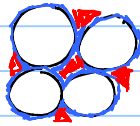


Water content in natural gas

Gas is always saturated with water @ a given P, T



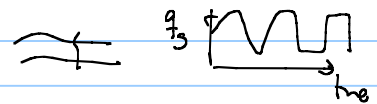
with P, T changes along the production system, water solubility in gas will change

typically with $P \downarrow, T \downarrow$ solubility is decreased $\leadsto$ water comes out of solution (free water)

can cause some issues

we need a way to estimate expected free water / water content in gas at any position of production system

- corrosion
- hydrates
- slugging (in transportation pipelines)



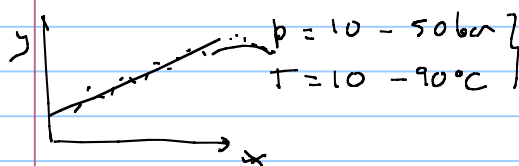
• scale

Correlations

EOS

equation of state

mathematical expressions
derived from measurements
in lab / field
often not based in physics



- ↳ not so accurate "out of the box"
- ↳ more general for wide range of conditions
- ↳ are usually customized with experimental data (by adjusting the default BIPs)

$$A = \sum_{i=1}^N \sum_{j=1}^N z_i \cdot z_j \cdot (1 - BIP_{ij}) \cdot \sqrt{A_i \cdot A_j}$$

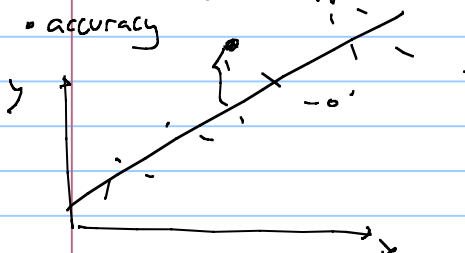
• advantages

- easy to use
- low computational expenses

for more information read section 9.3 of chapter 9
Whitson's monograph

• disadvantages

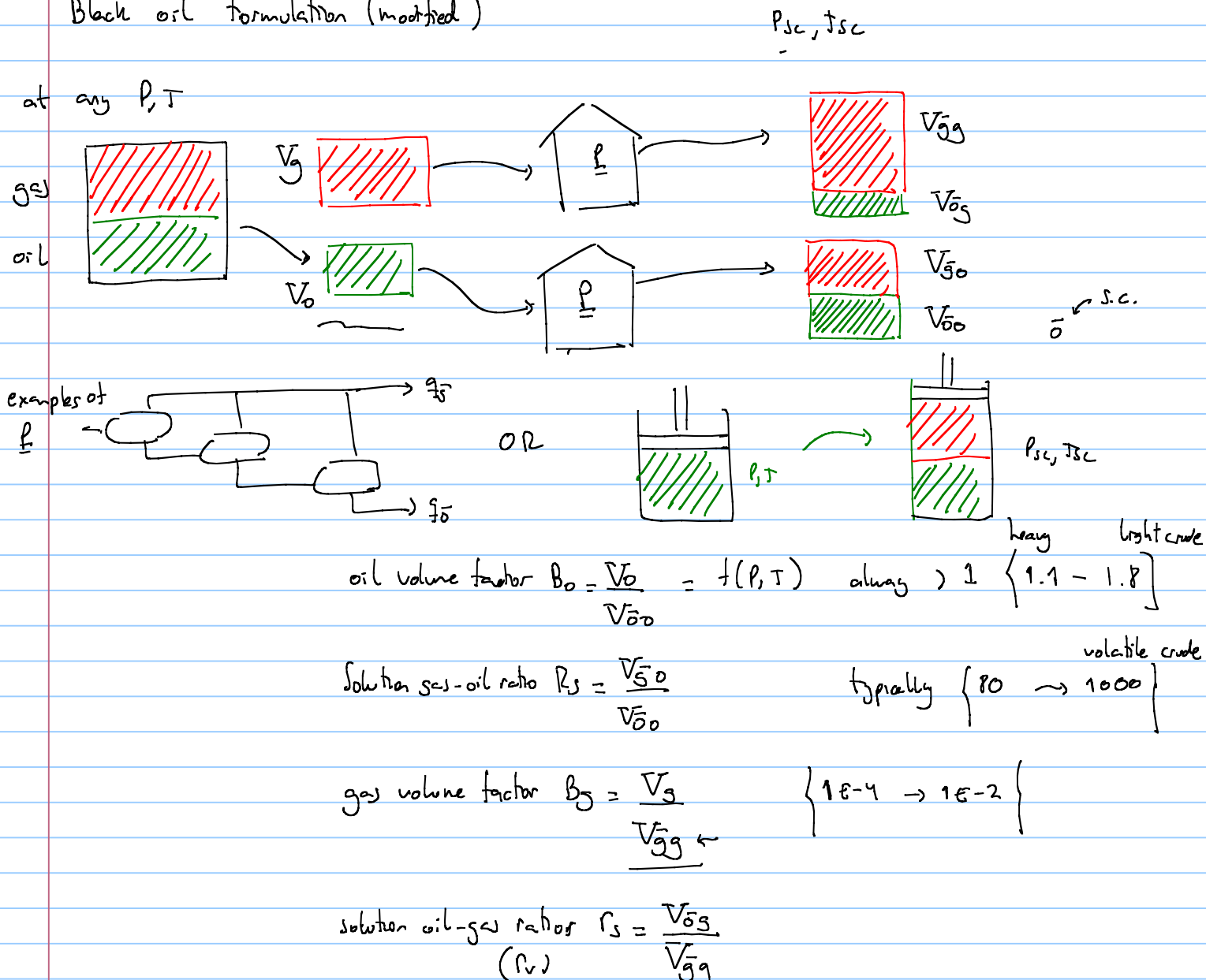
- limited range of applicability
- accuracy



