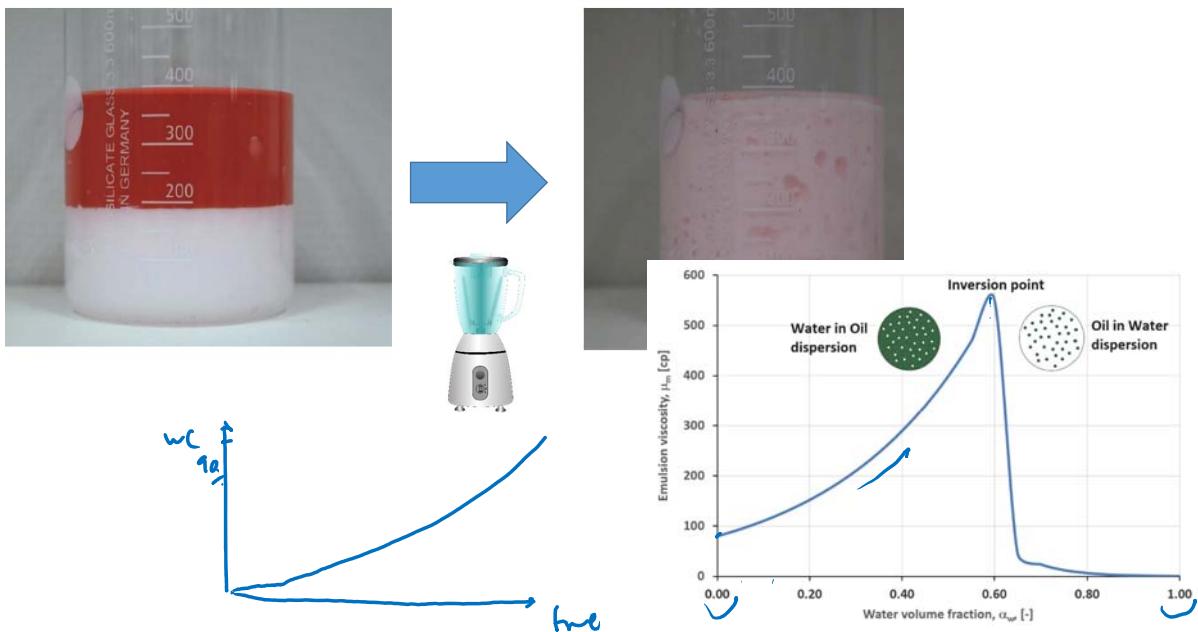
20

## Oil-water emulsions



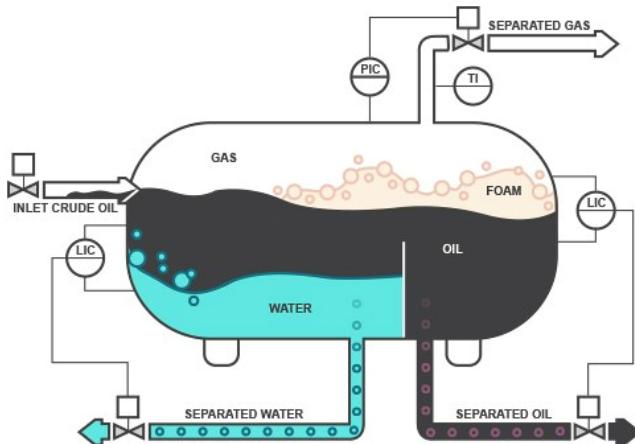
21

## Oil-water emulsions

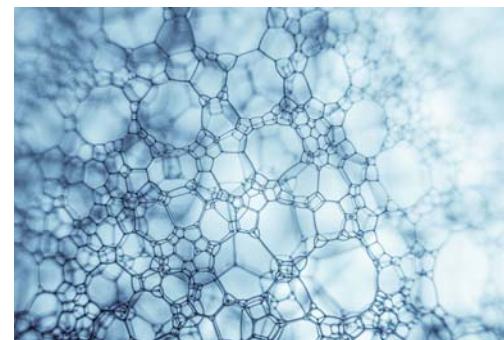


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# Foam



<https://www.arab-oil-naturalgas.com/foam-in-oil-gas-separators/>



<https://www.crodaoilandgas.com/en-gb/discovery-zone/functions/foamers>

23

Flow assurance issue	Causes	Potential Consequences	Prevention/solution	Tools available for analysis
<b>Hydrates</b>	<ul style="list-style-type: none"> <li>Small gas HC molecules</li> <li>Free water</li> <li>Begin to form at a given p and T (low T, high P) given by thermodynamic equilibrium of the hydrate phase.</li> </ul>	<ul style="list-style-type: none"> <li>Blockage of flowlines and pipelines</li> </ul>	<ul style="list-style-type: none"> <li>Reduce the hydrate formation region:           <ul style="list-style-type: none"> <li>Continuous or on-demand injection of chemical inhibitor (MEG or MEOH)</li> <li>Stay out of hydrate formation region:               <ul style="list-style-type: none"> <li>Improve thermal insulation</li> <li>Electric heating</li> <li>Others:                   <ul style="list-style-type: none"> <li><b>Cold flow*</b></li> <li><b>Water removal and gas dehydration*</b></li> </ul> </li> </ul> </li> </ul> </li> </ul>	<ul style="list-style-type: none"> <li>To determine Hydrate formation conditions:           <ul style="list-style-type: none"> <li>Laboratory tests</li> <li>Empirical correlations</li> <li>Thermodynamic simulators (e.g. Hysys, PVTsim, Unisim)</li> </ul> </li> <li>To determine p and T along the pipe:           <ul style="list-style-type: none"> <li>Multiphase simulator (Olga, LedaFlow).</li> <li>Computational fluid dynamics (CFD)</li> </ul> </li> </ul>
<b>Wax</b>	<ul style="list-style-type: none"> <li>Composition of the crude oil</li> <li>Begins to form at given p and T due to changes in solubility</li> <li>Cold wall</li> </ul>	<ul style="list-style-type: none"> <li>In wells, flowlines and pipelines:           <ul style="list-style-type: none"> <li>Increase pressure drop (pipe roughness)</li> <li>Reduction of cross section area</li> <li>Pipe blockage</li> <li>Changes fluid rheology</li> <li>Gelling (problem for startup)</li> </ul> </li> </ul>	<ul style="list-style-type: none"> <li>Pigging</li> <li>Thermal insulation</li> <li>Electric heating</li> <li>Chemical inhibitors</li> <li>Chemical dissolvers</li> <li>Pipe coating</li> <li><b>Cold flow*</b></li> </ul>	<ul style="list-style-type: none"> <li>Laboratory tests</li> <li>Transient multiphase simulators (e.g. Olga, LedaFlow)</li> <li>Computational fluid dynamics (CFD)</li> </ul>
<b>Slugging</b>	<ul style="list-style-type: none"> <li>Dynamics of multiphase flow of liquid and gas</li> <li>Reduction of rate</li> <li>Liquid accumulation on low points</li> </ul>	<ul style="list-style-type: none"> <li>Fluctuating liquid and gas input to processing facilities</li> <li>In flowlines and pipelines:           <ul style="list-style-type: none"> <li>Vibration</li> <li>Added pressure drop</li> <li>Fatigue</li> </ul> </li> </ul>	<ul style="list-style-type: none"> <li>Change separator size</li> <li>Pipeline dimensioning</li> <li>Maintain flow above minimum flow rate</li> <li>Gas lift in riser base</li> <li>Choking topside</li> <li>Pipeline re-routing</li> <li><b>Subsea separation*</b></li> </ul>	<ul style="list-style-type: none"> <li>Transient multiphase simulator (OLGA, LEDA)</li> <li>Structural analysis (usually with FEA, e.g. Ansys)</li> <li>Laboratory experiments</li> </ul>
