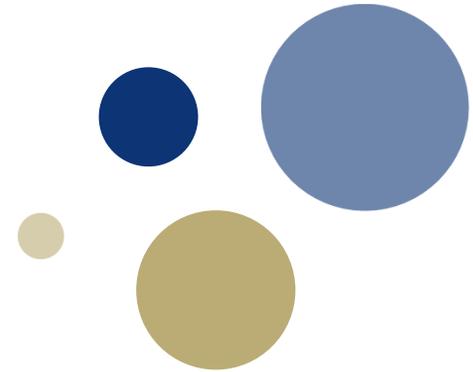




NTNU – Trondheim
Norwegian University of
Science and Technology



TPG 4135 Production Technology

Field Processing and Systems

Postdoc Mariana Díaz
01 /21/2019

Plan



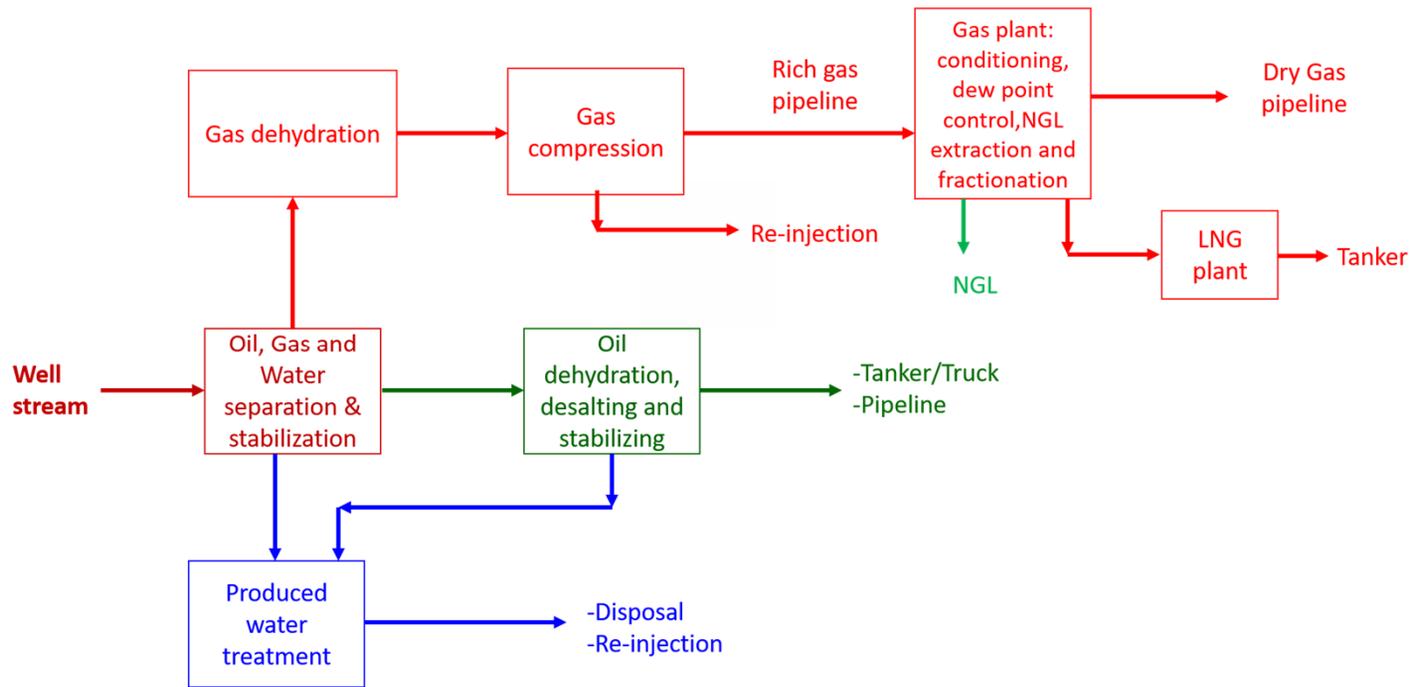
Week Nr.	Week starts	Topic	Lecturer
2	07.jan.19	Course introduction. Overview of field processing. Product specs.	MS
3	14.jan.19	Oil-Gas sep (VLE), Rachford Rice, EOS calculations.	MS
4	21.jan.19	Oil-Gas Separation . Introduction to process simulation (Hysys).	MD
5	28.jan.19	Oil-Gas Separation. Bubble and droplet dynamics. Separation capacity.	MD
6	04.feb.19	Oil-water separation	MD
7	11.feb.19	Water content in Natural gas. Gas dehydration (TEG)	MS
8	18.feb.19	Gas dehydration (TEG)	MS
9	25.feb.19	Pressure calculations in pipe (single and two-phase)	HA
10	04.mar.19	Pressure calculations in pipe (single and two-phase)	HA
11	11.mar.19	Heat transfer, pipe calculations, heat exchangers	HA
12	18.mar.19	Heat transfer, pipe calculations, heat exchangers	HA
13	25.mar.19	Pumping	MD
14	01.apr.19	Pumping/Compression	MD/HA
15	08.apr.19	Compression	HA
16	15.apr.19	Påskeferie	-
17	22.apr.19	Compression (probably one lecture only)	HA
18	29.apr.19	Spørretime	All

