



#### **TPG 4135 Production Technology**

Field Processing and Systems

Postdoc Mariana Díaz 03 /25/2019

#### **Plan**



Week Nr.	Week starts	Topic	Lecturer
		Course introduction. Overview of field processing. Product	
2	07.jan.19	specs.	MS
3	14.jan.19	Oil-Gas sep (VLE), Rachford Rice, EOS calculations.	MS
		Oil-Gas Separation . Introduction to process simulation	
4	21.jan.19	(Hysys). Oil-Gas Separation. Bubble and droplet dynamics.	MD
		Separation capacity.	
5	28.jan.19	Oil-water separation	MD
6	04.feb.19	Mechanical Design . Subsea and no standard separators	MD
7	11.feb.19	Water content in Natural gas. Gas dehydration (TEG)	MS
8	18.feb.19	Gas dehydration (TEG)	MS
9	25.feb.19	Pressure calculations in pipe (single and two-phase)	HA
10	04.mar.19	Pressure calculations in pipe (single and two-phase)	HA
11	11.mar.19	Heat transfer, pipe calculations, heat exchangers	HA
12	18.mar.19	Heat transfer, pipe calculations, heat exchangers	HA
13	25.mar.19	Pumping	MD
14	02.apr.19	Compression	HA
15	08.apr.19	Compression	НА
16	15.apr.19	Påskeferie	-
17	23.apr.19	Compression (probably one lecture only)	HA
18	29.apr.19	Spørretime	All

Monday: 12:15-14:00 (P12 PTS)

Tuesday: 14:15-16:00 (VG13 NHL)

Exercise: 16:15-18:00

Exam: 29.05, 15:00-19:00

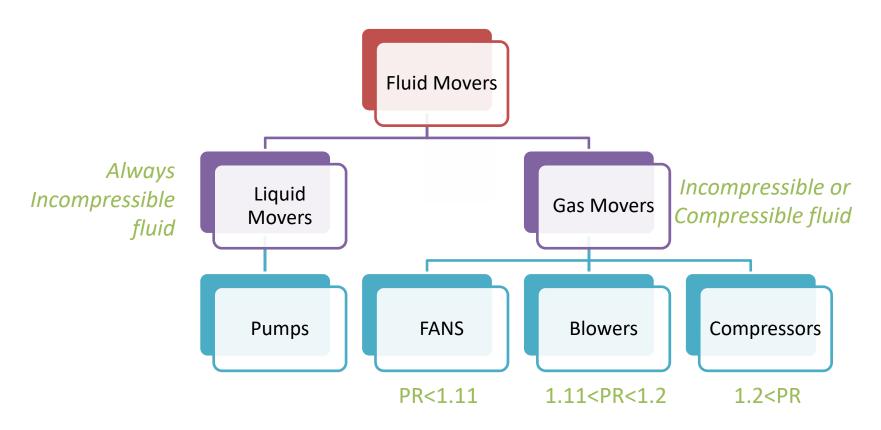


### **PUMPING**

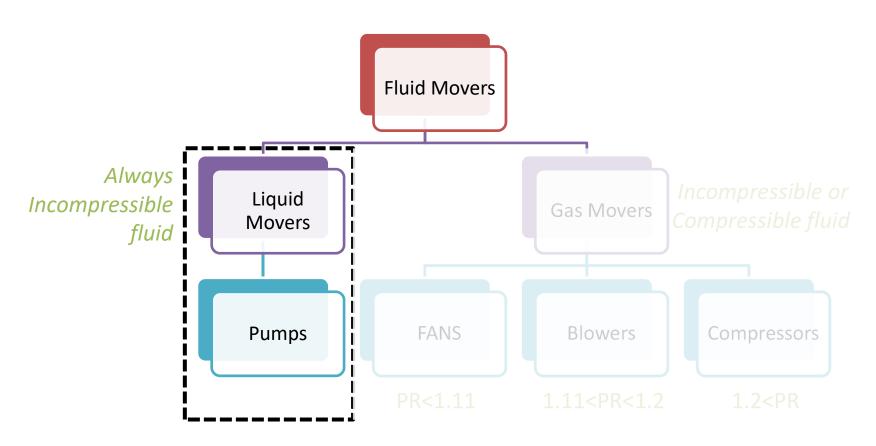


- Moving fluids from one place to another
- Fluids: gas or liquid
- Fluid movers: two main categories: liquid movers (PUMPS) and gas movers (FANS,BLOWERS,COMPRESSORS)
- Fluid movers are used to increase the total energy content of a fluid. This energy increase may be in the form of pressure increase, velocity increase, or the combined effect of both (Badr and Ahmed, 2014)
- Flow in liquid movers is always incompressible. Gas movers may be incompressible (FANS) or compressible (COMPRESSORS)