<b>Scaling</b>	<ul style="list-style-type: none"> <li>Changes in solubility (e.g. changes in P and T conditions, changes in pH, mixture of incompatible water, CO<sub>2</sub> injection)..</li> <li>Irregularities on surface</li> </ul>	<ul style="list-style-type: none"> <li>In wells, pipelines and flowlines:           <ul style="list-style-type: none"> <li>Reduction of cross section area</li> <li>Pipe blockage</li> <li>Malfunctioning of valves and equipment</li> </ul> </li> </ul>	<ul style="list-style-type: none"> <li>Continuous injection of chemical inhibitors</li> <li>Dilution by adding more water</li> <li>Chemical dissolvers</li> <li>Mechanical removal</li> <li>Coating</li> </ul>	<ul style="list-style-type: none"> <li>Laboratory tests</li> <li>Simulation tools</li> </ul>

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Flow assurance issue	Causes	Potential Consequences	Prevention/solution	Tools available for analysis
Erosion	<ul style="list-style-type: none"> <li>• Sand production</li> <li>• High flow velocities</li> <li>• Liquid droplets in the gas</li> <li>• Gas droplets in the liquid</li> </ul>	In wells, pipelines and flowlines: <ul style="list-style-type: none"> <li>• Structural damage</li> <li>• Vibration</li> <li>• Leaks</li> <li>• Corrosion</li> </ul>	<ul style="list-style-type: none"> <li>• Change geometry</li> <li>• Replacement and maintenance of components</li> <li>• Reduce flow rate (reduce formation drawdown)</li> <li>• Sand separation*</li> <li>• Coatings</li> </ul>	<ul style="list-style-type: none"> <li>• Standards (DNV-RP-0501)</li> <li>• Computational fluid dynamics</li> <li>• Laboratory testing</li> </ul>
Corrosion	<ul style="list-style-type: none"> <li>• Water</li> <li>• O<sub>2</sub></li> <li>• CO<sub>2</sub></li> <li>• H<sub>2</sub>S</li> </ul>	<ul style="list-style-type: none"> <li>• Leaks</li> <li>• Integrity</li> </ul>	<ul style="list-style-type: none"> <li>• Coatings</li> <li>• Material selection</li> <li>• Surface passivation</li> </ul>	<ul style="list-style-type: none"> <li>• Laboratory testing</li> </ul>
Emulsions	<ul style="list-style-type: none"> <li>• Emulsification agents in the crude</li> <li>• Mixing, shear when flowing through valves, chokes, etc</li> </ul>	<ul style="list-style-type: none"> <li>• Added pressure drop</li> <li>• Increased separation time</li> </ul>	<ul style="list-style-type: none"> <li>• Injection of demulsifiers</li> <li>• Heating</li> </ul>	<ul style="list-style-type: none"> <li>• Laboratory tests</li> <li>• Multiphase models</li> </ul>
Asphaltenes	<ul style="list-style-type: none"> <li>• Crude with asphaltenes</li> <li>• Pressure reduction</li> <li>• Addup of light hydrocarbon components</li> </ul>	<ul style="list-style-type: none"> <li>• Blockage of formation, well, flowline and pipeline</li> <li>• Loss of equipment functionality</li> <li>• Emulsification and foamification</li> </ul>	<ul style="list-style-type: none"> <li>• Mechanical removal</li> <li>• Chemical injection</li> </ul>	<ul style="list-style-type: none"> <li>• Laboratory tests</li> <li>• Some simulation tools</li> </ul>

