

Software suite from Petroleum Experts: UK, Edinburgh

IPM Integrated petroleum management

MBAL  $\rightarrow$  material balance

Prosper<sup>\*</sup>  $\rightarrow$  well modeling

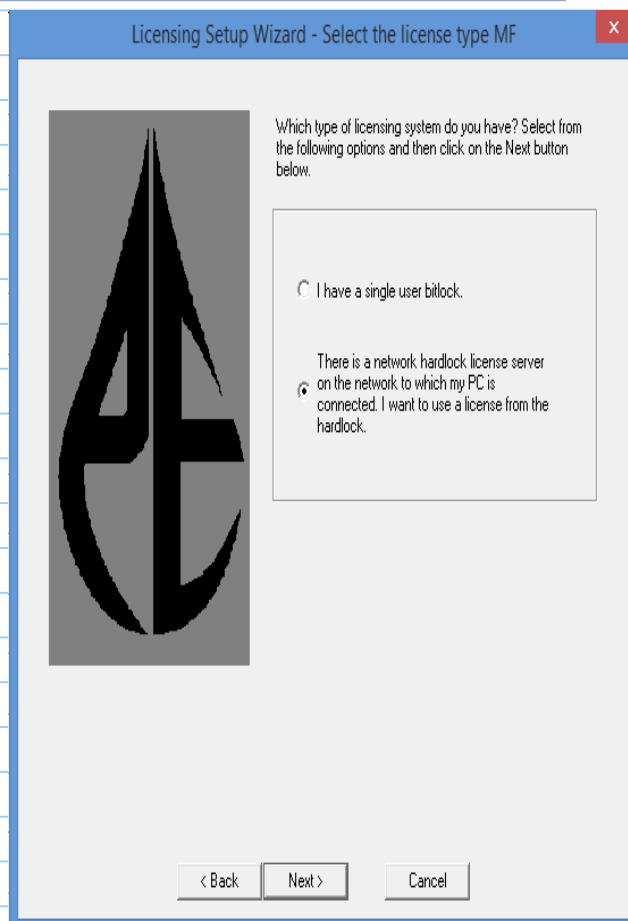
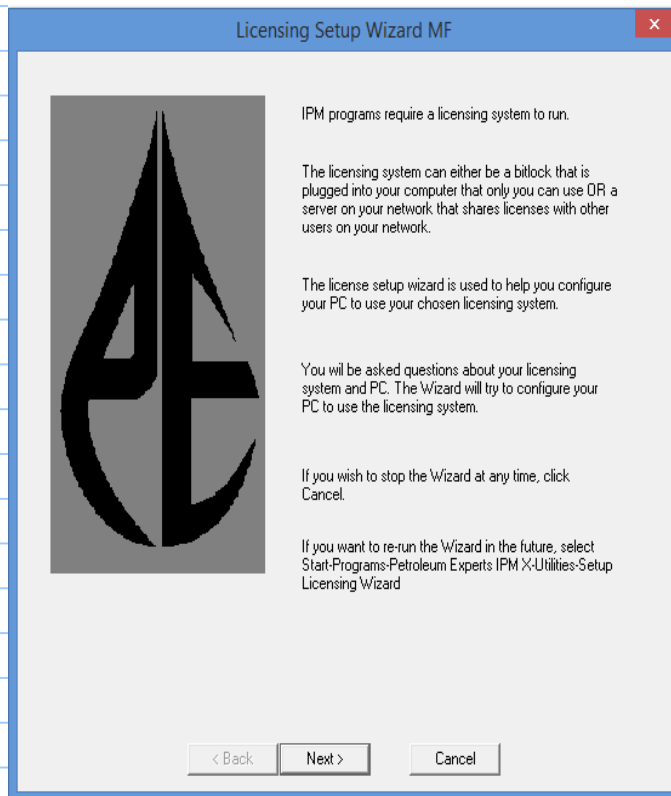
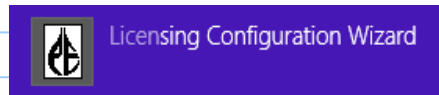
GAP<sup>\*</sup>  $\rightarrow$  networks and production systems (optimization)