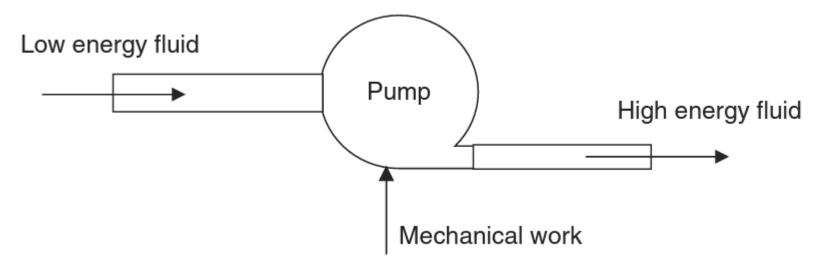








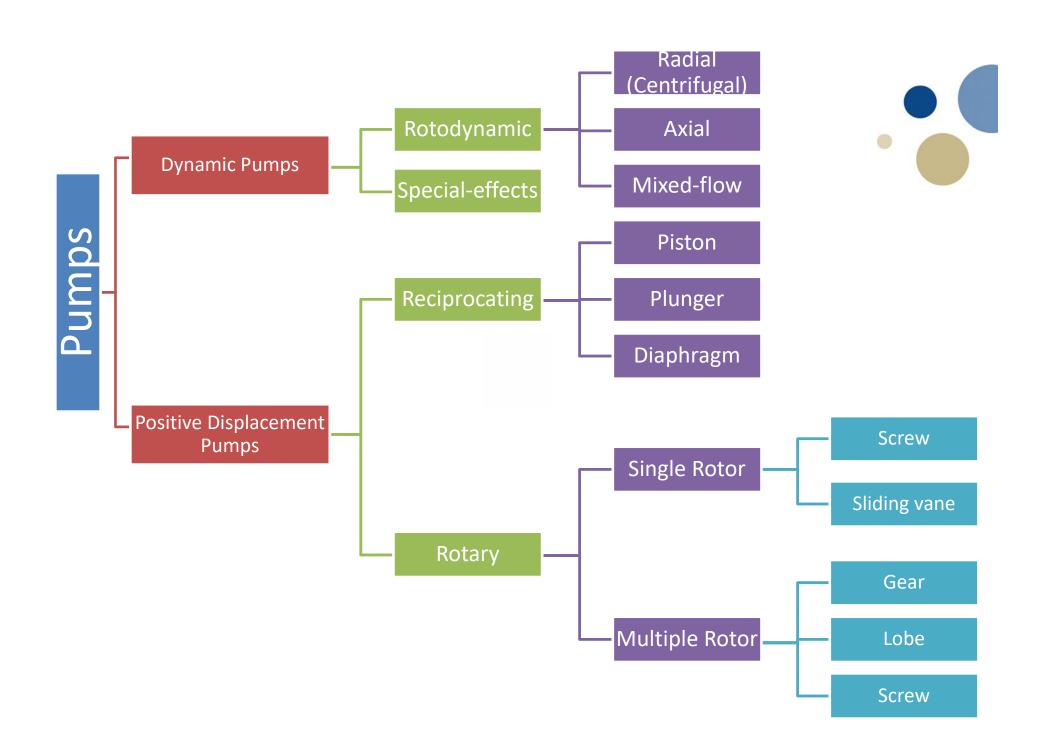
A pump is a liquid mover that utilizes mechanical work to increase the total energy content of a fluid



(Badr and Ahmed, 2014)

Performance characteristics depend on:

- Fluid properties
- Shape and size of the machine
- Speed of rotation





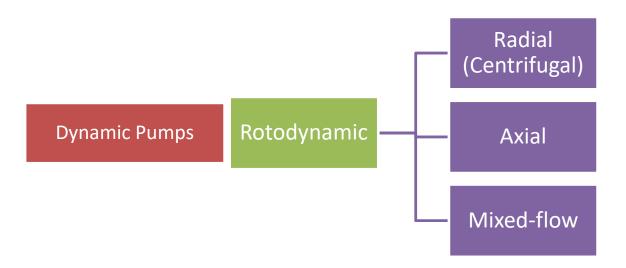
**Dynamic Pumps** 

The **fluid velocity is increased inside the pump** to values higher than the discharge velocity. **Velocity reductions within or after the pump create higher pressure** (Badr and Ahmed, 2014)