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## Measures and consequences

- **Chemical injection**
- System design, e.g.
  - pipe and component insulation
  - heat tracing
  - dead legs
  - pipeline routing
- Well intervention needs
- Water injection strategy
- Define procedures when shutting down and starting up
- Ensure proper distribution of chemicals



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## Example of chemical injection program

**Tabell 5-2. Foreløpig oversikt over kjemikalietyper**

Type kjemikalie	Konsentrasjon (ppm vol.)	Tilsettes i	Frekvens
Avleiringshemmer A	50	Produsert vann	Kontinuerlig
Avleiringshemmer B	20-50	Sjøvann	Kontinuerlig
Korrosjonshemmer	50	Produsert vann	Kontinuerlig
Emulsjonsbryter	50	Total væske 1)	Kontinuerlig ved behov
Skumdemper	5	Total væske	Periodisk
Flokkulant	10	Produsert vann	Kontinuerlig
Vokshemmer	150	Total væske 1)	Periodisk
Biocid	80	Total væske 1)	Kontinuerlig
Oksygenfjerner	5	Sjøvann	Kontinuerlig
H <sub>2</sub> S fjerner	150	Produsert vann	Kontinuerlig ved behov
MEG	Batch	Brønnstrøm	Ved behov

1) Olje og produsert vann.

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## Release and disposal of chemicals

**Tabell 7-1 Klassifisering av kjemikaler i henhold til OSPAR**

	Svart kategori: Stoffer som er lite nedbrytbare og samtidig viser høyt potensial for bioakkumulering og/eller er svært akutt giftige. I utgangspunktet er det ikke lov å slippe ut kjemikaller i svart kategori. Tillatelse til bruk og utsipp til spesifikke kjemikaller gis dersom det er nødvendig av sikkerhetsmessige og tekniske grunner.
	Rød kategori: Stoffer som brytes sakte ned i det marine miljøet, og viser potensielle for bioakkumulering og/eller er akutt giftige. Kjemikaller i rød kategori kan være miljøfarlige og skal derfor prioriteres for utskifting med mindre miljøfarlige alternativer. Tillatelse til bruk og utsipp gis kun av sikkerhetsmessige og tekniske hensyn.
	Gul kategori: Kjemikaller i gul kategori omfatter stoffer som ut fra iboende egenskaper ikke defineres i svart eller rød kategori og som ikke er oppført på PLONOR-listen (se under). Ren gul kategori er uorganiske kjemikaller med lav giftighet eller kjemikaller som brytes ned >60% innen 28 dager. Gul-Y1 er 20-60% nedbrutt og forventes å brytes ned fullstendig over tid. Gul-Y2 er moderat nedbrytbare til ikke giftige og ikke-nedbrytbare komponenter. Y2 skal forsøkes substituert på lik linje med røde kjemikaller.
	Grunn kategori: Stoffer som er oppført på OSPAR-konvensjonens PLONOR-liste (Substances used and discharged offshore which are considered to Pose Little Or No Risk to the Environment). Disse kjemikaliene vurderes å ha ingen eller svært liten negativ miljøeffekt. Kjemikaller i grunn kategori omfatter også vann som inngår i kjemikaliene.

From Ivar Aasen PDO,  
Del 2

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## Release and disposal of chemicals

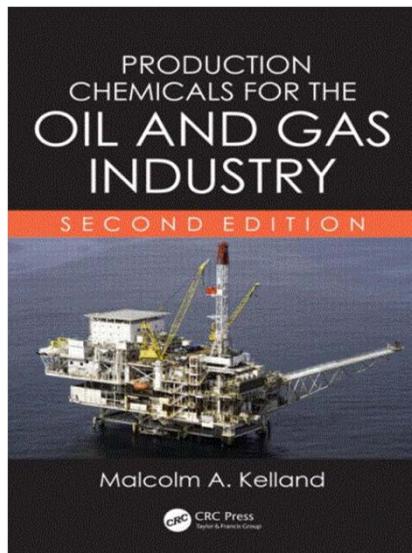
Tabell 7-4 Miljømessige egenskaper til produksjonskjemikalier som vil følge produsert vann fra Johan Castberg-feltet

Type kjemikal	Vannfase/oljefase	Klassifisering
Avleiringshemmer	Vannløselig. Følger produsert vann.	Det er antatt at gult kjemikalie (i klassen Y2) kan velges. Kjemikaliet er moderat bionedbrytbart til ikke bionedbrytbart Det er ikke giftig og vil ikke bioakkumuleres i næringskjeden.
Emulsjonsbryter	Oljeløselig. Følger hovedsakelig oljefasen (95%). 5% følger produsert vann.	
Vokshemmer	Oljeløselig. Følger oljefasen.	Alle disse kjemikaliene er klassifisert som røde, pga det ikke er bionedbrytbart.
Skumdemper	Oljeløselig. Følger i all hovedsak oljefasen, lave konsentrasjoner i produsert vann.	De er ikke giftige og vil ikke bioakkumuleres i næringskjeden.
Flokkulant	Vannløselig, men binder seg til oljedråper. Følger hovedsakelig oljefasen (80%). 20% er antatt å følge produsert vann.	
Biocid/Glutaraldehyd	Vannløselig. Følger injeksjonsvannet eller produsert vann.	Kjemikalie er klassifisert som gult pga giftighet. Det er ikke nedbrytbart og vil ikke bioakkumuleres i næringskjeden.