Monday: 12:15-14:00 (P12 PTS)
 Tuesday: 14:15-16:00 (VG13 NHL)
 Exercise: 16:15-18:00

Exam: 29.05, 15:00-19:00

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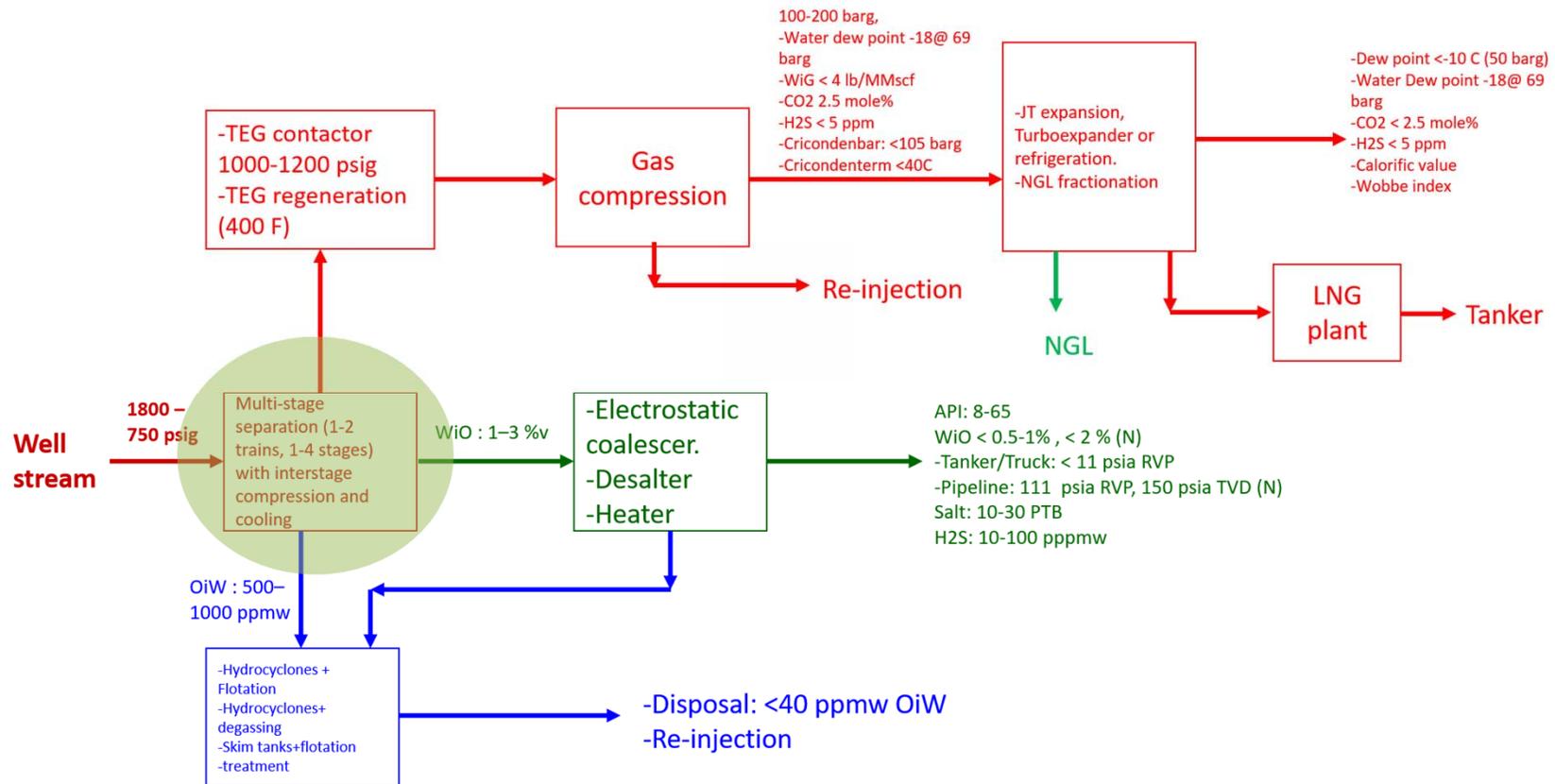
Processing Block Diagram