Positive Displacement Pumps Energy is added to the fluid by the direct application of a force that moves the fluid from the low pressure side to the high pressure side. (Badr and Ahmed, 2014)

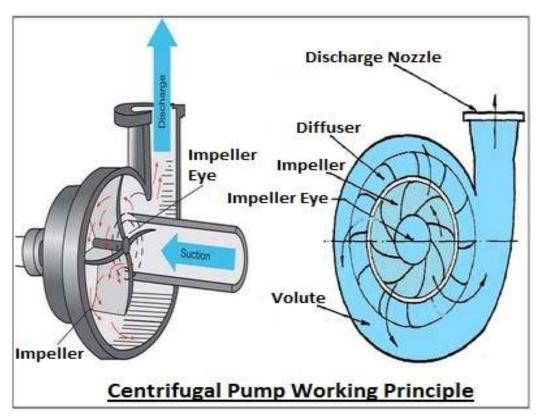
These pumps operate with enclosed liquid volumes which are forced forward in the direction of pumping (Nesbitt, 2006)





It is characterized by one or more **impellers** equipped with **vanes** which rotate in a **pump casing** 

#### Radial (Centrifugal)



https://mechanicallyinfo.com/centrifugal-pump-working-principle/





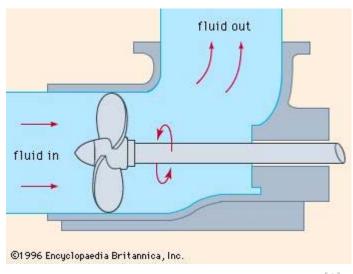




Semi-open impeller

Closed impeller



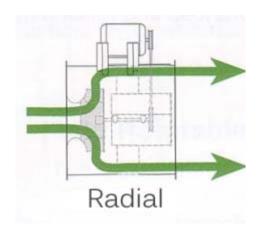


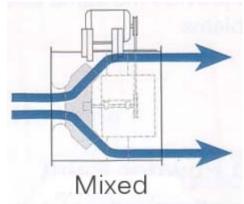


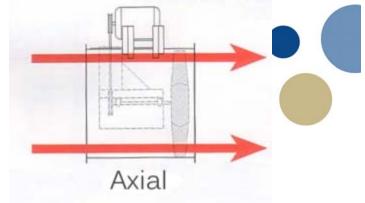
[1]

- http://www.writeopinions.com/axial-flow-pump
- https://www.globalspec.com/learnmore/flow\_transfer\_control/pumps /axial\_flow\_pumps
- [3] https://www.indiamart.com/proddetail/axial-pump-impeller-10585051862.html

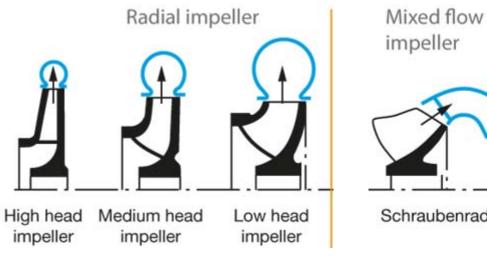






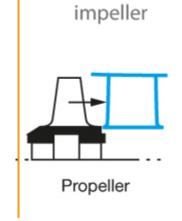


[1]



[2]