From Johan Castberg  
PDO, Del 2

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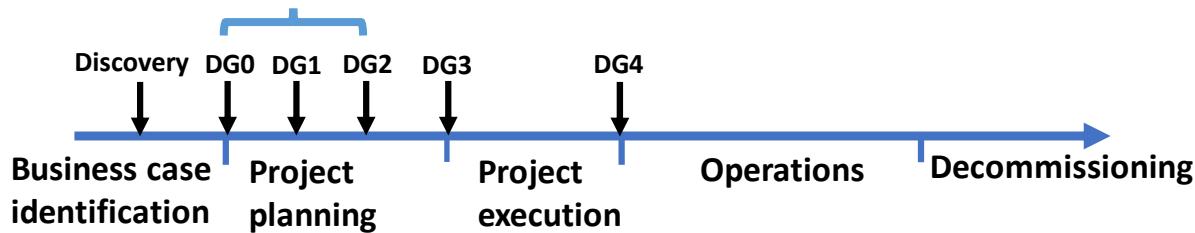
## More about production chemicals



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## Flow assurance evaluation during field planning

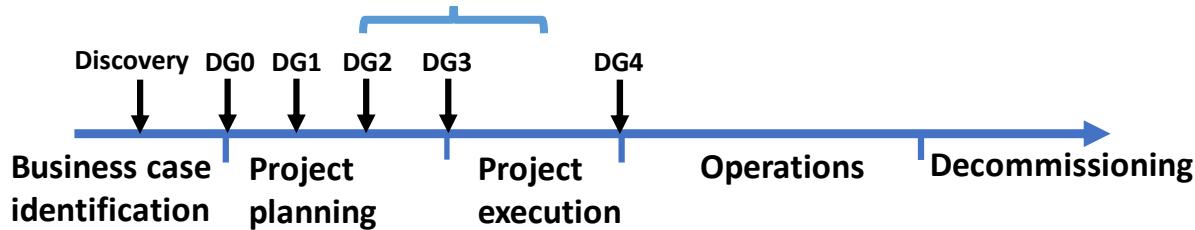
- Detect potential showstoppers and communicate technical constraints and repercussions to field planner
- Laboratory tests



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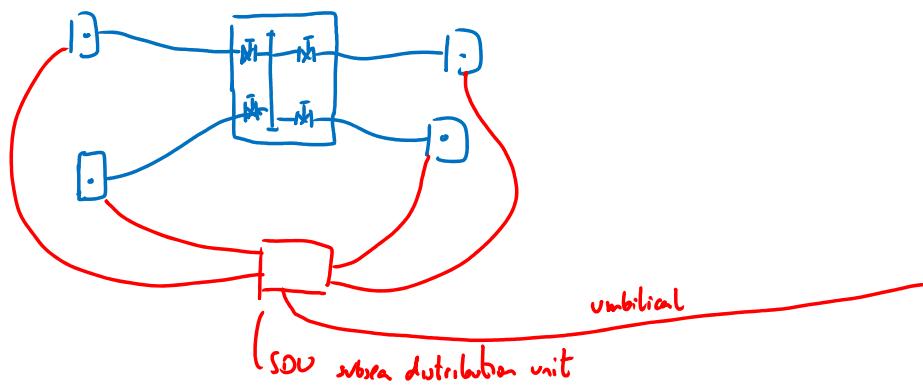
## Flow assurance evaluation during field planning

Refine the flow assurance strategy  
 -More laboratory tests  
 -Management plan  
 -prediction of p and T  
 -Study of startup and shutdown  
 -System design and verification  
 -FIV