Stanko Milan (2018)

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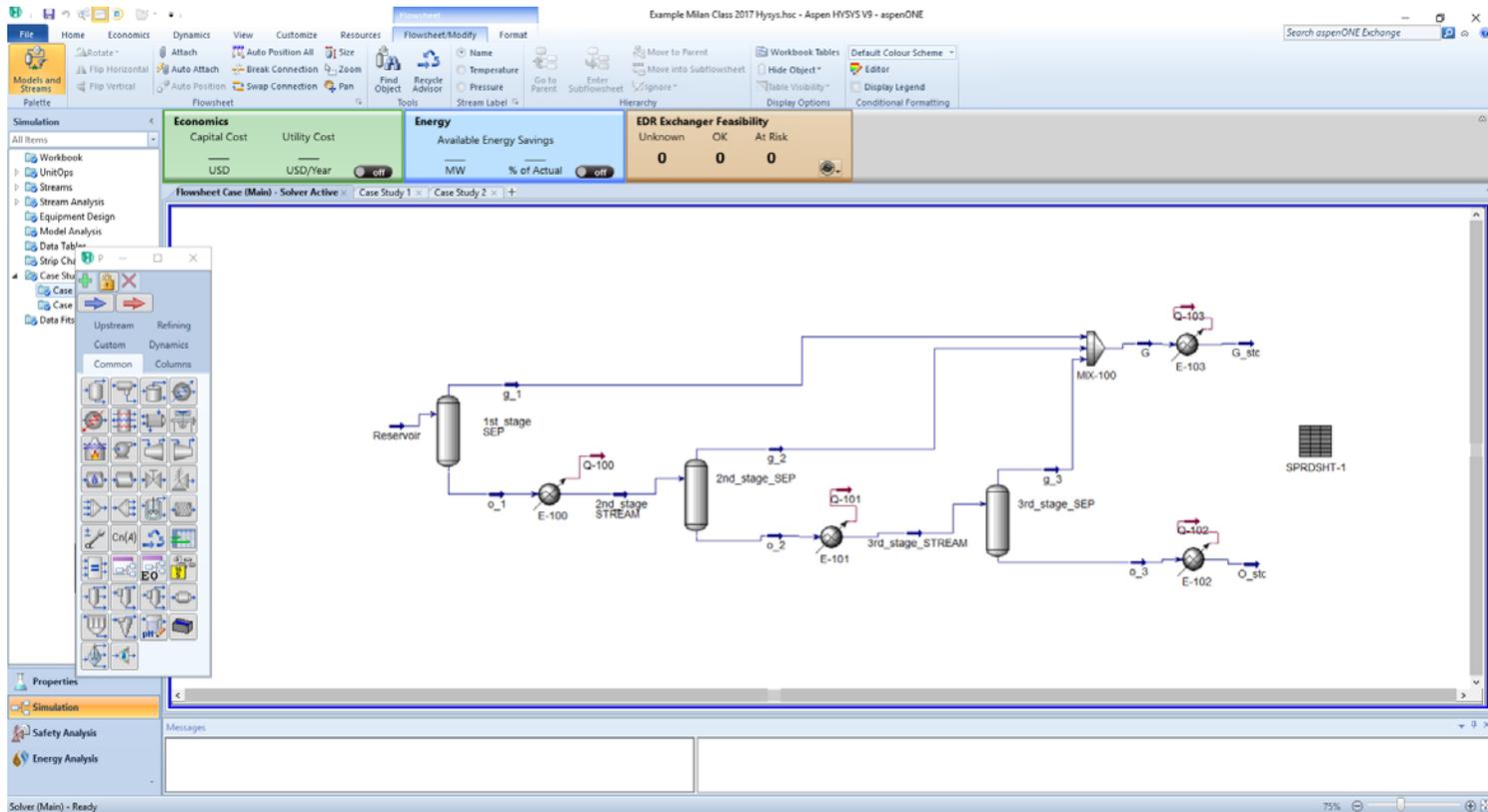
Processing Block Diagram