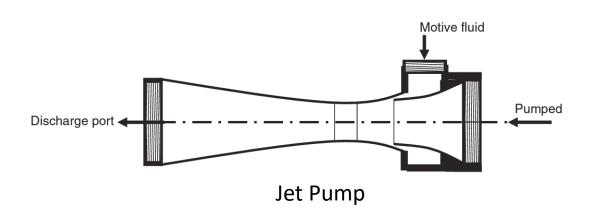
Axial flow

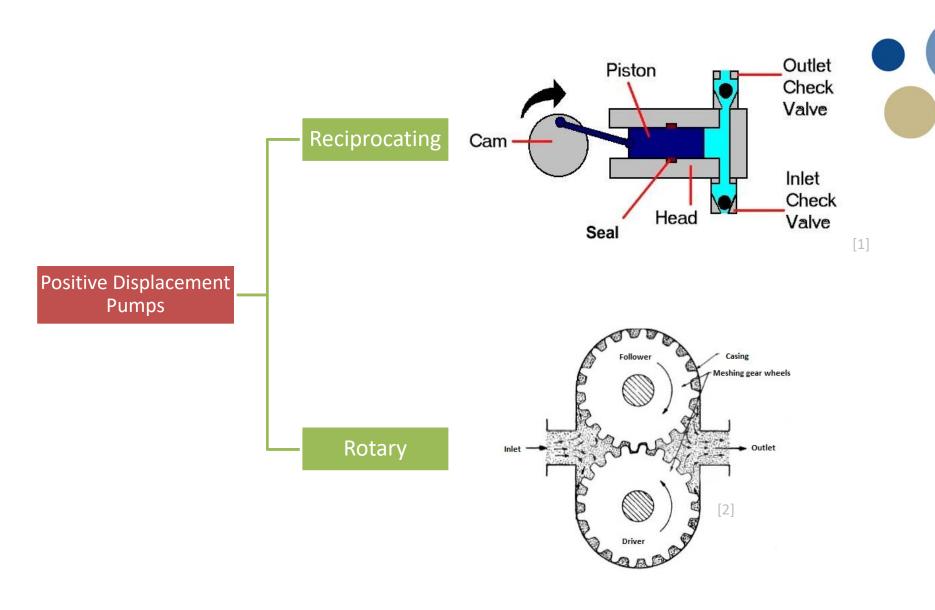
- https://www.globalspec.com/learnmore/flow\_control\_flow\_transfer/pumps/impellers [1]
  - https://www.ksb.com/centrifugal-pump-lexicon/specific-speed/191172/