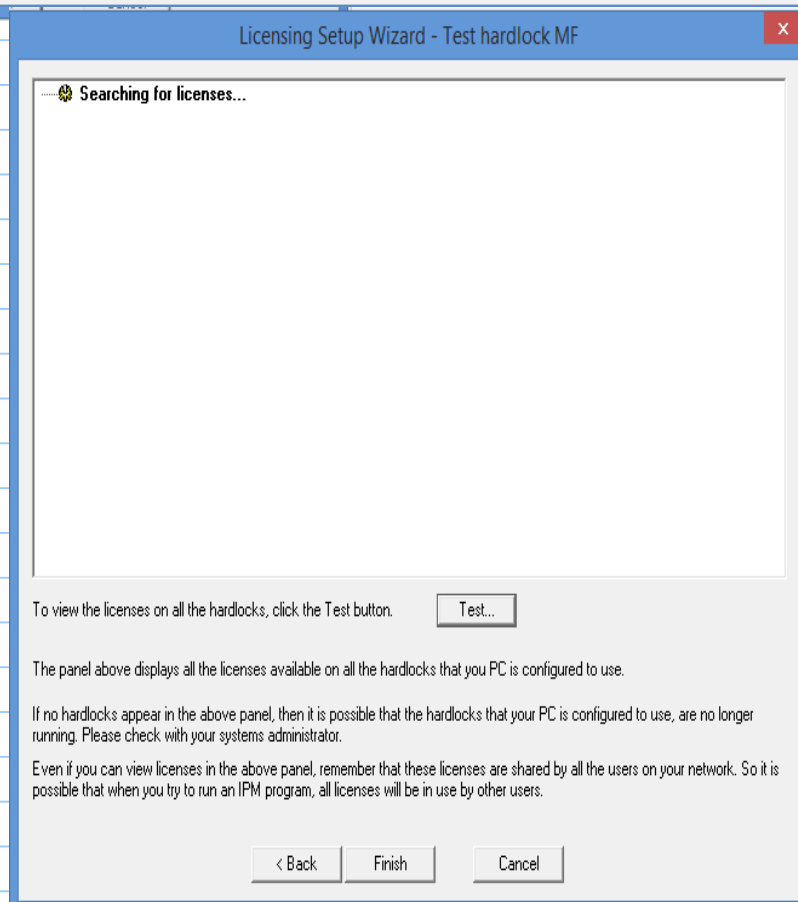
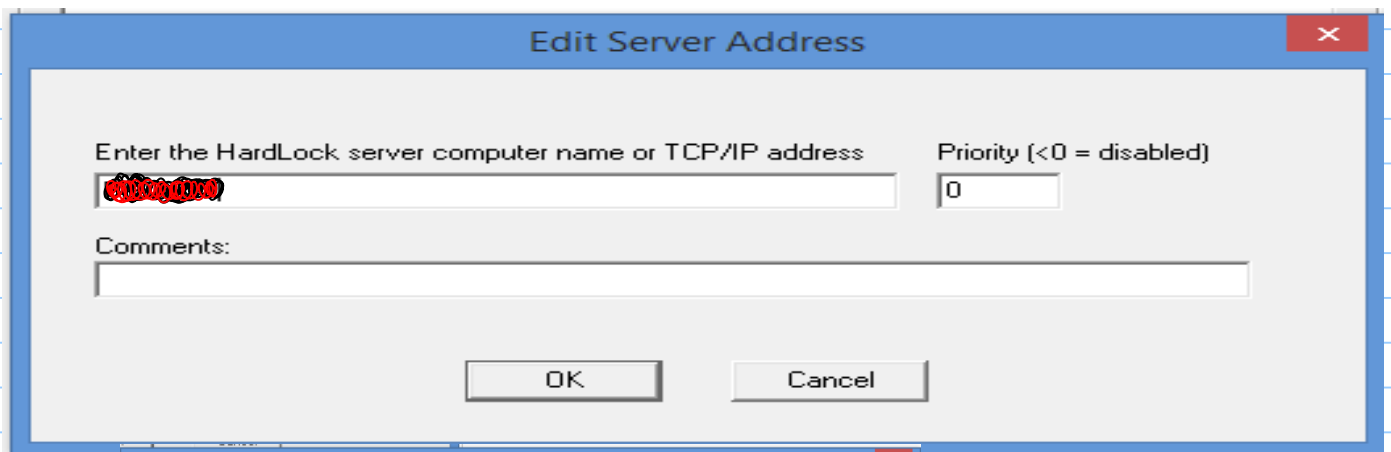
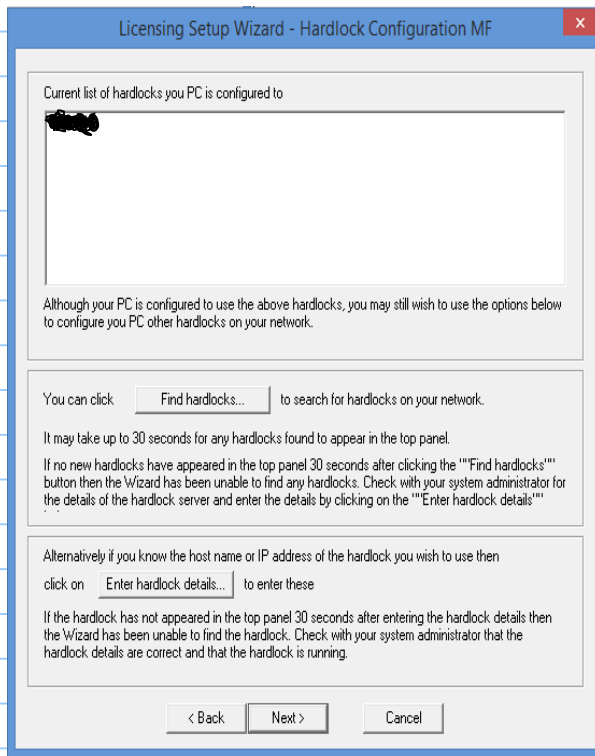
Reveal  $\rightarrow$  res. simulator

PVTP  $\rightarrow$  fluid analysis and modeling

Resolve  $\rightarrow$  coupling between reservoir + production system

IAM integrated asset modeling





**Exercise in Prosper and GAP, TPG4230, Milan Stanko, 20170309.****1. Subsea oil well modeling in Prosper****Fluid information:**

Use the black oil correlation of Glasø ( $p_b$ ,  $R_s$ ,  $B_o$ ) and Beal (viscosity) to model your PVT behavior.