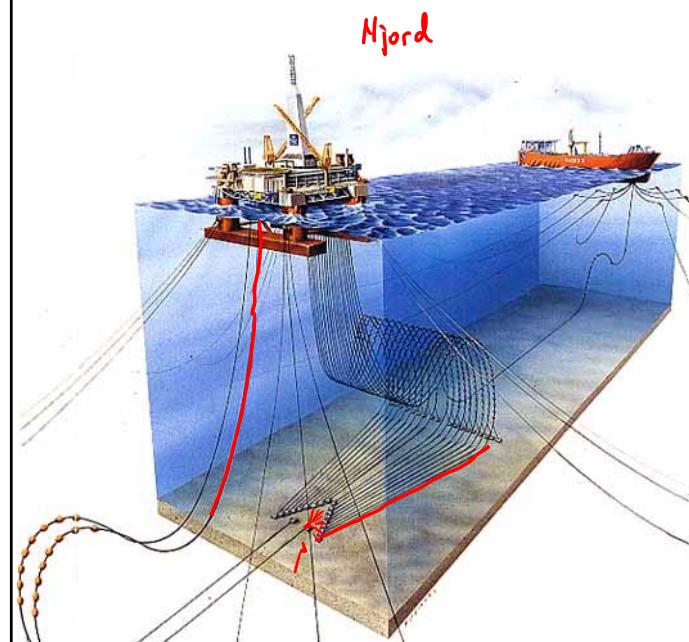
32

## Injection of production chemicals subsea



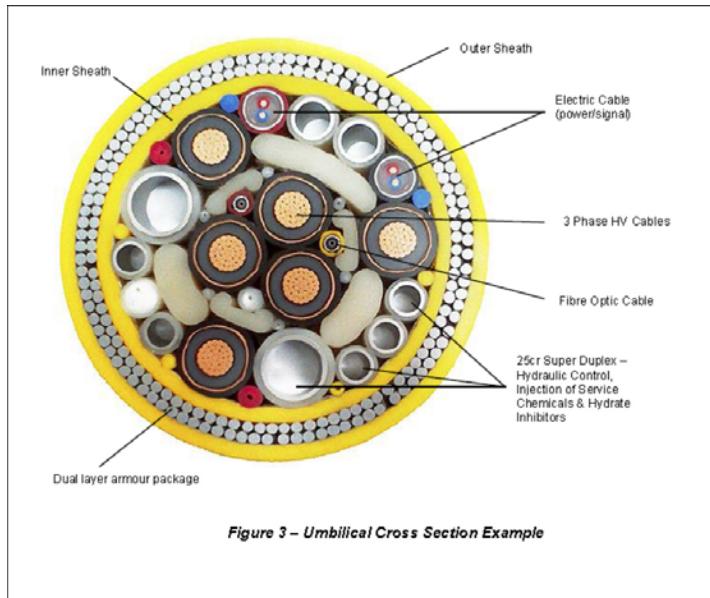
33

## Injection of production chemicals



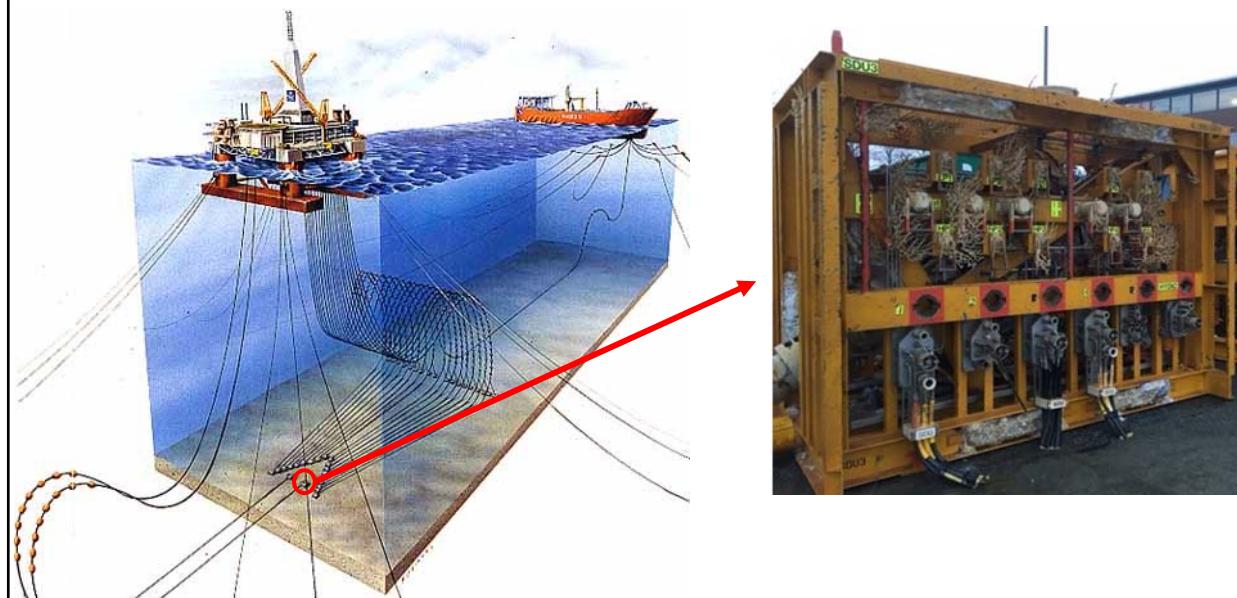
34