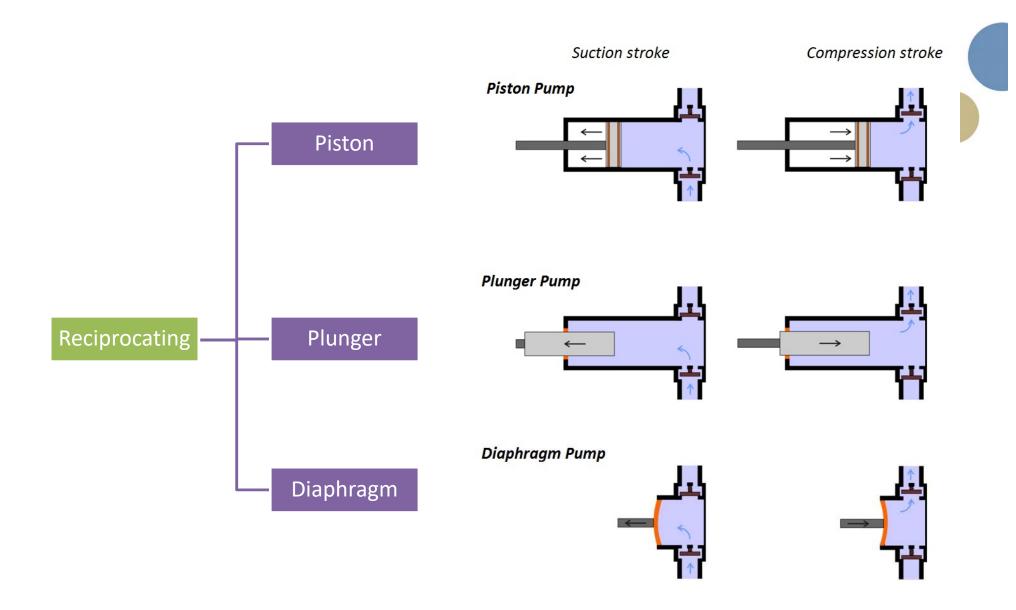
#### Dynamic Pumps

Special-effects

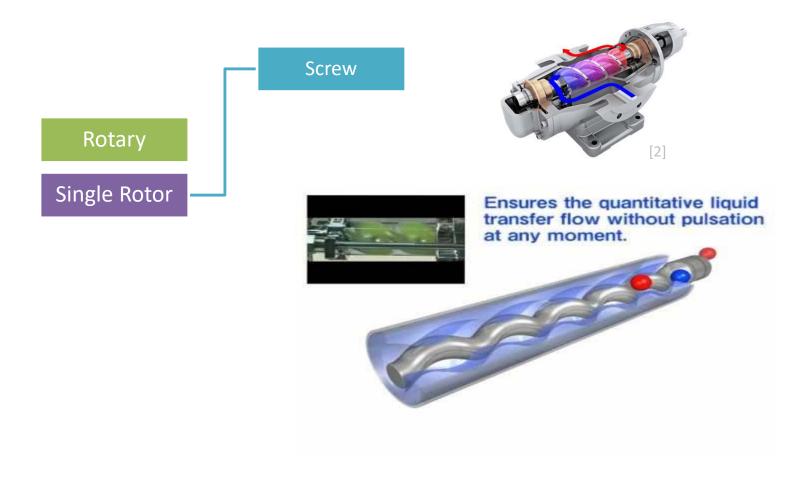




- [1] http://marinersgalaxy.com/what-is-reciprocating-pump-and-how-i/
- [2] https://www.brighthubengineering.com/marine-engines-machinery/41121-working-principle-of-rotary-pumps/

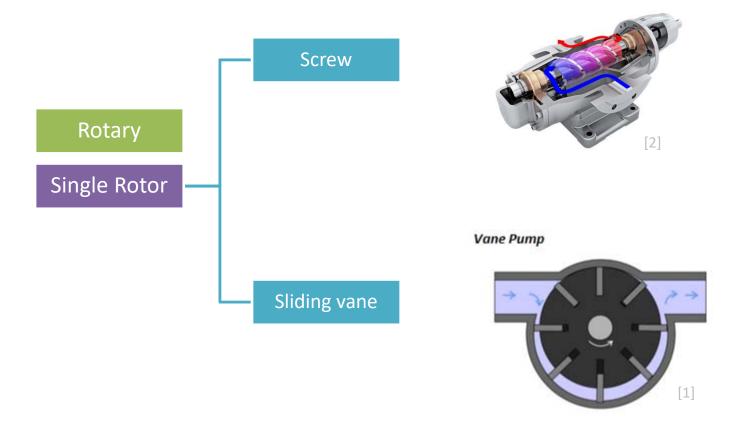




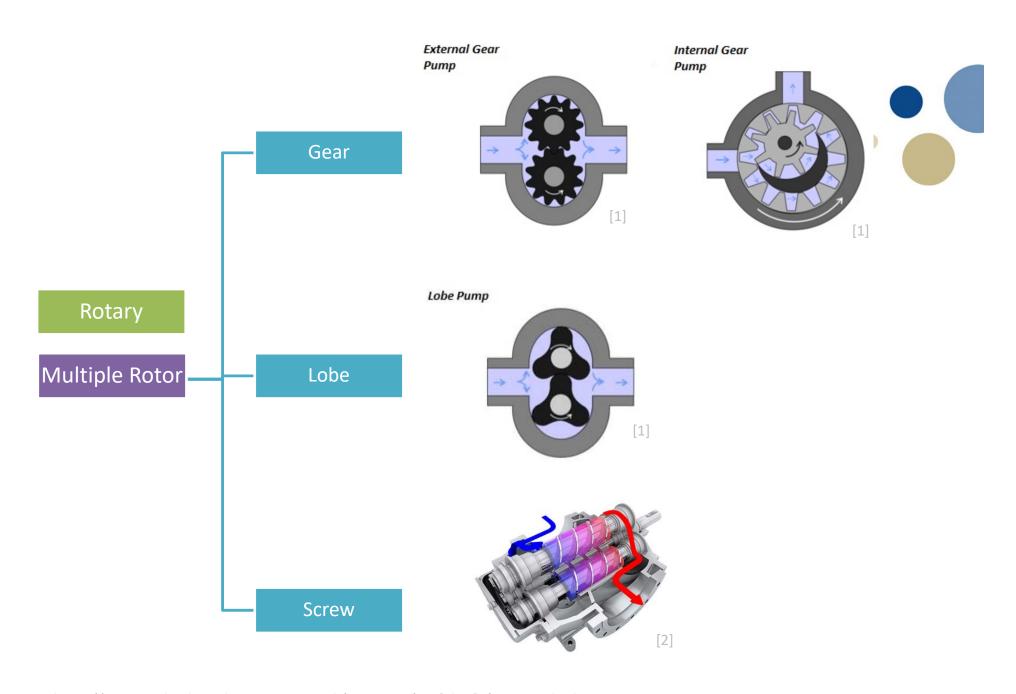


- [1] https://www.michael-smith-engineers.co.uk/resources/useful-info/positive-displacement-pumps
- [2] https://www.dynapumps.com.au/pressure-pumps/screw-pumps.aspx





