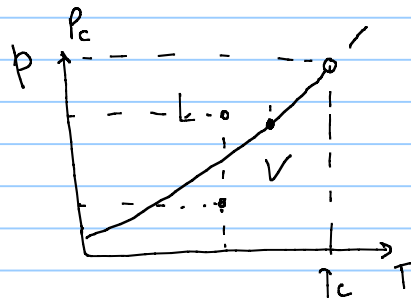


Class 3

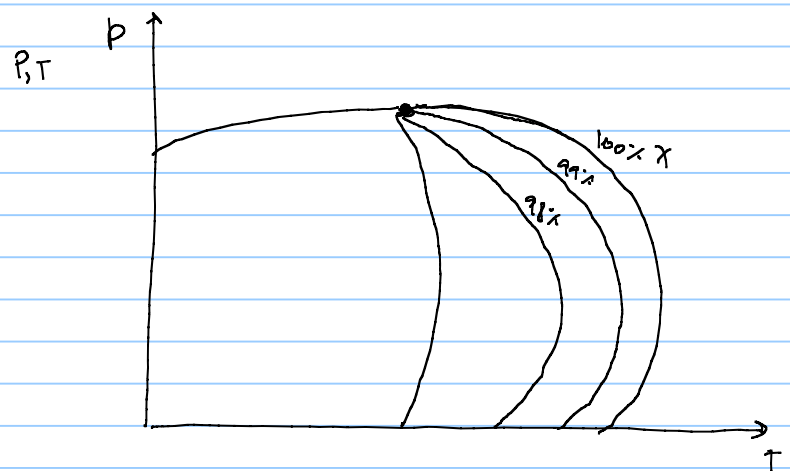
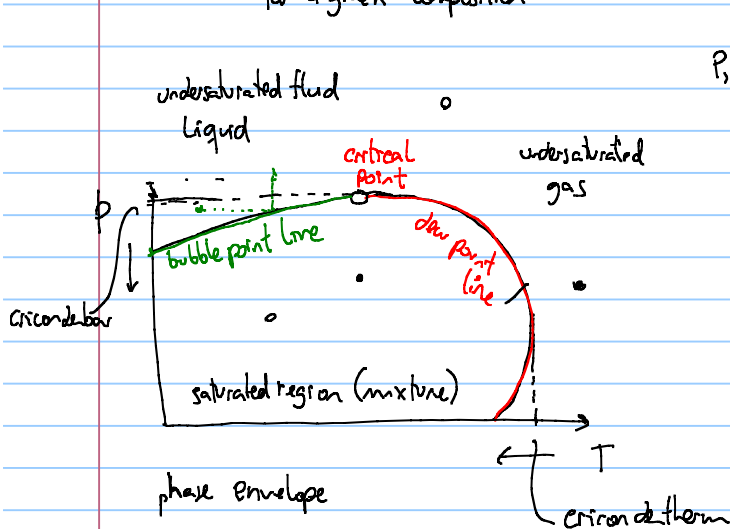
Phase diagram
pure component
/ single component



multicomponent
mixture

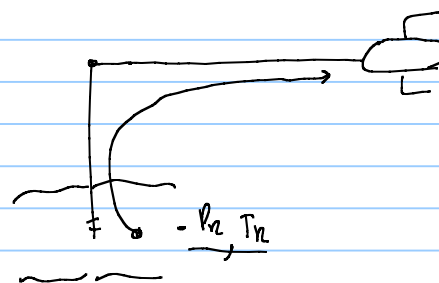
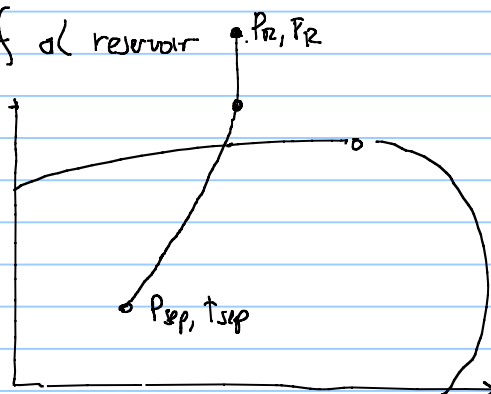