Stanko Milan (2018)

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PROCESS SIMULATION HYSYS



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PROCESS SIMULATION HYSYS



Example Milan Class 2017 Hysys.hsc - Aspen HYSYS V9 - aspenONE

File Home Economics Dynamics View Customize Resources Flowsheet/Modify Format

Simulation Economics Energy EDR Exchanger Feasibility

Capital Cost	Utility Cost	Available Energy Savings	Unknown	OK	At Risk	
USD	USD/Year	MW	% of Actual	0	0	0

Flowsheet Case (Main) - Solver Active x Case Study 1 Case Study 2 x

Reservoir

Q-103
G G_stc
E-103

Q-102
O_3 O_stc
E-102

SPRDSHT-1

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Properties Simulation Safety Analysis Energy Analysis

Solver (Main) - Ready 75%

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PROCESS SIMULATION HYSIS



Webpage for RemoteApps

NTNU
Norwegian University of Science and Technology

RemoteApps

Help

User name:

Password:

Security ([show explanation](#))

This is a public or shared computer

This is a private computer

Warning: By logging in to this web page, you confirm that this computer complies with your organization's security policy.

To protect against unauthorized access, your RD Web Access session will automatically time out after a period of inactivity. If your session ends, refresh your browser and sign in again.

For non-Windows clients we recommend the installation of MS Remote Desktop:

Mac computer: iPad/iPhone: Android phone & pad: Linux:

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Current folder: /Scientific

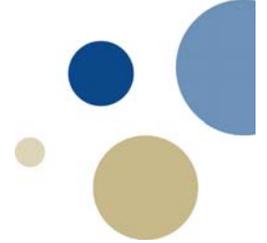
Up	AIM-Spice 6.0 [C]	ANSYS AqwaGS 19.1 [C]	ANSYS CFD-Post 19.1 [C]	ANSYS CFX 19.1 [C]	ANSYS Fluent 19.1 [C]	ANSYS ICEM CFD 19.1 [C]	ANSYS Icepak 19.1 [C]	ANSYS Mechanical APDL 19.1 [C]	ANSYS Polyflow 19.1 [C]
ANSYS SpaceClaim 19.1 [C]	ANSYS Workbench 19.1 [C]	Aspen Energy Analyzer V9 [C]	Aspen HYSYS V9 [C]	Aspen Plus V9 [C]	Cain [C]	CASAnova [C]	Ceetron 3D Viewer (64 bit) [C]	ChemBio3D Ultra 14.0 [C]	ChemBioDraw Ultra 14.0 [C]
ChemBioFin... Jltra 14.0 [C]	CMG Launcher 2013.10 [C]	CoolPack [C]	Cytoscape [C]	DelftShip [C]	fap2D 4.1 [C]	Fiji [C]	GLview Inova (64 bit) [C]	GLview Report Builder (64 bit) [C]	HEC-RAS 5.0.3 [C]
HSC 9 [C]	LISREL 9.30 Student [C]	Neuron Studio [C]	OlyVIA [C]	ReluxPro [C]	S3GRAF V7.2 [C]	Schlumberger Simulation Launcher [C]	Sensor6k Cmd [C]	SIMIEN [C]	SOLIDW... 2017 x64 Edition [C]
SOLIDWORKS Electrical	Spartan '14 [C]	SSIIM 1 [C]	SSIIM 2 [C]	TESS 2.3.1 [C]	UniSim Design R460	UniSim ThermoWor... R460	VMGSim [C]	WinEEG [C]	

