

Comments about tubing equation

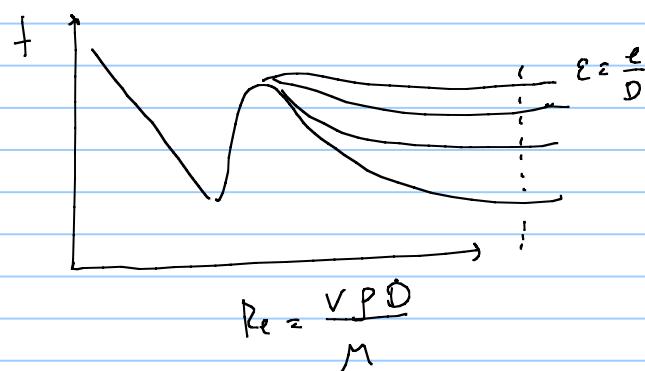
to compute G

$$T_{av} \rightarrow \frac{T_{w1} + T_{wh}}{2}$$

An estimate of T_{wh} is needed

$$T_{av} \rightarrow \frac{T_{w1} + T_{wh}}{2}$$

for friction factor



$M_g \ll M_2$

$$V = f(q_{local})$$

for gas $V \uparrow \uparrow$ ρ is low compared

$$q_{local} = f(\rho)$$

(liquid $V = [0.5 - 4] \text{ m/s}$ to liquid)

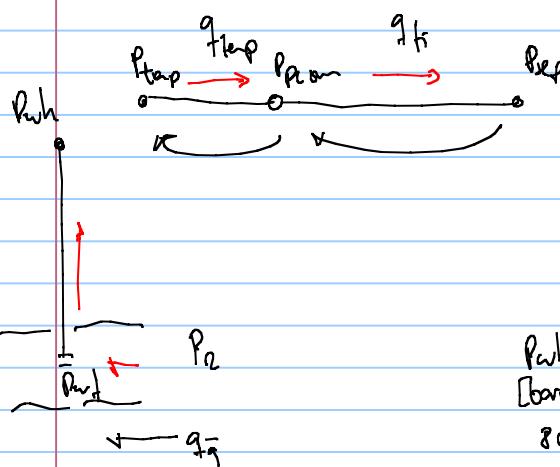
$$\text{gas } V = [5 - 40] \text{ m/s}$$