Type of System	Recommended Property Method
TEG Dehydration	PR
Sour Water	PR, Sour PR
Cryogenic Gas Processing	PR, PRSV
Air Separation	PR, PRSV
Atm Crude Towers	PR, PR Options, GS
Vacuum Towers	PR, PR Options, GS (<10 mm Hg), Braun K10, Esso K
Ethylene Towers	Lee Kesler Plucker
High H ₂ Systems	PR, ZJ or GS (see T/P limits)
Reservoir Systems	PR, PR Options
Steam Systems	Steam Package, CS or GS
Hydrate Inhibition	PR
Chemical systems	Activity Models, PRSV
HF Alkylation	PRSV, NRTL (Contact Hyprotech)
TEG Dehydration with Aromatics	PR (Contact Hyprotech)
Hydrocarbon systems where H ₂ O solubility in HC is important	Kabadi Danner
Systems with select gases and light hydrocarbons	MBWR

Correlations are built following the same principle as Black oil properties

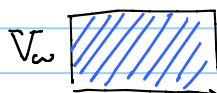
Black oil formulation (modified)



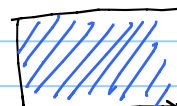
- BO properties are usually generated:
- by lab measurements
 - correlations (e.g. Glasø, Standing)
 - Use EOS simulator

for water, a similar approach is used

@ P, T



@ P_{sc}, T_{sc}



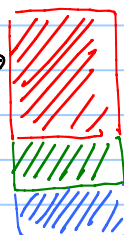
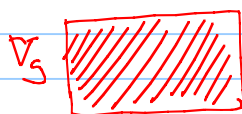
V_w



water volume factor

$$B_w = \frac{V_w}{V_w} \quad \text{due to compressibility of water}$$

$$B_w > 1$$



V_{sg} → 20 E6 m³/d

V_{og}

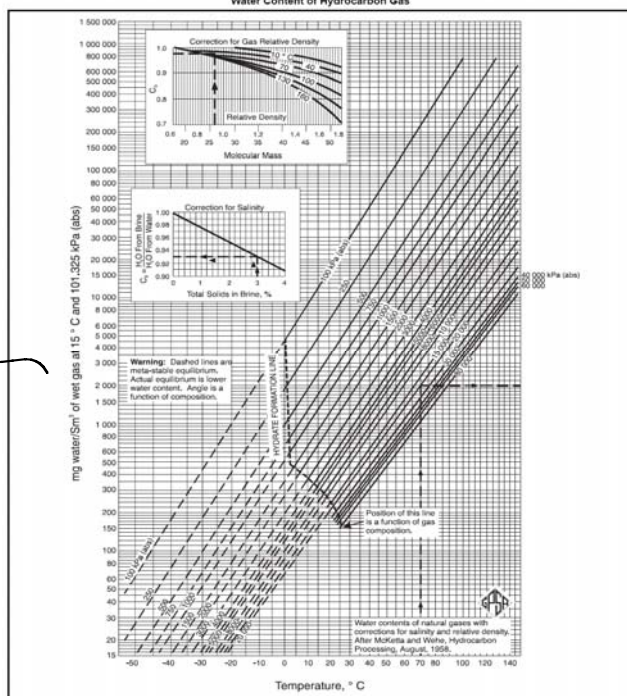
V_{wg}

V_{wg}

solution water-gas ratio

$$r_{sw} = \frac{V_{wg}}{V_{sg}}$$

FIG. 20-4
Water Content of Hydrocarbon Gas



$$r_{sw} = \frac{\text{m}^3}{\text{m}^3} \rightarrow \frac{\text{m}^3}{[\text{m}^3]}$$