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Mac computer: iPad/iPhone: Android phone & pad: Linux:

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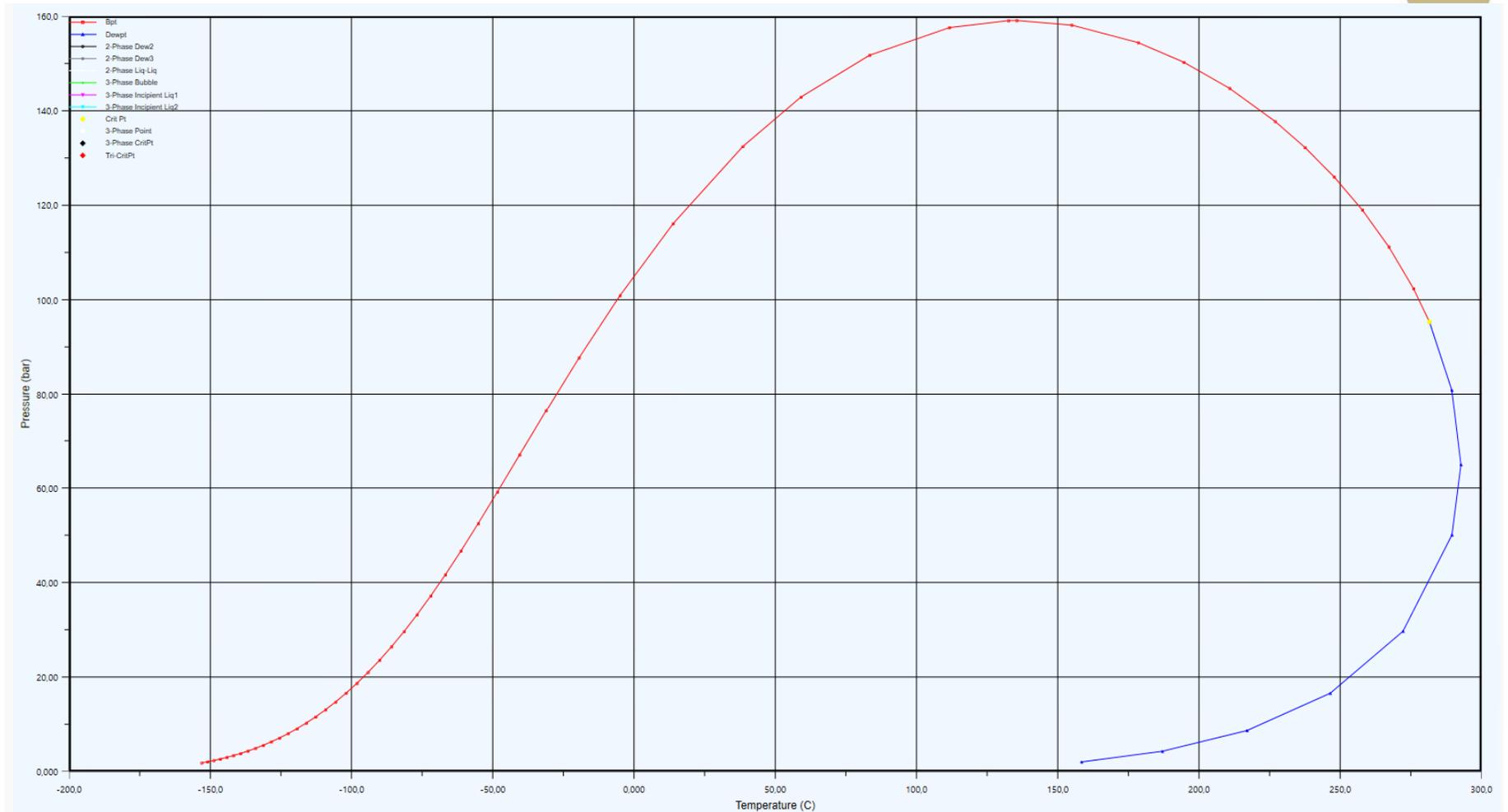
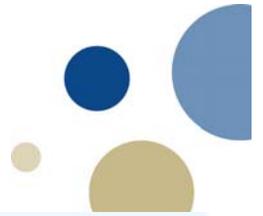
Fluid Composition 1