$$Re_g \gg$$

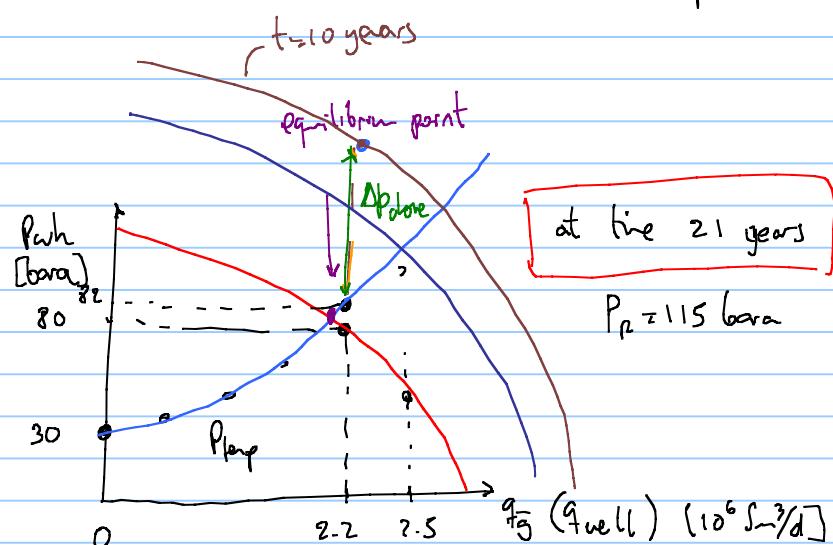
always in fully turbulent regime

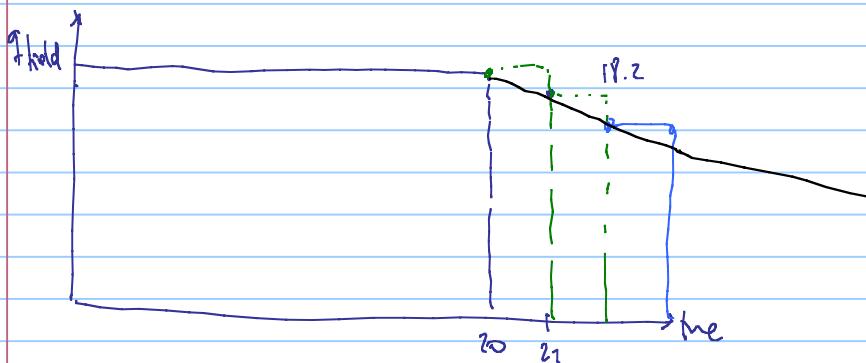
$$f_n = f(\epsilon)$$

however $\epsilon \neq f(D)$
due to manufacturing



$$q_{field} = 3 q_{flow} = q_{well}$$





In reality the well+network simulator works differently, as a system of equations solver
for example

$$\text{IPR} \quad \dot{q}_{\bar{s}_w} = C_R \left(P_w^2 - P_{wh}^2 \right)^n \quad \begin{matrix} \text{EQUATION} \\ 1 \end{matrix} \quad \begin{matrix} \text{UNKNOWN} \\ 2 \end{matrix}$$

$$\text{TPR} \quad \dot{q}_{\bar{s}_w} = C_T \left(\frac{P_w^2}{\epsilon^2} - P_{wh}^2 \right)^{0.5} \quad \begin{matrix} \text{EQUATION} \\ 2 \end{matrix} \quad \begin{matrix} \text{UNKNOWN} \\ 3 \end{matrix}$$

$$\text{FPR} \quad \dot{q}_{\bar{s}_T} = C_F \left(P_{temp}^2 - P_{pcon}^2 \right)^{0.5} \quad \begin{matrix} \text{EQUATION} \\ 3 \end{matrix} \quad \begin{matrix} \text{UNKNOWN} \\ 6 \end{matrix}$$

$$\text{PPR} \quad \dot{q}_{\bar{s}_f} = C_P \left(P_{pcon}^2 - P_{exp}^2 \right)^{0.5} \quad \begin{matrix} \text{EQUATION} \\ 4 \end{matrix} \quad \begin{matrix} \text{UNKNOWN} \\ 7 \end{matrix}$$

$$\text{choke} \quad \dot{q}_{\bar{s}_f} = f(P_{wh}, P_{temp}, \text{opening}) \quad \begin{matrix} \text{EQUATION} \\ 5 \end{matrix} \quad \begin{matrix} \text{UNKNOWN} \\ 7 \end{matrix} \quad (\text{if opening is given})$$

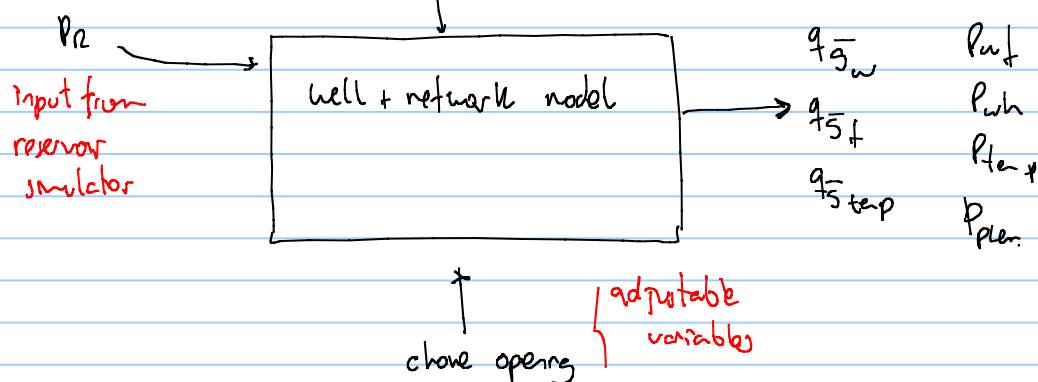
$$\dot{q}_{\bar{s}_w} = \dot{q}_f / N_w \quad \begin{matrix} \text{EQUATION} \\ 6 \end{matrix} \quad \begin{matrix} \text{UNKNOWN} \\ 7 \end{matrix}$$