for a given composition

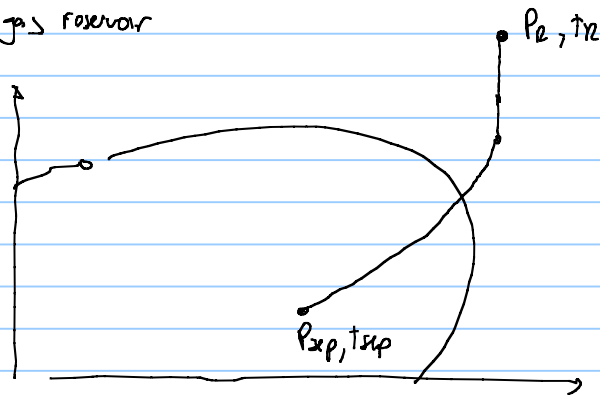


$$X = \frac{n_v}{n_T}$$

if a reservoir



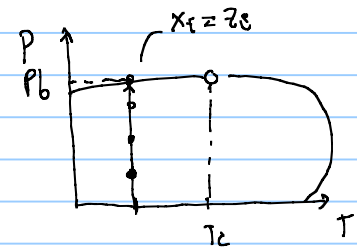
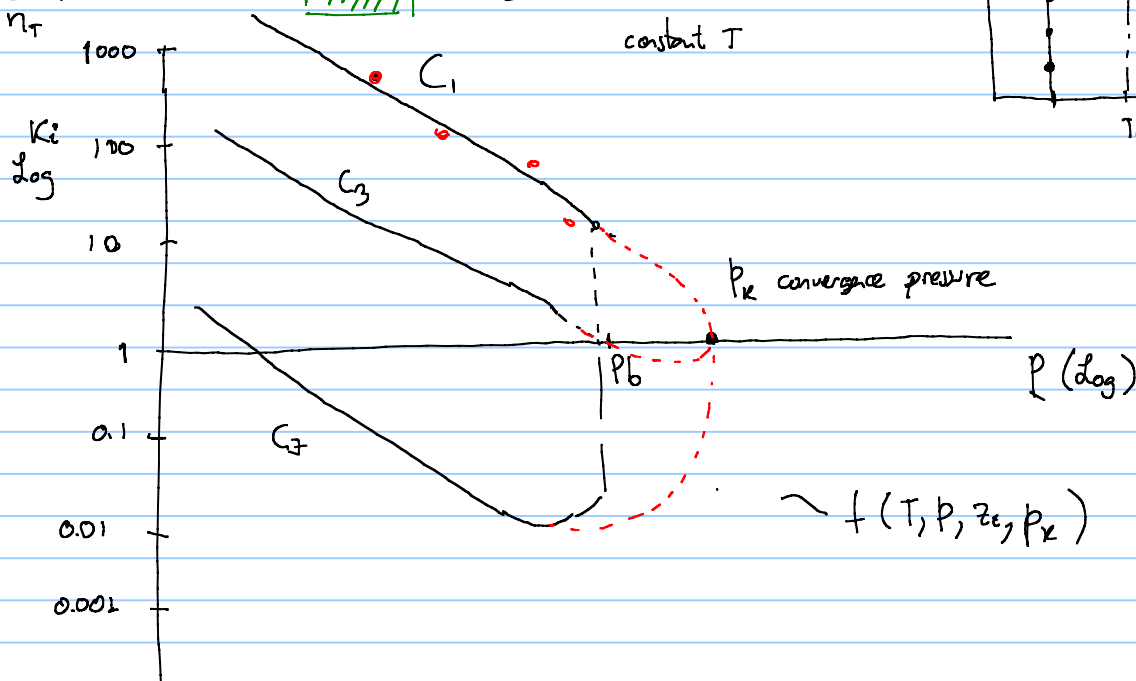
if gas reservoir



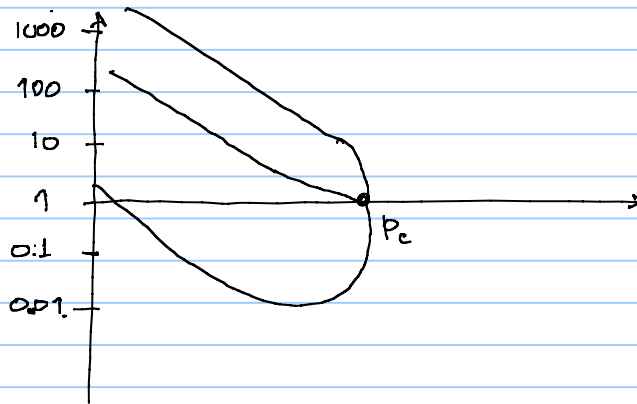
Methods for performing flash calculations
equilibrium

equilibrium ratio $K_i = \frac{y_i}{x_i}$
 ↑
 for component "i"

z_i {  $\frac{n_{c1}}{n_v} = y_{c1}$
 $z_{c1} = \frac{n_{c1}}{n_T}$  $\frac{n_{c1}}{n_L} = x_{c1}$



if the plot is made at T_c



Given p, T } K_i . $\begin{matrix} x_i \\ y_i \end{matrix}$ if N components $(2 \cdot N)$ unknowns

$$K_i = \frac{y_i}{x_i} \quad N \text{ equations}$$

$$\sum_{i=1}^N y_i = 1 \quad 1 \text{ eq}$$

$$\sum_{i=1}^N x_i = 1 \quad 1 \text{ eq}$$

$$\begin{matrix} z_i \\ \} \\ n_i \end{matrix} \quad \begin{matrix} y_i \\ \} \\ n_{vi} \end{matrix} \quad \begin{matrix} x_i \\ \} \\ n_{li} \end{matrix}$$

$$n_i = n_{vi} + n_{li}$$

divide
 n_T

$$\frac{n_i}{n_T} = \frac{n_{vi}}{n_T} + \frac{n_{li}}{n_T}$$

vapor fraction $\frac{n_v}{n_T} = f_v \rightarrow 0 \dots 1$

$$z_i = f_v \underbrace{\frac{n_{vi}}{n_v}}_{y_i} + \frac{n_{li}}{n_l} (1 - f_v)$$

$$n_T = \frac{n_v}{f_v}$$

$$\frac{n_l}{n_T} = (1 - f_v)$$

$$z_i = f_v y_i + x_i (1 - f_v)$$

N eq

1 unknown

	Unknowns	equation
$K_i = \frac{y_i}{x_i}$	$2 \cdot N$	N
$\sum y_i = 1$	0	1
$\vdots$		
$z_i = f_v y_i + (1 - f_v) x_i$	1	N
	$(2 \cdot N + 1)$	$2 \cdot N + 1$