	T (C)	P (bar)
Stage 1	75	65
Stage 2	65	20
Stage 3	60	2
Standard Conditions	15.66	1.01325

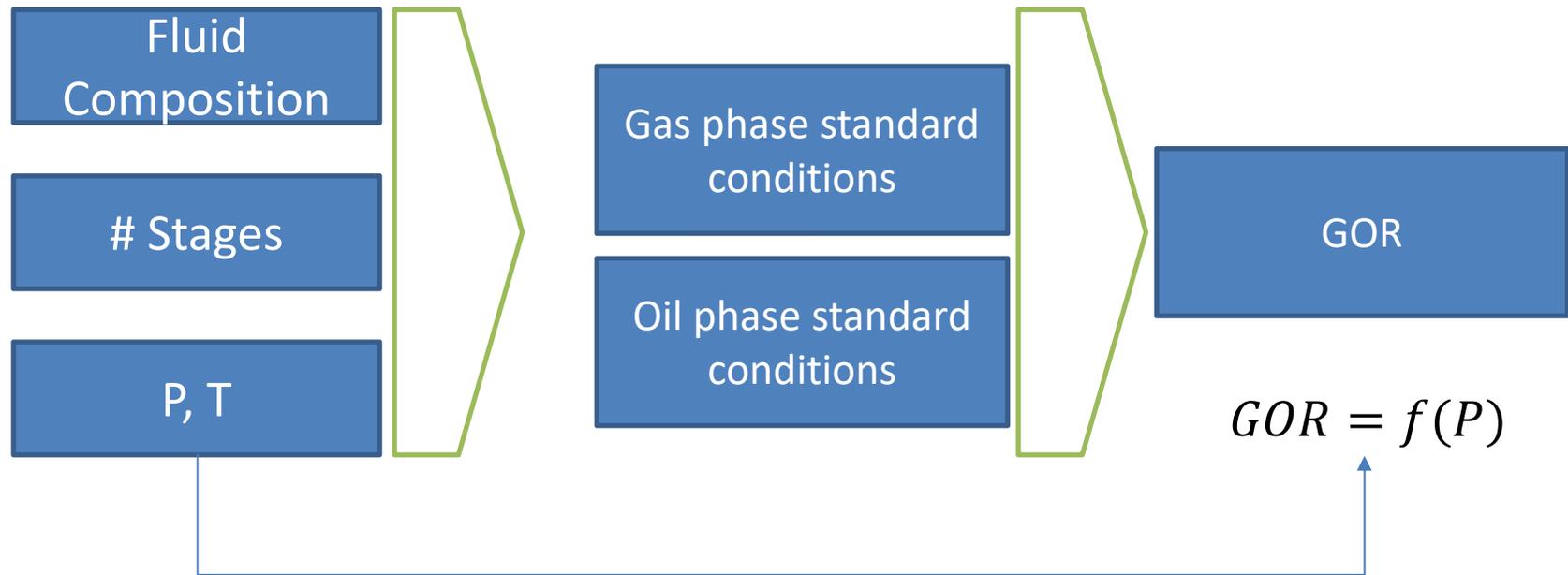
Component	Mole Fraction
Nitrogen	0.003672
CO2	0.001092
Methane	0.429256
Ethane	0.046897
Propane	0.029618
i-butane	0.014919
n-butane	0.009325
i-pentane	0.008446
n-pentane	0.005030
Hexanes	0.018433
Heptanes	0.041418
Octanes	0.049891
Nonanes	0.038403
Decanes	0.303600