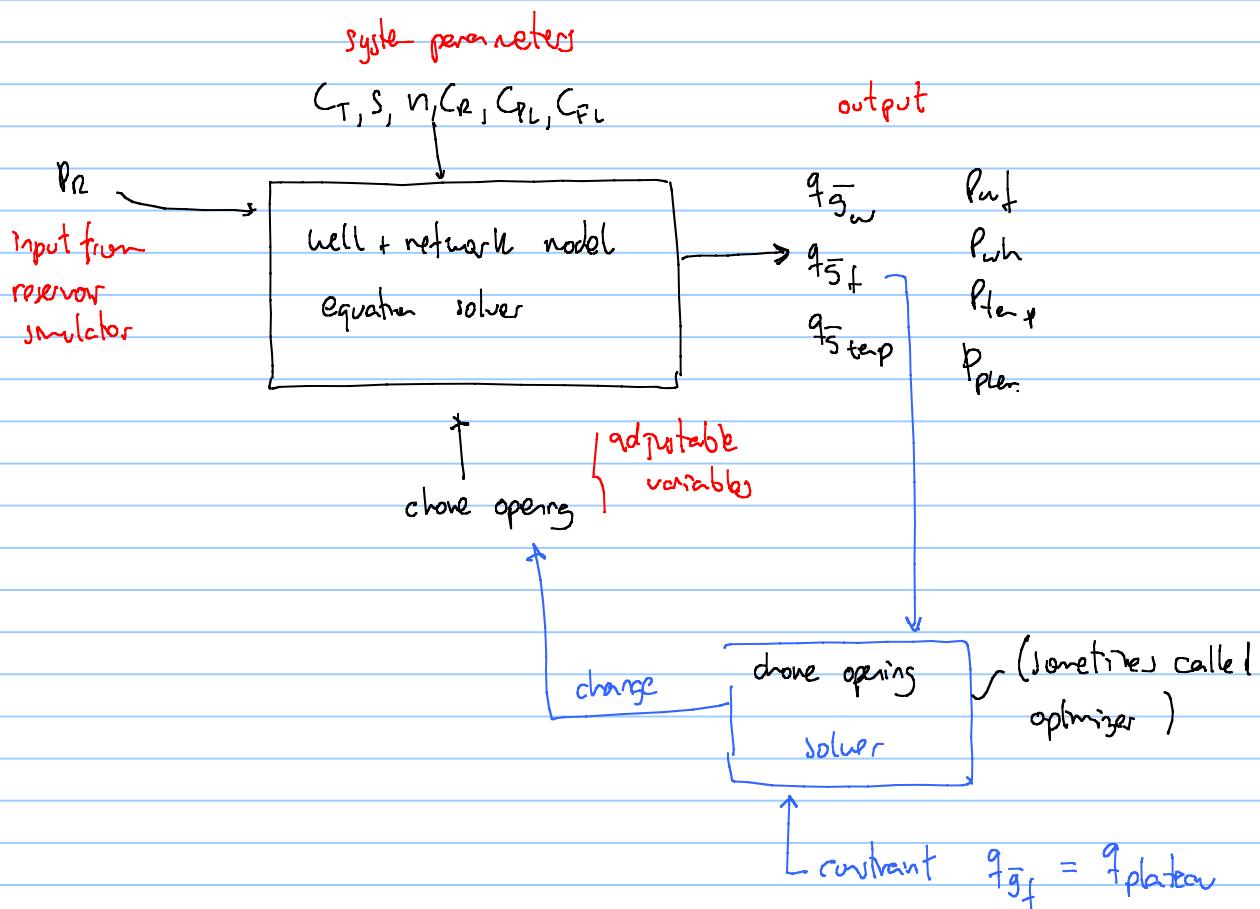
$$\dot{q}_{\bar{s}_b} = \dot{q}_f / N_{temp} \quad \begin{matrix} \text{EQUATION} \\ 7 \end{matrix} \quad \begin{matrix} \text{UNKNOWN} \\ 7 \end{matrix}$$

system parameters

C_T, S, n, C_R, C_P, C_F

output





choke equation for dry gas: (page 166)
"opening" tuning factor

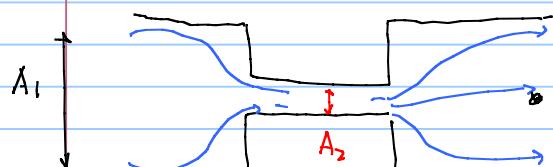
$$q_{\bar{g}} = \frac{p_1 \cdot T_{sc} \cdot A_2 \cdot C_d}{p_{sc}} \cdot \sqrt{\frac{R}{2 \cdot Z_1 \cdot T_1 \cdot M_W} \cdot \frac{k}{k-1} \cdot \left(y^{\frac{2}{k}} - y^{\frac{k+1}{k}} \right)}$$