Solution GOR = 142 Sm <sup>3</sup> /Sm <sup>3</sup>	Formation Water salinity = 23000 ppm
Producing GOR = 142 Sm <sup>3</sup> /Sm <sup>3</sup>	No H <sub>2</sub> S, CO <sub>2</sub> , N <sub>2</sub> .
Oil gravity = 30 API (876 Kg/m <sup>3</sup> )	Heat capacity of oil = 2.219 KJ/Kg/K
Gas gravity = 0.76	Heat capacity of gas = 2.1353 KJ/Kg/K
At initial conditions no water.	Heat capacity of water = 4.1868 KJ/Kg/K

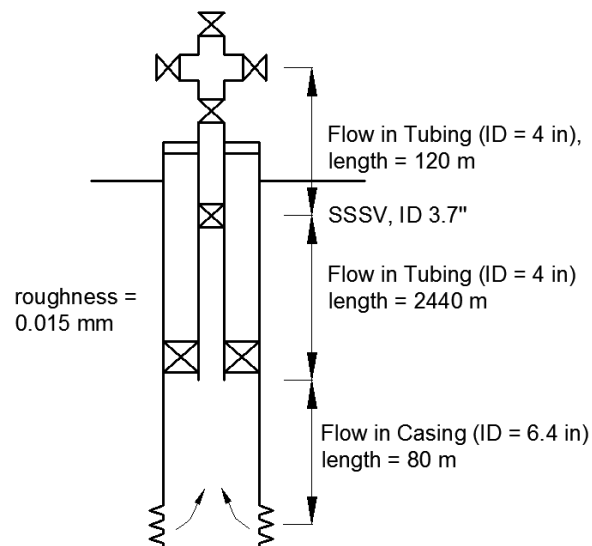
**Well layout:**

Deviation survey

MD [m]	TVD [m]
0	0
123	122
1059	1036
2164	2103
2640	2560

Geothermal gradient

MD [m]	T [C]
0	4
2640	100



**Overall heat transfer coefficient = 45 W/m<sup>2</sup> K**

**Reservoir info:**

Producing from a single layer  
 Reservoir pressure = 360 bara  
 Reservoir temperature = 100 C  
 Water cut = 0%

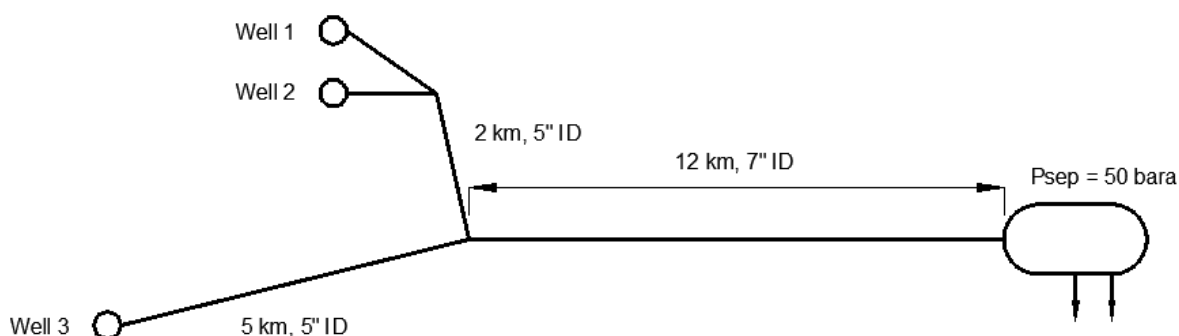
Productivity index =  $12 \text{ Sm}^3/\text{d}/\text{bara}$

### Tasks:

- Set up a prosper model of a subsea oil well.
- Report the bubble point pressure at reservoir temperature as predicted by the BO correlation.
- Estimate the producing rate using flow equilibrium assuming that the well is producing against a constant wellhead pressure of 100 bar. Is it correct to assume a linear productivity index?.
- Generate and export lift curves to be used in GAP (in the following exercise).  $p_{wh}$  range: 30-150 bara, GOR range: 141 – 500  $\text{Sm}^3/\text{Sm}^3$ . WC range: 0 – 50 %

### 2. Modeling of a subsea network with three oil wells in GAP

The layout of the production network layout is shown below. The S riser is not included in the figure. Assume that the water depth is 300 m, and the separator is 30 m above the sea level. The production riser is a lazy "S" riser with a total length of 700 m.



The wells have the same layout as the well created in the previous section, but with different GOR, WC and PI as specified in the table below:

Well	GOR [ $\text{Sm}^3/\text{Sm}^3$ ]	WC [%]	PI [ $\text{Sm}^3/\text{d}/\text{bara}$ ]
Well 1	142	0	12
Well 2	200	40	8
Well 3	250	20	15

### Tasks:

- Build the GAP model of three subsea wells producing to a FPSO.
- Calculate the natural equilibrium flow of the network. Report the flow potential of each well and calculate their split factor.
- Now, assume that the system has to be operated at a constant rate of  $2000 \text{ Sm}^3/\text{d}$ . Try the following methods:
  - Adding a constraint to the separator, add a choke pressure drop (controlled), and run an optimization.
  - Adding a constraint to the wells, and run an optimization

Exercise available here:

[http://folk.ntnu.no/stanko/Courses/TPG4230/2017/Class\\_files/20170309/Exercise\\_in\\_Prosper\\_and\\_GAP.pdf](http://folk.ntnu.no/stanko/Courses/TPG4230/2017/Class_files/20170309/Exercise_in_Prosper_and_GAP.pdf)

via Norwegian STI → PROSPER main interface

**Options Summary** (Box 1): general options

**PVT DATA** (Box 2): put model and calculations

**IPR DATA** (Box 3): IPR setup and model

**EQUIPMENT DATA** (Box 4): well components and architecture

**ANALYSIS SUMMARY** (Box 5): vlp model and performance

**Prosper (32bit) 13.0**

IPM V9.0 - Build # 120 - Jul 4 2014

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C:\HD\NTNU\SEMESTER\Semester\_V\_2015\TPG4230\Notes\20150324\Prosper  
License Number : 04471  
File Format Version : 816  
Current File Version : Original=816 Current=816  
Memory - Load 44% Physical (4095/2047Mb) Virtual (4095/1781Mb)  
Windows (6.2) Build 9200 - 32-bit  
C:\Program Files (x86)\Petroleum Experts\IPM 9\prosper.exe

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Prosper file structure

Oil Well	Anl	541 608 24.03.2015 09:38 -a-
Oil Well	Out	619 439 24.03.2015 09:38 -a-
Oil Well	Pvt	55 729 24.03.2015 09:38 -a-
Oil Well	Sin	179 870 24.03.2015 09:38 -a-
Oil Well	Tpd	9 973 24.03.2015 09:37 -a-
Oil Well	Op	93 183 24.03.2015 09:37 -a-

main prosper file

related with box 2

vlp exported for GAP

related with box 5

Double click to access each box:

- Remember to save your file.
- The first box has to be completed to input in the other boxes

System Summary (Oil\_Well.Out)

Done Cancel Report Export Help Datestamp

Fluid Description: Fluid: oil and water, Method: Black Oil

Separator: Single-Stage Separator

PVT Warnings: Disable Warning

Water Viscosity: Use Default Correlation

Water Vapour: No Calculations

Well: Flow Type: Tubing Flow, Well Type: Producer

Artificial Lift: Method: None

User Information: Company, Field, Location, Well, Platform, Analyst, Date: 24. mars 2015

Calculation Type: Predict: Pressure and Temperature (offshore), Model: Rough Approximation, Range: Full System

Well Completion: Type: Cased Hole, Sand Control: None

Reservoir: Inflow Type: Single Branch

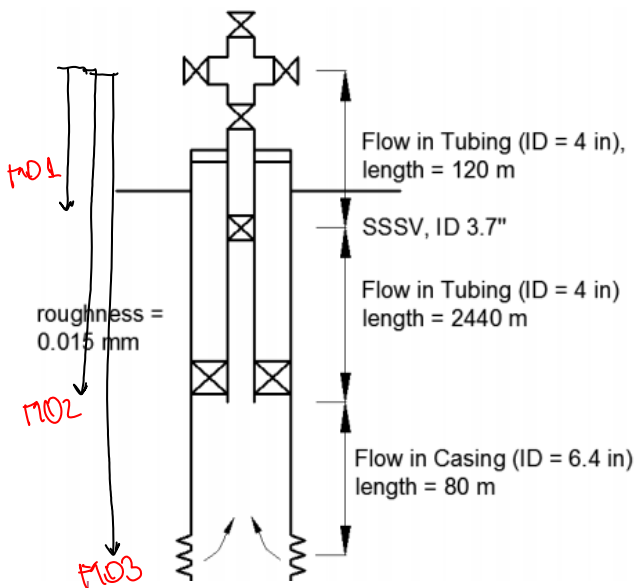
Comments (Ctrl-Enter for new line)

In proper the convention to input

downhole equipment is:

locate yourself at the wellhead (x-mas tree) and list, from top down, how many different sections do you observe: flow in tubing, flow in SSSV, flow in tubing and flow in casing.

- Introduce each one on the table. the measured depth is the depth of the end of the section measured from the wellhead.



DOWNHOLE EQUIPMENT (Oil\_Well.Sin)

