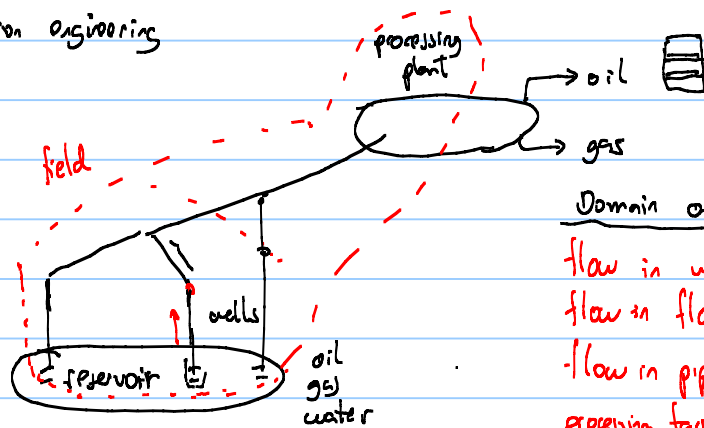


Prof. Milan Stanko NTNU → Norwegian university of science and technology

Production engineering

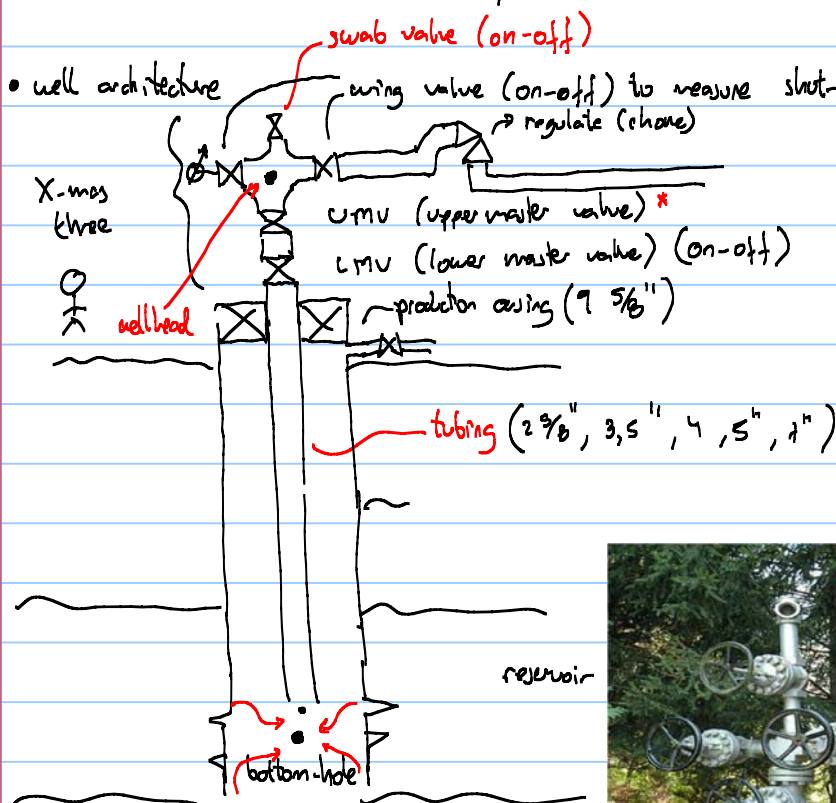


Domain of production engineering

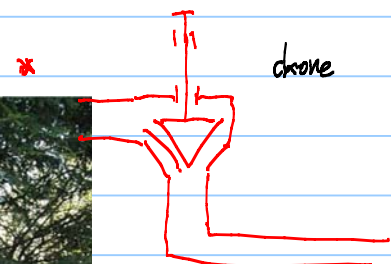
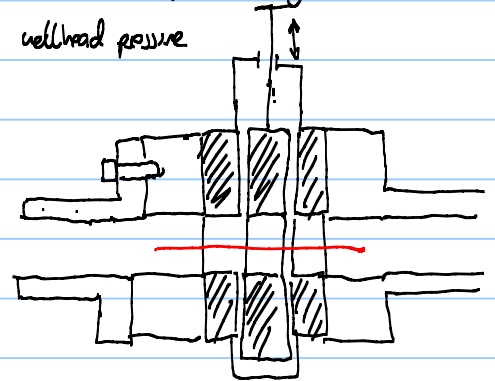
flow in wells (near wellbore formation)
 flow in flowlines } gathering system
 flow in pipelines
 processing facilities