$$\nu = \frac{C_p}{C_v}$$

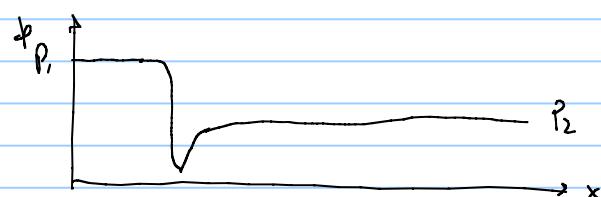
$$p_{sc} = 1.01325 \text{ bar}$$

$$T_{sc} = 15.56^\circ\text{C}$$

$$y = \frac{p_2}{p_1} \begin{matrix} (\text{downstream}) \\ (\text{upstream}) \end{matrix}$$



if $y > y_c \approx 0.6$, there is untracal flow at the throat



$$\text{if } y > y_c \quad q_{\bar{g}} = q_{\bar{s}_c} =$$

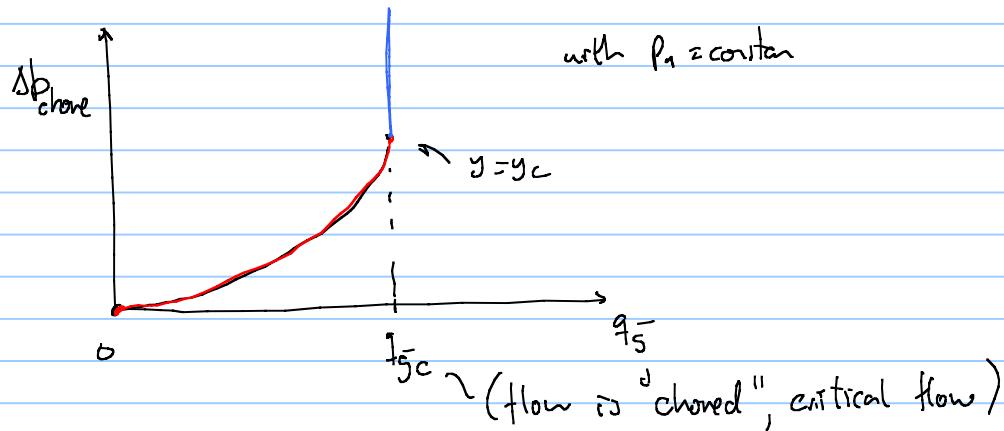
$$q_{\bar{g}} = \frac{p_1 \cdot T_{sc} \cdot A_2 \cdot C_d}{p_{sc}} \cdot \sqrt{2 \cdot \frac{R}{Z_1 \cdot T_1 \cdot M_w} \cdot \frac{k}{k-1} \cdot \left(y^{\frac{2}{k}} - y^{\frac{k+1}{k}} \right)}$$

in blue y_c y_c

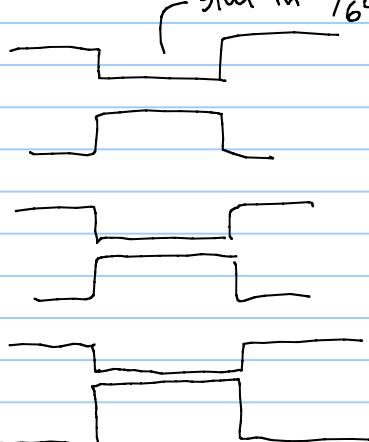
if $y < y_c$

$$q_{\bar{g}} = \frac{p_1 \cdot T_{sc} \cdot A_2 \cdot C_d}{p_{sc}} \cdot \sqrt{2 \cdot \frac{R}{Z_1 \cdot T_1 \cdot M_w} \cdot \frac{k}{k-1} \cdot \left(y^{\frac{2}{k}} - y^{\frac{k+1}{k}} \right)}$$

in red y_c



in onshore fields, beam chokes are often used
given in $\frac{y}{64}$ "



offshore often adjustable
chokes are used
needle choke