Rachford - Rice

$$z_i = f_v y_i + (1 - f_v) x_i$$

$$k_i = \frac{y_i}{x_i}$$

$$y_i = k_i x_i$$

$$z_i = f_v k_i x_i + (1 - f_v) x_i$$

$$z_i = x_i \cdot (f_v k_i + 1 - f_v)$$

$$x_i = \frac{z_i}{f_v k_i + 1 - f_v}$$

$$\sum_{i=1}^N x_i = 1$$

$$\sum_{i=1}^N (y_i - x_i) = 0$$

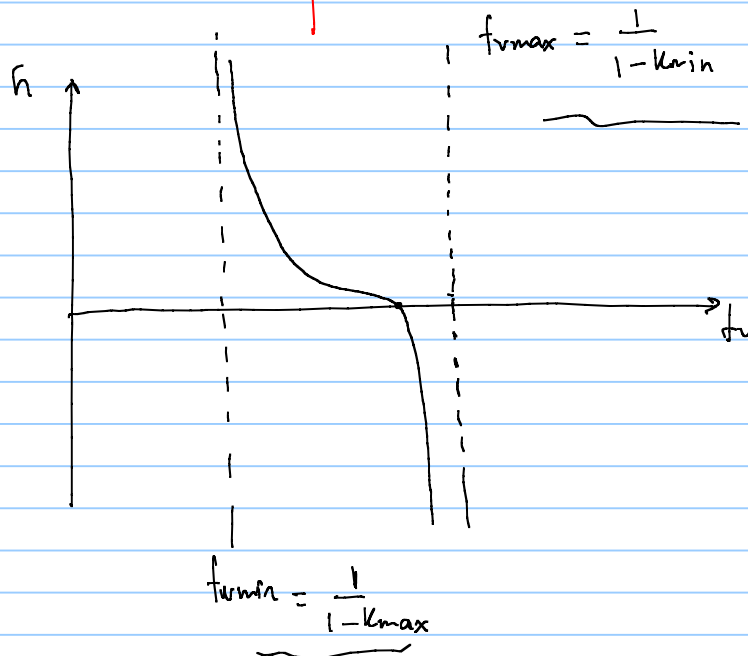
$$\sum_{i=1}^N y_i = 1$$

$$y_i = k_i x_i$$

$$\sum_{i=1}^N (k_i - 1) x_i = 0$$

$$(k_i - 1) x_i = \frac{(k_i - 1) z_i}{f_v k_i + 1 - f_v}$$

$$\sum_{i=1}^N (k_i - 1) x_i = 0 = \sum_{i=1}^N \frac{(k_i - 1) z_i}{f_v k_i + 1 - f_v} \quad h(f_v)$$



RR could give

$0 < f_v < 1$ in mixture

$f_v = 0$ saturated liquid

$f_v = 1$ saturated gas

$f_v < 0$ liquid

$f_v > 1$ undersaturated gas

EX: MULTISTAGE SEPARATION FLASH. By Prof. Milan Stanko (NTNU)

SEPARATION PROCESS

Stage	p	T	z-C1	z-C3	z-N-C10	x-C1	x-C3	x-N-C10	y-C1	y-C3	y-N-C10	f _v
[-]	bara	C	[-]	[-]	[-]	[-]	[-]	[-]	[-]	[-]	[-]	[-]
1-HP	50	70	0.5	0.2	0.3	0.07679	0.22803	0.69518	0.81955	0.17884	0.00162	0.56978
2-MP	35	50	0.07679	0.22803	0.69518							
3-LP	1.01325	15.56	0.00000	0.00000	0.00000							

COMPONENT PROPERTIES

Pk	[bara]	689	
Comp	T _c	p _c	AF (ω)
	[K]	[bara]	
C1	190.6	46.1	0.0115
C3	369.8	42.5	0.1454
N-C10	617.7	21.0	0.4902

FLASH CALCULATIONS

p	[bara]	50
T	[C]	70
	f _{vmin}	-0.103
	f _{vmax}	1.002
	f _v	0.5698

Comp	z _i	K _i (T)	RR_term	x _i	y _i
C1	0.5	10.6723	7.43E-01	0.07679	0.81955
C3	0.2	0.7843	-4.92E-02	0.22803	0.17884
N-C10	0.3	0.0023	-6.94E-01	0.69518	0.00162
	SUM=		-7.40E-09	1.00000	1.00000