Fluid Composition



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Summary



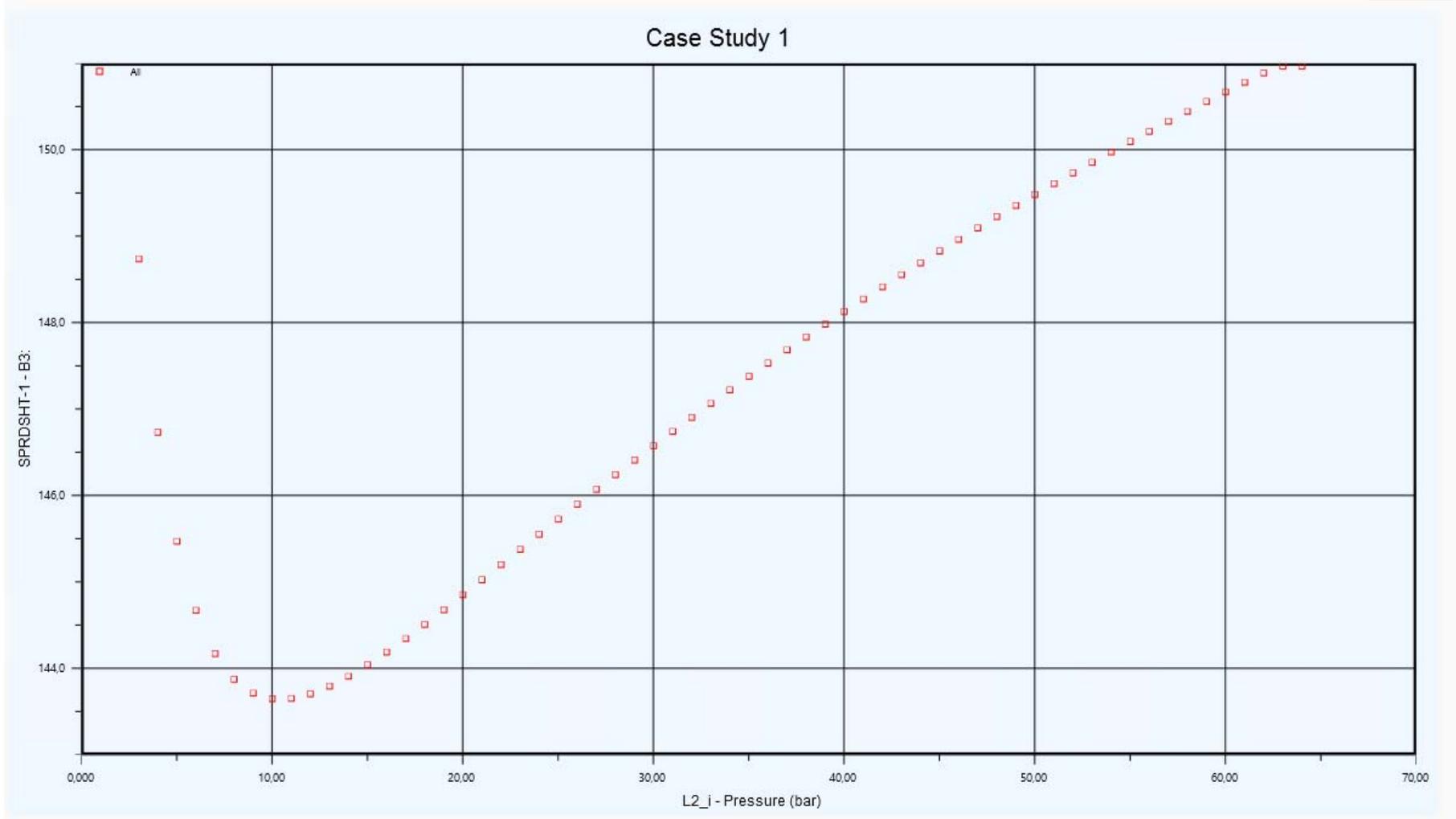
GOR calculation



Imported Variables

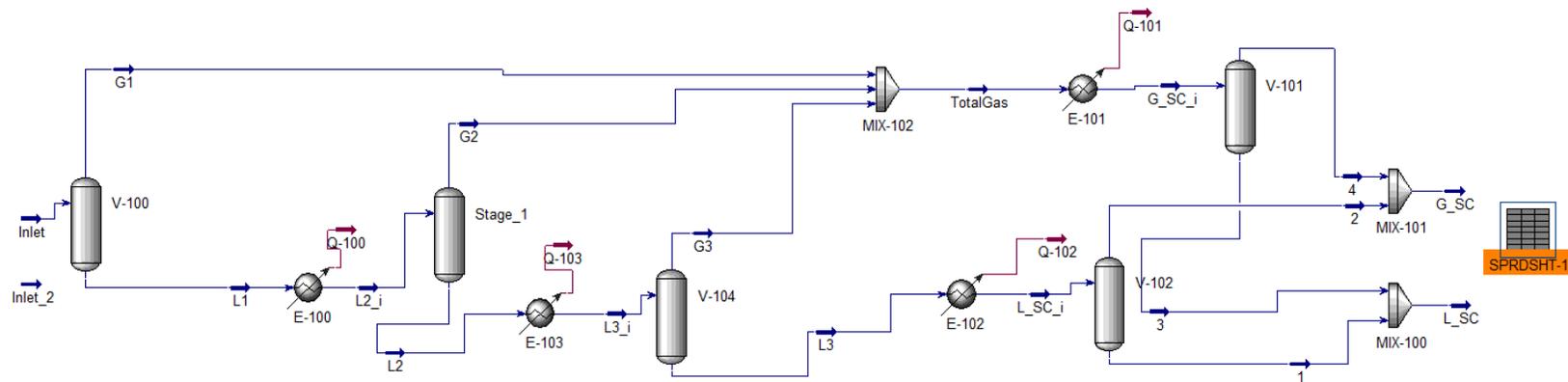
Cell	Object	Variable Description
B1	G_SC	Phase Actual Volume Flow (Vapour Phase)
B2	L_SC	Phase Actual Volume Flow (Liquid Phase)
C1	G_SC_j	Phase Actual Volume Flow (Vapour Phase)
C2	L_SC_j	Phase Actual Volume Flow (Liquid Phase)

Summary



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Summary



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Exercises



1. Change the number of stages: 1, 2 and 4 stages