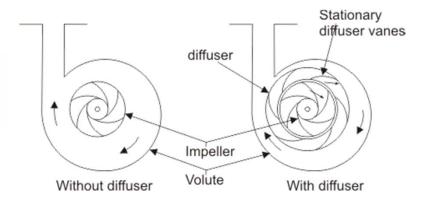
- [1] https://www.michael-smith-engineers.co.uk/resources/useful-info/positive-displacement-pumps
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 Shape of casing: volute, double volute, diffuser, annular, tubular, split casing, etc







• Inlet geometry: single suction, double suction, axial inlet, side inlet, top inlet, etc.





• Layout: horizontal shaft, vertical shaft, or inclined shaft





 Number of stages: for radial and mixed flow centrifugal pumps they can be classified as single-stage, double stage, or multiple stage

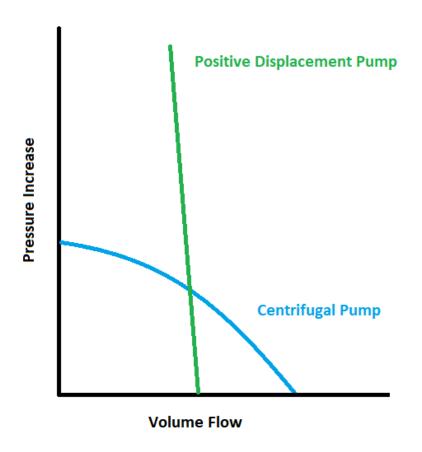


- Liquid handled (corrosive, abrasive, solid particles...)
- Material of pump parts: material used for manufacturing the impeller and pump casing
- Type of prime mover: electric motors, diesel engines, steam or gas turbines
- Discharge pressure: low pressure, high pressure, or high energy
- Operating conditions: submersibles pumps, wet motor pump, standby, and auxiliary pump:

# Determination of Flow Rate in a Pumping System

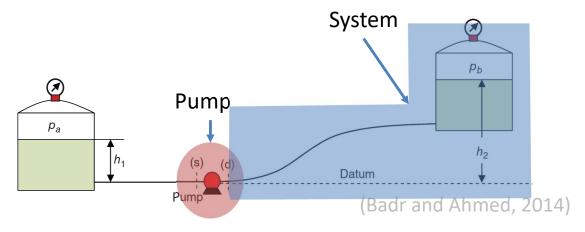
- The flow in a pump is determined by the relationship of the specified pump pressure increase to the backpressure (the resistance in the system)
- The pipe system has a characteristic curve
- The pump can only operate where the pump characteristic intersects the system characteristic
- The pump characteristics can be modified by adjusting the pump speed
- The system characteristics can be changed by opening or closing valves or changing levels in tanks

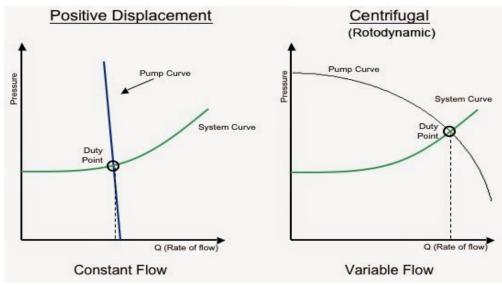
### Pump performance characteristics •



### System characteristic







http://www.hkdivedi.com/2015/05/difference-between-positive-and-non.html



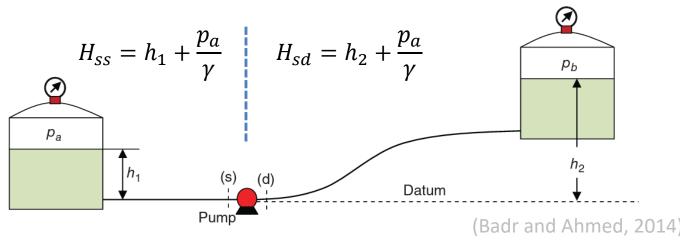
## **Rotodynamic Pumps**



 Pump Capacity (Q)/ displacement: express the actual volume flow rate delivered by the pump