Done Cancel Main Import Export Report Tubing DB Casing DB Help

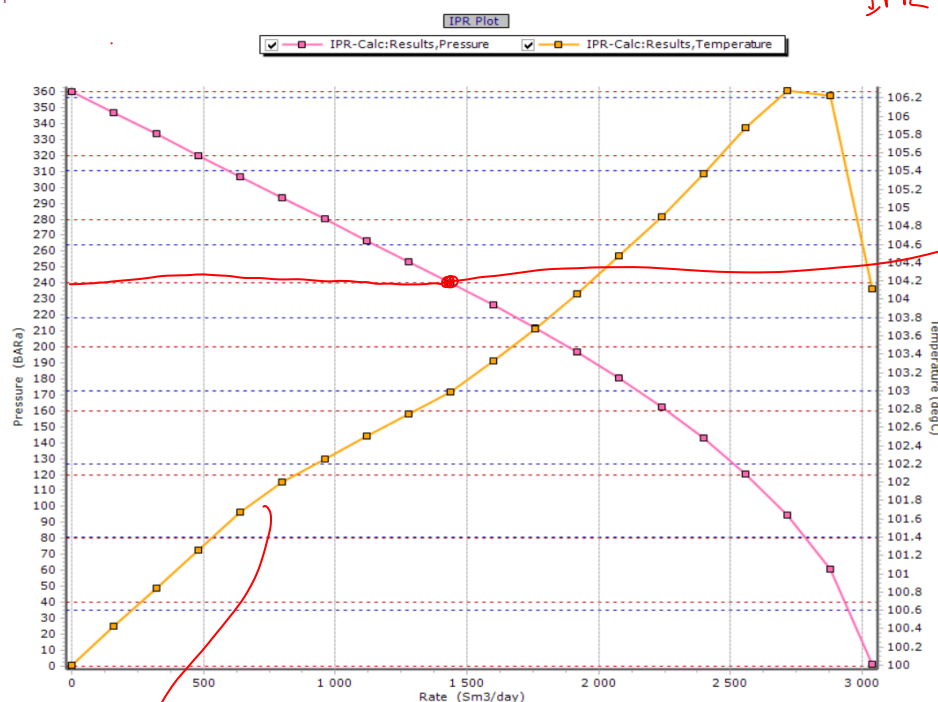
Input Data

Point	Label	Type	Measured Depth (m)	Tubing Inside Diameter (m)	Tubing Inside Roughness (m)	Tubing Outside Diameter (m)	Tubing Outside Roughness (m)	Casing Inside Diameter (m)	Casing Inside Roughness (m)	Rate Multiplier
1		Xmas Tree	0							
2		Tubing	120	0.1	1.524e-5					1
3		SSSV		0.09						1
4		Tubing	2560	0.1	1.524e-5					1
5		Casing	2640					0.16	1.524e-5	1
6										
7										
8										
9										
10										
11										
12										
13										
14										
15										
16										
17										
18										

MD1  
MD1  
(we assume that  
the SSSV has  
no length)

MD2  
MD3

IPR Before leaving the IPR  
• make remember to click  
"calculate". In that way the  
IPR is available for further  
calculations

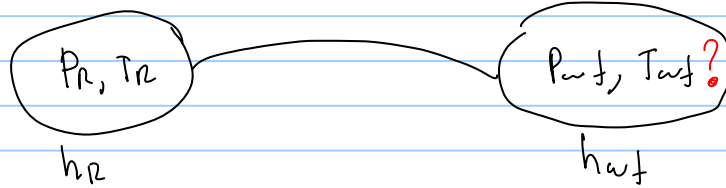


$P_b @ P_r$

below this part  
the curve will deviate  
from the straight  
line.

here, PROSPER assumes that  $P_r \neq P_{wf}$ . this is because the fluid  
experiences an expansion process from  $P_r \rightarrow P_{wf}$ .

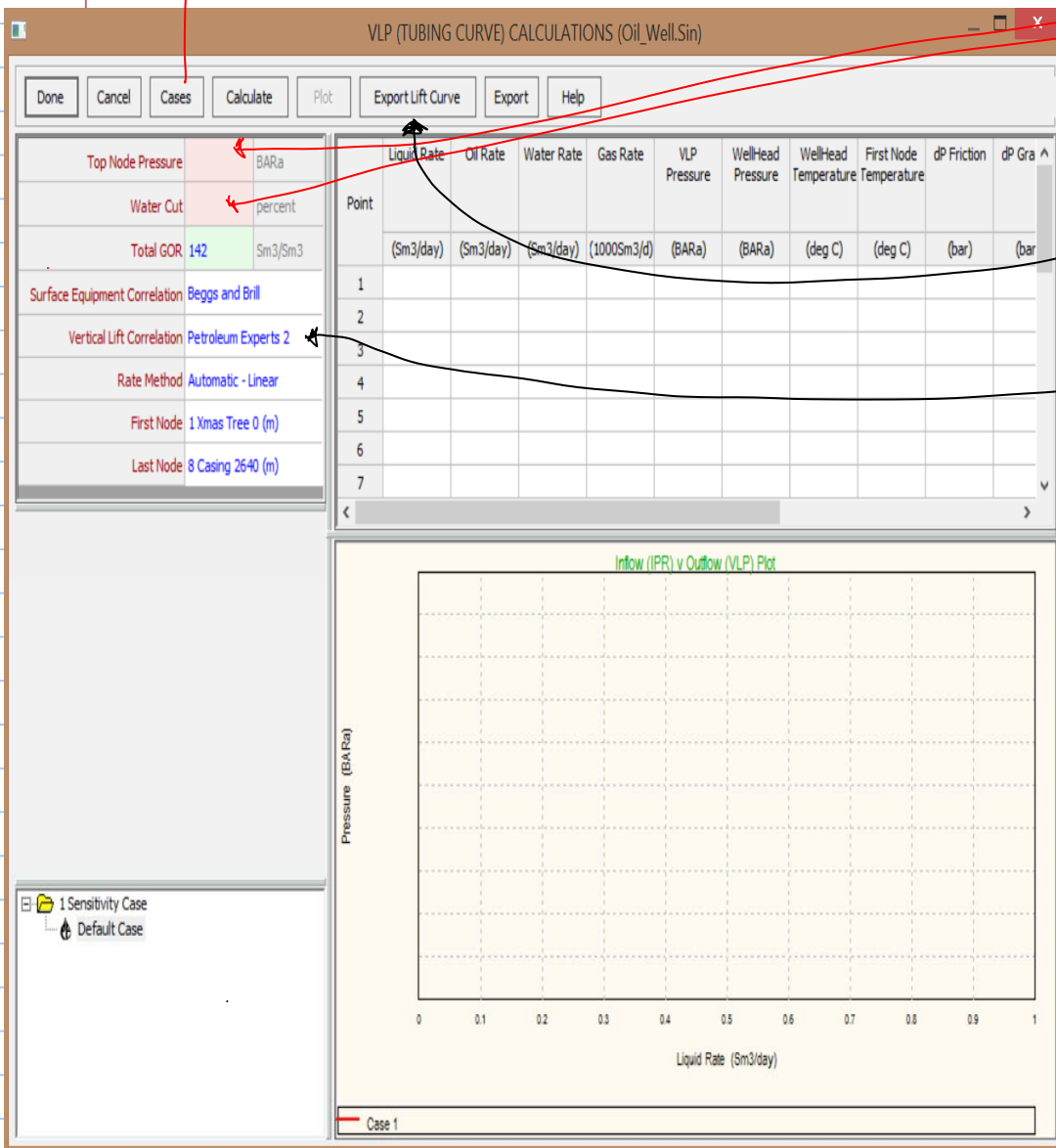
this expansion process is often modeled as isenthalpic, meaning  $h_R = h_{wf}$