2. Propose the temperature and pressure of the 3rd stage such the GOR is minimum when using 3 stages
3. Compare the liquid recovery at the end of the separation train for 1, 2 and 3 stages. Create a plot like Figure 1 for each case
4. Change the composition (Table 1)
5. Sensibility analysis of the first stage, P (80 to 30)

Table 1

Nitrogen	0.0024005
CO2	0.0157031
Methane	0.8687738
Ethane	0.0560112
Propane	0.0212042
i-Butane	0.0029006
n-Butane	0.0065013
i-Pentane	0.0020004
n-Pentane	0.0026005
n-Hexane	0.0032006
n-Heptane	0.0023005
n-Octane	0.0024005
n-Nonane	0.0018004
n-Decane	0.0122024

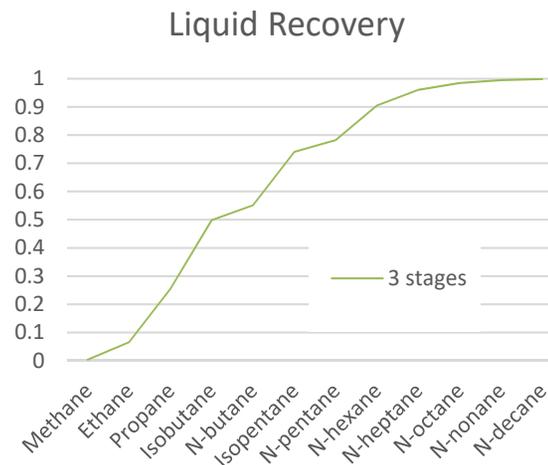


FIGURE1