#### 2. Pump Heads:

- Static suction head ( $H_{ss}$ ) pressure head at the suction nozzle at zero flow rate
- Static delivery head ( $H_{sd}$ ) pressure head at the delivery nozzle at zero flow rate
- Total static head  $(H_{st})$  difference between the  $H_{ss}$  and  $H_{st}$



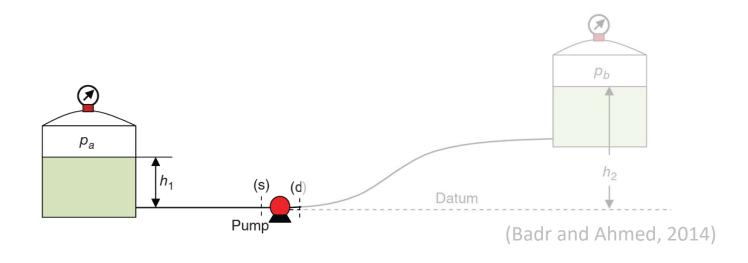


#### 2. Pump Heads:

– Pump suction head ( $H_s$ ): pressure head at the pump suction nozzle when the <u>pump is in operating condition</u>

$$H_S = h_1 + \frac{p_a}{\gamma} - \frac{V_S^2}{2g} - h_{LS}$$

 $h_{Ls}...$  friction head losses between the suction reservoir and the suction nozzle



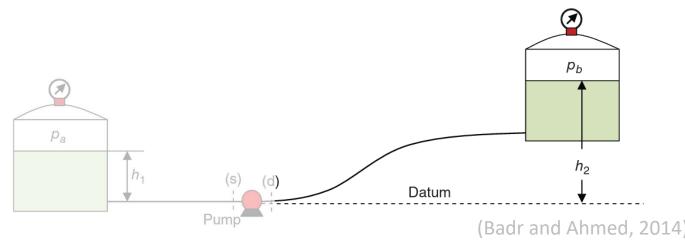


#### 2. Pump Heads:

- Pump suction head  $(H_s)$ : pressure head at the pump suction nozzle when the pump is in operating condition
- Pump delivery head ( $H_d$ ): pressure head at the pump delivery nozzle when the pump is in operating condition

$$H_d = h_2 + \frac{p_b}{\gamma} - \frac{V_d^2}{2g} + h_{Ld}$$

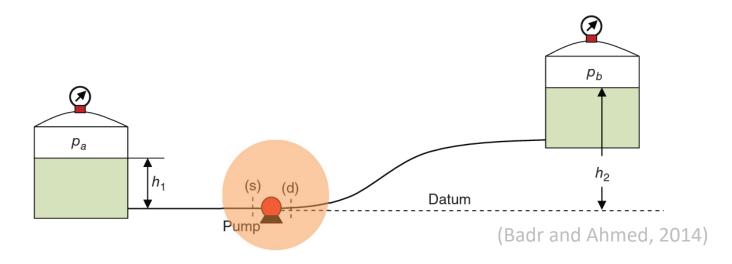
 $h_{Ld}...$  friction head losses between the delivery nozzle and the receiving tank