with  $h_{wf}$  and  $P_{wf}$  it is possible to calculate  $T_{wf}$ .

VLP

in "cases", the expected variations of GOR, WC, Pwh are input. To be able to access it, make sure that you filled these two boxes:



to export the curves  
use

multiphase "expert"



### 2.8.1.3.1 VLP Correlation Applications

**Fancher Brown** is a no-slip hold-up correlation that is provided for use as a quality control. It gives the lowest possible value of VLP since it neglects gas/liquid slip; it should always predict a pressure, which is less than the measured value. Even if it gives a good match to the measured down hole pressures, Fancher Brown should not be used for quantitative work. Measured data falling to the left of Fancher Brown on the correlation comparison plot indicates a problem with fluid density (i.e. PVT) or field pressure data. **This is thus essentially, a correlation for quality control purposes.**

For oil wells, **Hagedorn Brown** performs well for slug flow at moderate to high production rates but well loading is poorly predicted. Hagedorn Brown should not be used for condensates and whenever mist flow is the main flow regime. Hagedorn Brown under predicts VLP at low rates and should not be used for predicting minimum stable rates.

**Duns and Ros Modified** The Duns and Ros Modified correlation is derived from the Duns and Ros Original correlation. The original correlation was modified by Petroleum Experts to overestimate the pressure drop in oil wells for the slug flow regime. This correlation should not be used for calculating the pressure drop in the wellbore or pipelines and hence should not be used for lift curve generation either. **This correlation should only be used for quality checking of the input well test data.**

**Duns and Ros Original** The Duns and Ros Original Correlation is derived from the original published method. In **PROSPER** the original Duns and Ros correlation has been enhanced and optimised for use with condensates. This correlation performs well in mist flow cases and may be used in high GOR oil wells and condensate wells.

**Petroleum Experts** correlation combines the best features of existing correlations. It uses the Gould et al flow map and the Hagedorn Brown correlation in slug flow, and Duns and Ros for mist flow. In the transition regime, a combination of slug and mist results is used.

**Petroleum Experts 2** includes the features of the PE correlation plus original work on predicting low-rate VLPs and well stability.

**Petroleum Experts 3** includes the features of the PE2 correlation plus original work for viscous, volatile and foamy oils.

**Petroleum Experts 4** is an advanced mechanistic model for any angled wells (including downhill flow) suitable for any fluid (including Retrograde Condensate).

**Petroleum Experts 5.** The PE5 mechanistic model is an advancement on the PE4 mechanistic model. PE4 showed some instabilities (just like other mechanistic models) that limited its use across the board. PE5 reduces the instabilities through a calculation that does not use flow regime maps as a starting point. PE5 is capable of modelling any fluid type over any well or pipe trajectory. This correlation accounts for fluid density changes for incline and decline trajectories. The stability of the well can also be verified with the use of PE5 when calculating the gradient traverse, allowing for liquid loading, slug frequency, etc. to be modelled.

**Petroleum Experts 6** includes the features of the PE3 correlation plus original work on the effects that water cut can have on a viscous oil.

**Orkiszewski** correlation often gives a good match to measured data. However, its formulation includes a discontinuity in its calculation method. The discontinuity can cause instability during the pressure matching process; therefore its use is not encouraged.

**Beggs and Brill** is primarily a pipeline correlation. It generally over-predicts pressure drops in vertical and deviated wells.

**Gray** correlation gives good results in gas wells for condensate ratios up to around 50 bbl/MMscf and high produced water ratios. Gray contains its own internal PVT model which over-rides **PROSPER**'s normal PVT calculations.