## Umbilicals, injection of production chemicals



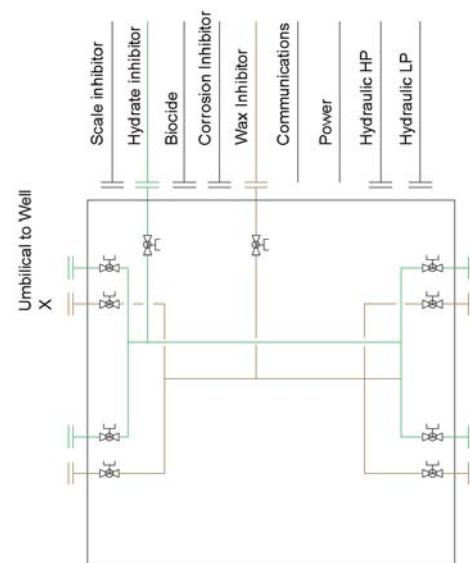
35

## Umbilicals, injection of production chemicals

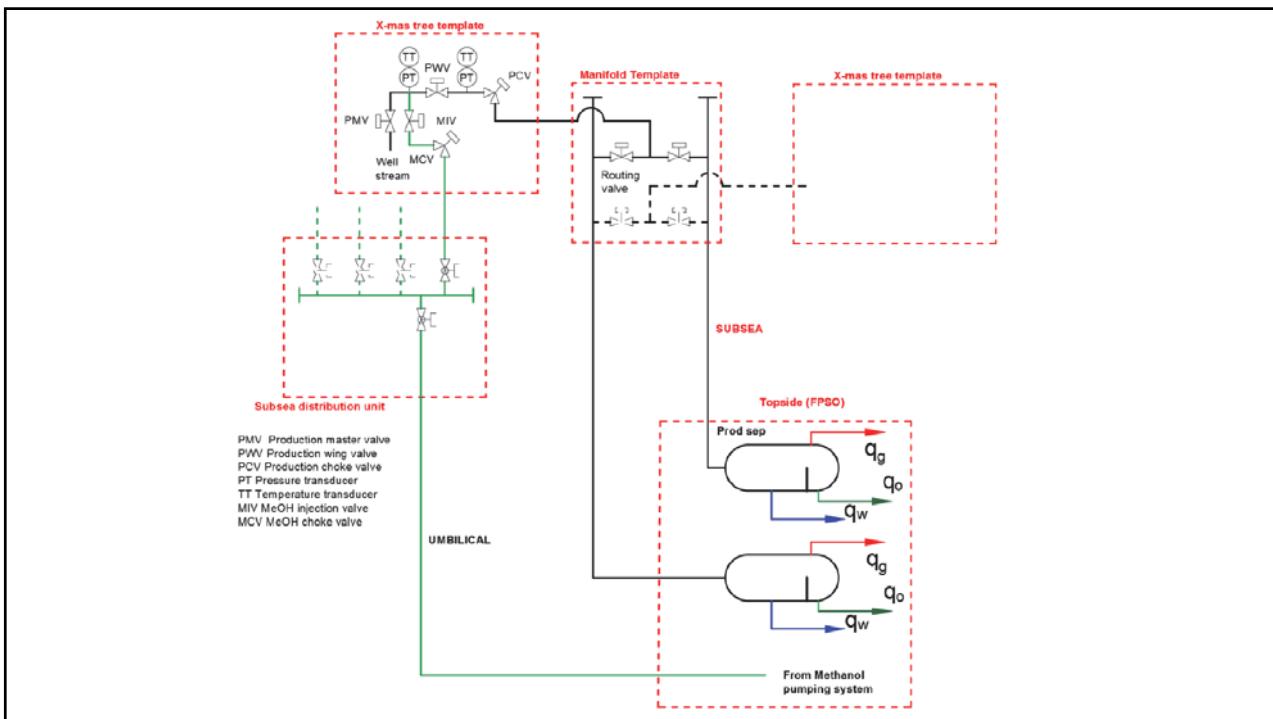


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## Release and disposal of chemicals