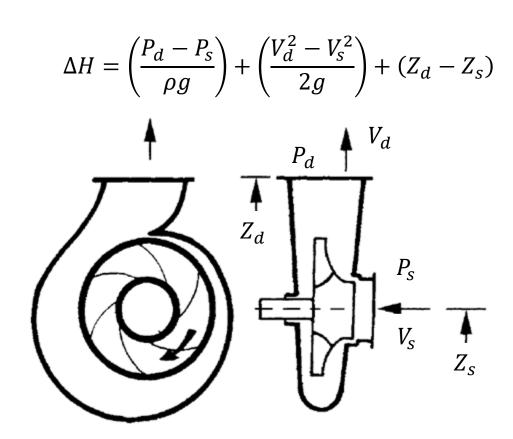


#### 2. Pump Heads:

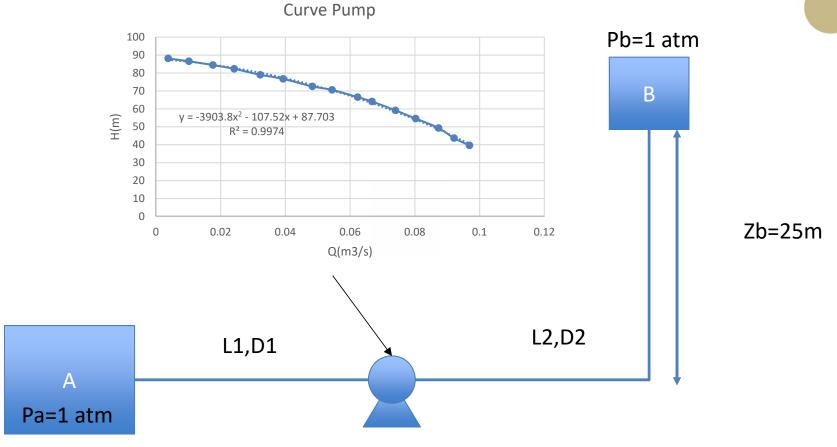
- Pump suction head ( $H_s$ ): pressure head at the pump suction nozzle when the pump is in operating condition
- Pump delivery head ( $H_d$ ): pressure head at the pump delivery nozzle when the pump is in operating condition
- Pump total head ( $\Delta H$ ): represents the energy added to the fluid by the pump (between the suction and delivery nozzles) per unit weight of fluid.



#### 2. Pump Heads:







L1=6.7cm D1=15cm

L2=205m

D2=15cm

 $h_{l \ minors} = 5.9m$ 

f=0.018

operating point??



System characteristic

$$\Delta H = H_d - H_s$$

Suction line

From A to Pump suction 
$$H_S = \frac{P_A}{\rho g} - \frac{V_S^2}{2g} - \Delta h_{l1}$$

Discharge line

From Pump discharge to B 
$$H_d = \frac{P_B}{\rho g} - \frac{V_d^2}{2g} + (Z_B - Z_d) + \Delta h_{l2}$$

$$\Delta H = H_d - H_s = \frac{P_B - P_A}{\rho g} + \frac{V_s^2 - V_b^2}{2g} + (Z_B - Z_d) + \sum \Delta h_l$$

$$\Delta H = (Z_B - Z_d) + \sum \Delta h_l$$



**Head losses** 

$$\sum \Delta h_l = \Delta h_{l1} + \Delta h_{l2} = \frac{fL_1 V_s^2}{2gD_1} + \frac{fL_2 V_d^2}{2gD_2} + h_{l \ minors}$$
 
$$\sum k \frac{V^2}{2g} = 5.9m$$

$$V_d^2 = V_S^2 = V^2 = \left(\frac{Q}{A}\right)^2$$

$$\sum \Delta h_l = 5093Q^2$$

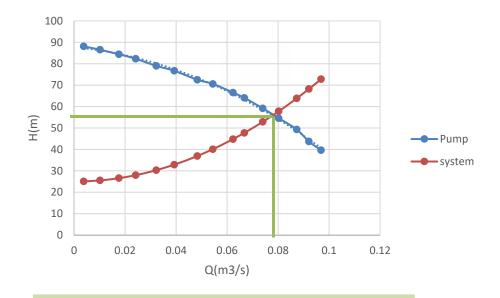
System Curve

$$\Delta H = (Z_B - Z_d) + \sum \Delta h_l = 25 + 5093Q^2$$



System Curve

$$\Delta H = (Z_B - Z_d) + \sum \Delta h_l = 25 + 5093Q^2$$

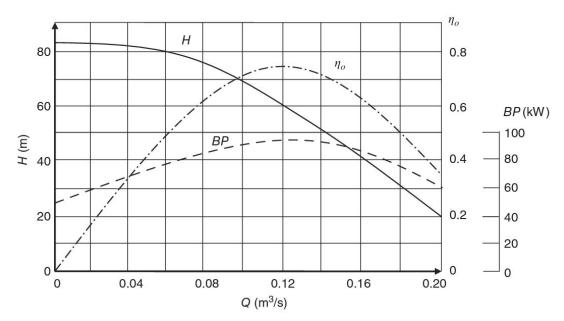


$$Q = 0.077 \, m^3/s$$
  $H = 56 \, m$ 



#### 3. Pump performance characteristics

- It refers to the relationship between each of the **total head (H)**, the **pump power consumption (BP)**, the pump overall **efficiency**  $(\eta_o)$ 



Typical performance curve for a radial-type centrifugal pump operating at a constant speed



(Badr and Ahmed, 2014)

#### 3. Pump performance characteristics

- Presented as a set of Iso-efficiency curves at:
  - Different speeds
  - Different size for geometrically similar pumps at constant speed