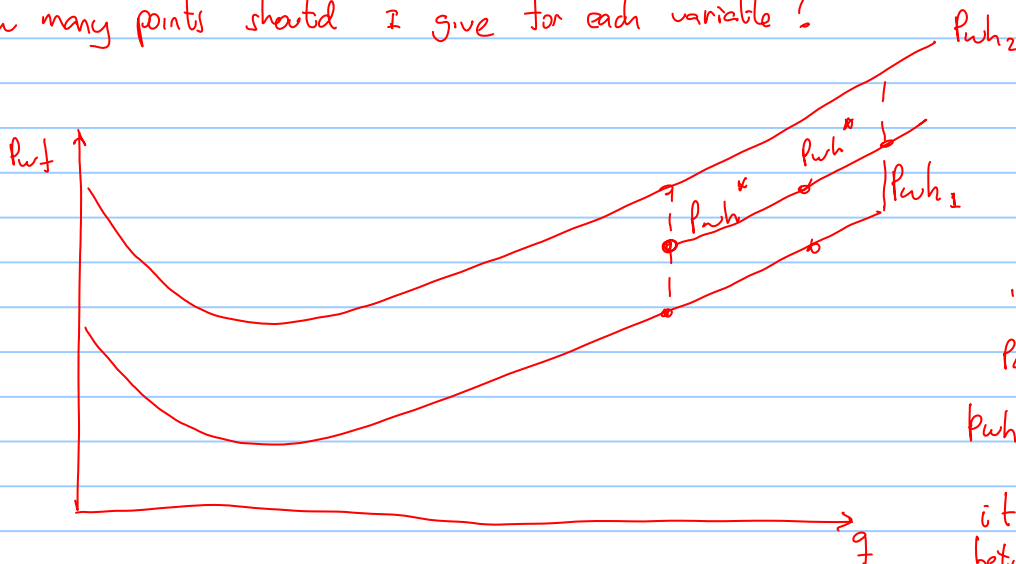
**Hydro 3P (internal)** is a mechanistic model and considers three phase flow.



There is no universal rule for selecting the best flow correlation for a given application. It is recommended that the Correlation Comparison always be carried out. By inspecting the predicted flow regimes and pressure results, the User can select the correlation that best models the physical situation.



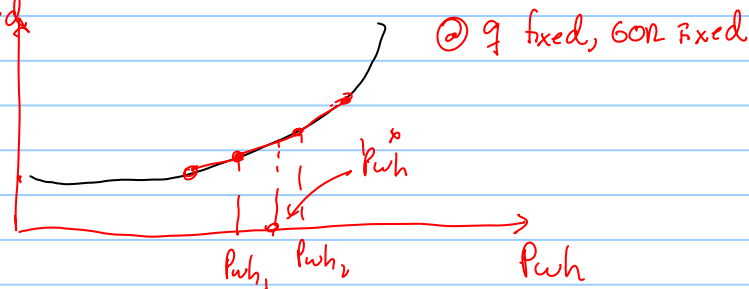
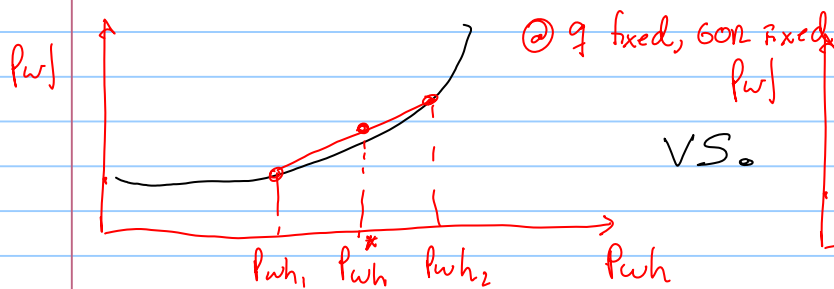
how many points should I give for each variable?



if I need  $P_{wf}$  for  $P_{wh}^*$  between  $P_{wh1} \leq P_{wh} \leq P_{wh2}$

it will interpolate between the two curves above

if  $P_{wh1}$  is relatively close to  $P_{wh2}$  the interpolation error will be small.



Prosper manual available here :

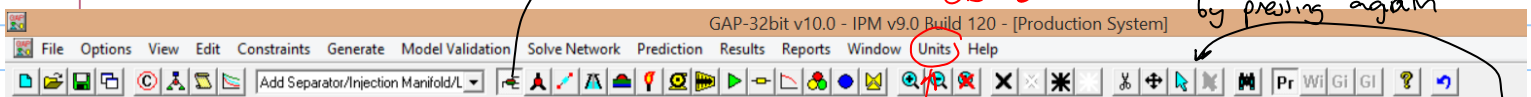
[C:\Program Files \(x86\)\Petroleum Experts\IPM 9\pdf\prosper](C:\Program Files (x86)\Petroleum Experts\IPM 9\pdf\prosper)

GAP network.

make the network layout

click on the element and click again in the canvas where you want to place it.