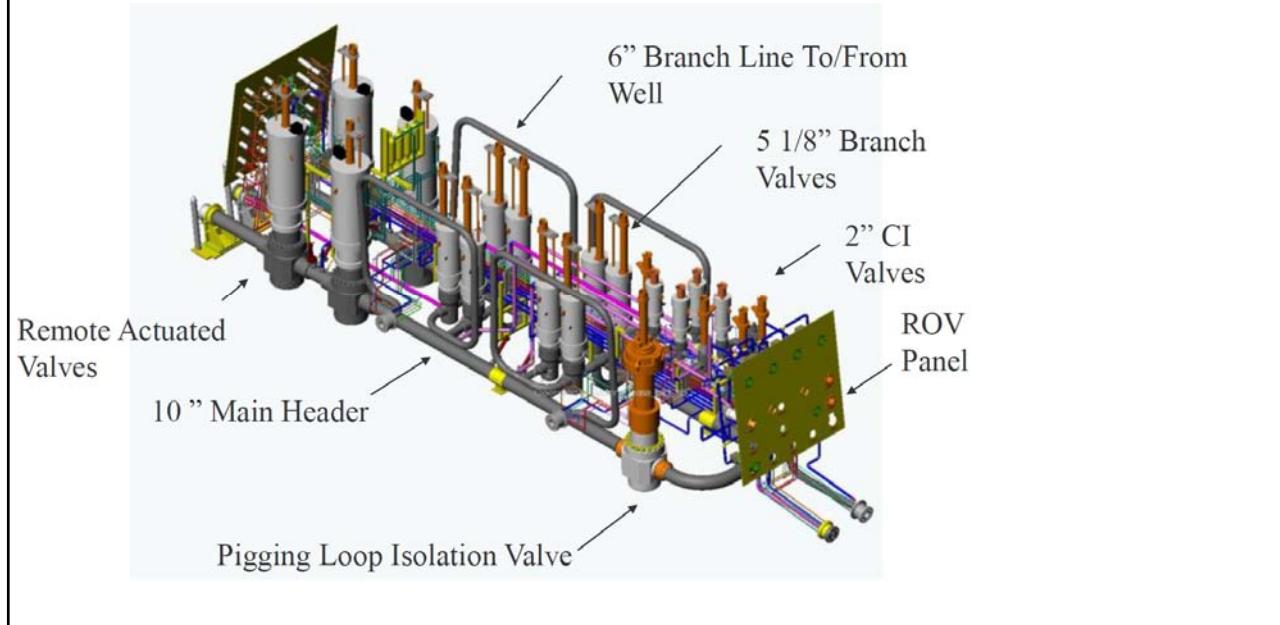
37



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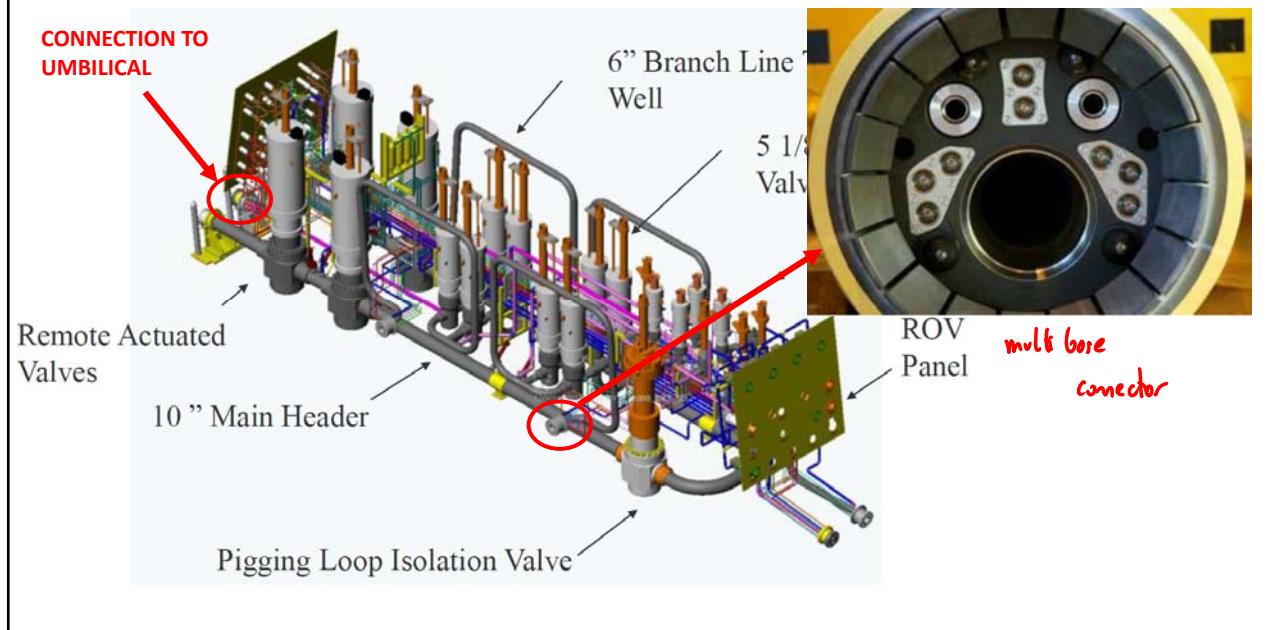
19

## Injection of production chemicals – template wells

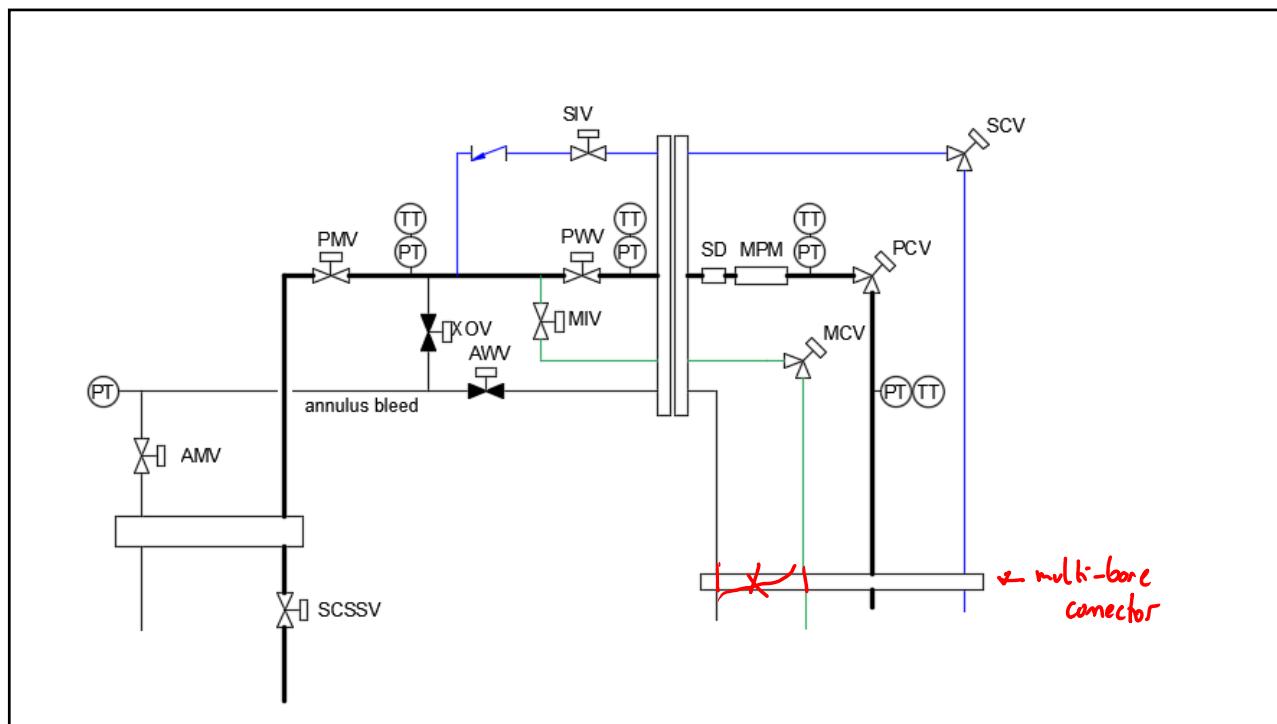


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## Injection of production chemicals – template wells