$$r_{sw} = \frac{\rho_w}{\rho_g} \rightarrow \frac{\text{kg}}{[\text{m}^3]}$$

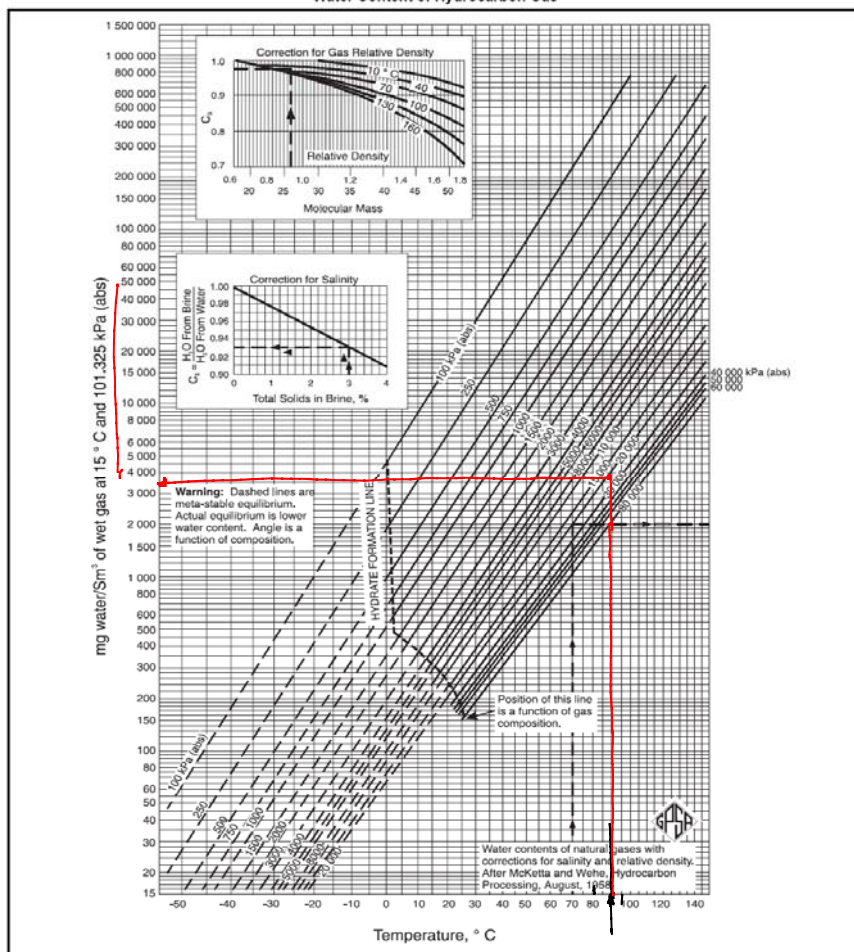
1000 kg/m³

Prof. Milan Stanko. TPG4135 - Water content in gas field

Gas MW	16 [Kg/Kmol]			
Gas gravity	0.552			
Water salinity	0.0 [ppm]			
CO2	0.0 [mole %]			
H2S	0.0 [mole %]			
Gas field rate	2.00E+07 [Sm ³ /d]			
Nwells	8			
Well gas rate	2.50E+06			
Location	p	T	rsw	qw
	[bara]	[C]	[Sm ³ /1E06 Sm ³]	[m ³ /d]
Reservoir	276	90		
Wellhead	160	70		
Choke downstream	120			
Separator	30	5		

@ P_R, T_R

FIG. 20-4
Water Content of Hydrocarbon Gas



20-5

$$P_R = 276 \text{ bara} \rightarrow 27600 \text{ kPa}$$

$$1 \text{ bar} = 1.05 \text{ Pa}$$

$$1 \text{ bar} = 100 \text{ kPa}$$

$$3500 \text{ mg/Sm}^3 = r_{sw} \cdot P_w$$

$$3.5 \frac{\text{kg}}{\text{Sm}^3} = r_{sw} \cdot P_w$$

$$r_{sw} = \frac{3.5 \text{ kg}}{1000 \left(\frac{\text{kg}}{\text{Sm}^3} \right) \cdot m^3}$$

$$r_{sw} = 3.5 \cdot 10^{-3} \frac{\text{Sm}^3}{\text{Sm}^3}$$

r_{sw} is typically expressed in

$$\frac{\text{Sm}^3}{1006 \text{ Sm}^3}$$

$$r_{sw} = 3.5 \cdot 10^{-3} \frac{\text{Sm}^3}{\text{Sm}^3} \cdot \frac{1006 \text{ Sm}^3}{[1006 \text{ Sm}^3]}$$

$$r_{sw} = 3500 \frac{\text{Sm}^3}{[1006 \text{ Sm}^3]}$$

It stands for Mega

$$q_w = q_g \cdot r_{sw}$$

$$q_w = 20 \left[\frac{\text{M Sm}^3}{\text{d}} \right] \cdot 3500 \left[\frac{\text{Sm}^3}{\text{M Sm}^3} \right] = 70000 \text{ Sm}^3/\text{d}$$