OBS! remember to unselect it by pressing again



! change units to Norwegian SI

the button or pressing here otherwise you might add the same component again by mistake



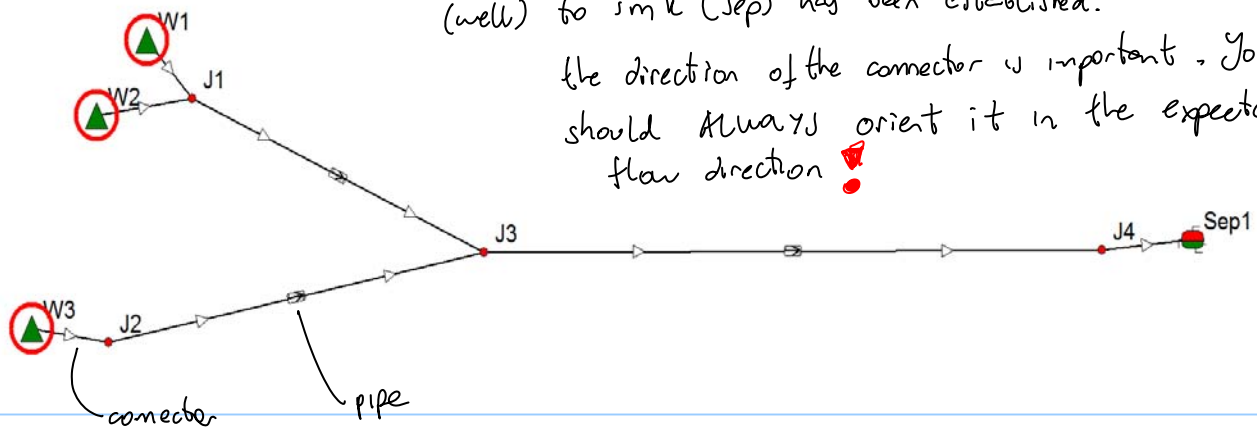
• pipe can only exist between two joints

• a connector between an element or a joint just means that the  $P_{wh}$  of  $W3$  is equal to  $P_{J2}$ , have the same water and conditions



the colors become bright when a full flow path from source (well) to sink (sep) has been established.

the direction of the connector is important. You should ALWAYS orient it in the expected flow direction!



Double click on the wells and link all of them to the proper file we just created

Well 'W1' - Summary

Label	Name	Mask
W1		Included in system

Comments

Well Type: Oil Producer (No lift) | Model: VLP / IPR intersection | Rate Model: Use volumes | ☐ Tight Oil

PROSPER File: C:\Users\Milan\Desktop\Oil\_Well.Out | Valid | Browse

Data Summary (click item to activate)

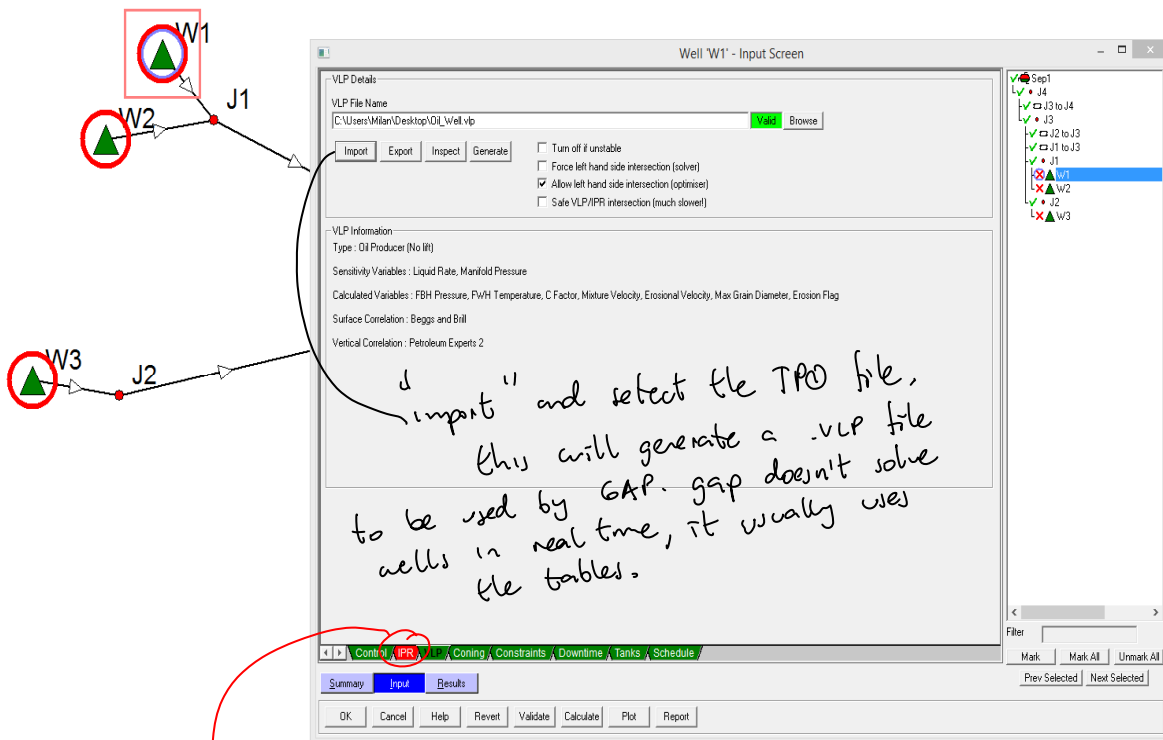
Tank Conns	OK	Controls	Not Set
IPR	Invalid	Downtime	None
VLP	Invalid	Coning	None
Constraints	None	Schedule	None

Summary | Input | Results

OK | Cancel | Help | Revert | Validate | Calculate | Plot | Report

click here to assign the VLP.

we will assume that all wells have the same layout architecture.



IPR hasn't been defined. To transfer it from prosper to GAP go to "Generate IPR"