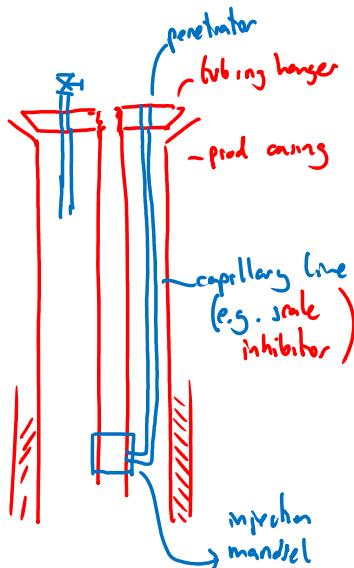


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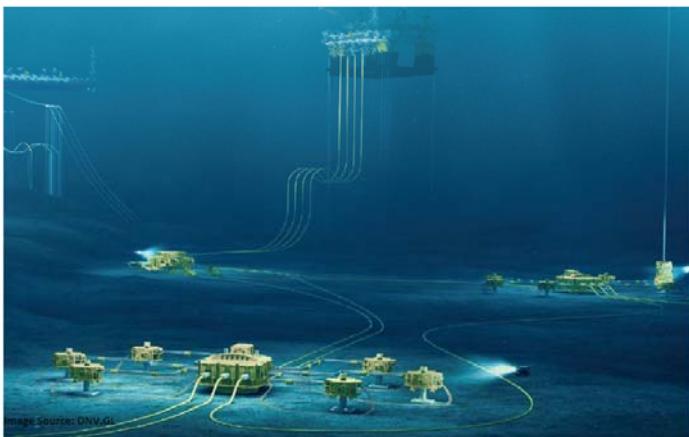
## Injection of production chemicals in well



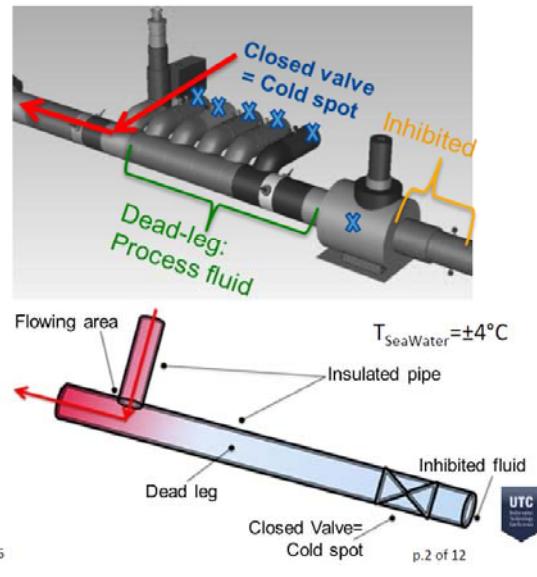
42

## Subsea manifold and dead-leg geometry

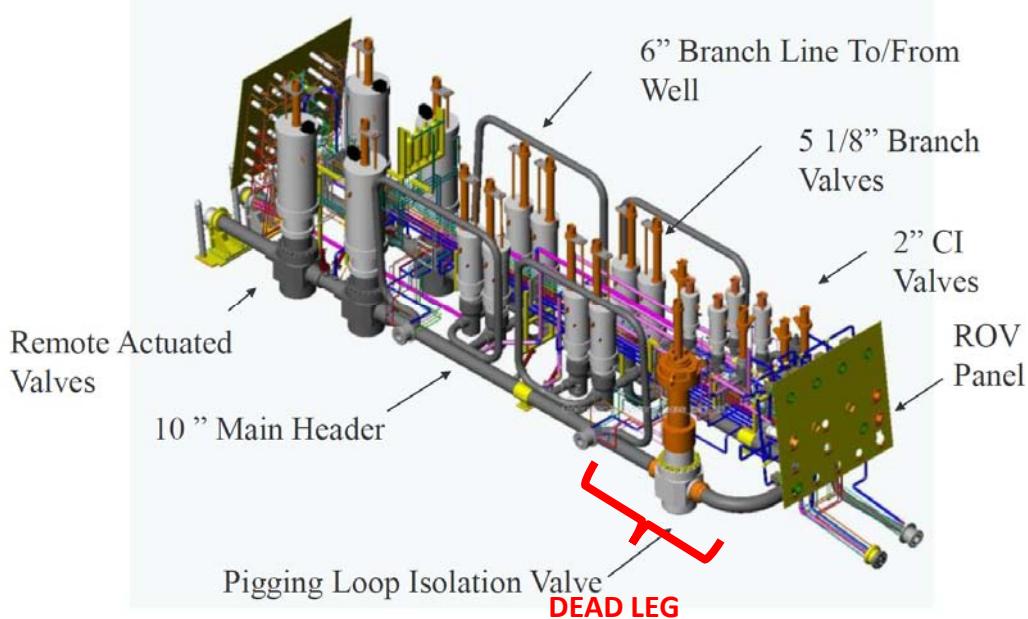
- Dead-legs are inherently present



UTC Bergen - 16<sup>th</sup> June 2016



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## Tools for analysis

- Laboratory tests of fluids (oil, gas, water)
- Steady state flow simulators (Hysys, Gap, Pipesim, Olga, Leda, FlowManager)
- Transient flow simulators (Olga, LedaFlow, FlowManager, Hysys)
- Thermodynamic or PVT simulators (PVTsim, Hysys)
- Standards (DNV, API)
- CFD simulation for 3D flow analysis of pressure and temperature (Comsol, Ansys)
- Finite element analysis for structural analysis and heat transfer in solids (Abacus, Ansys)