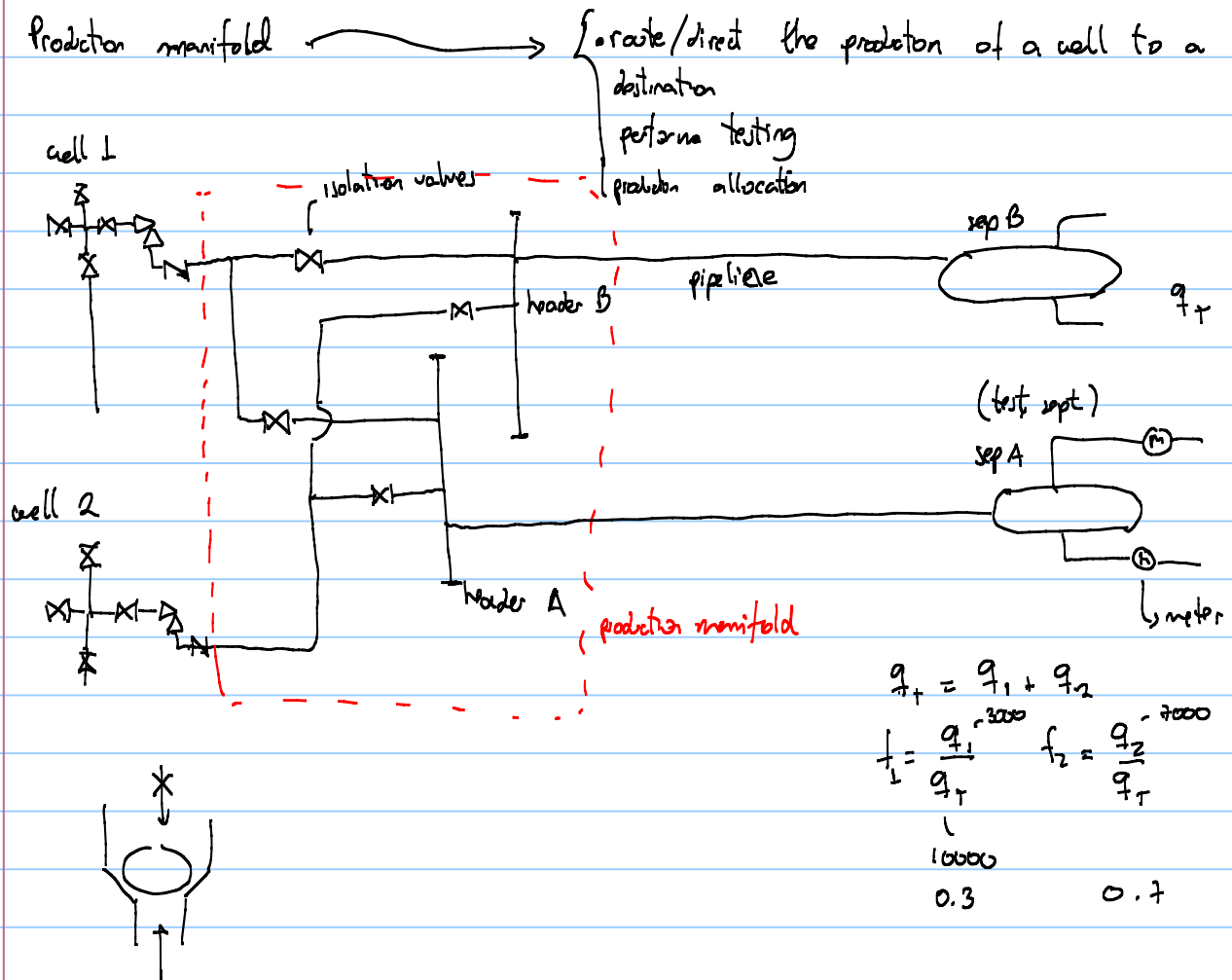
tasks of a production engineer are:

- to understand the subsurface { the reservoir {, production mechanism, productivity
- to manage the development { to produce reserves in a way that is economically viable
- to optimize the development { maximize revenue, reduce cost, reduce failures

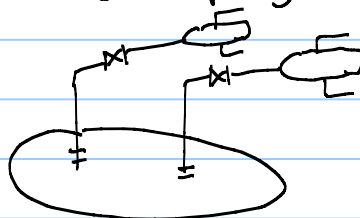


on-off are gate valves

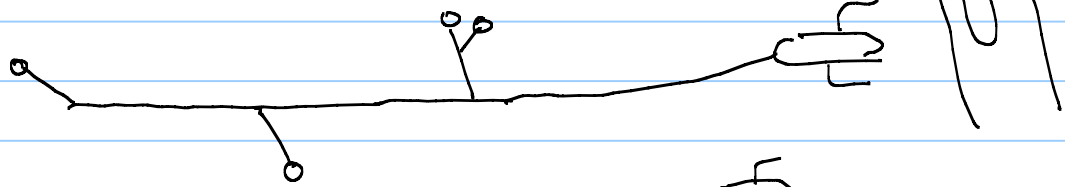




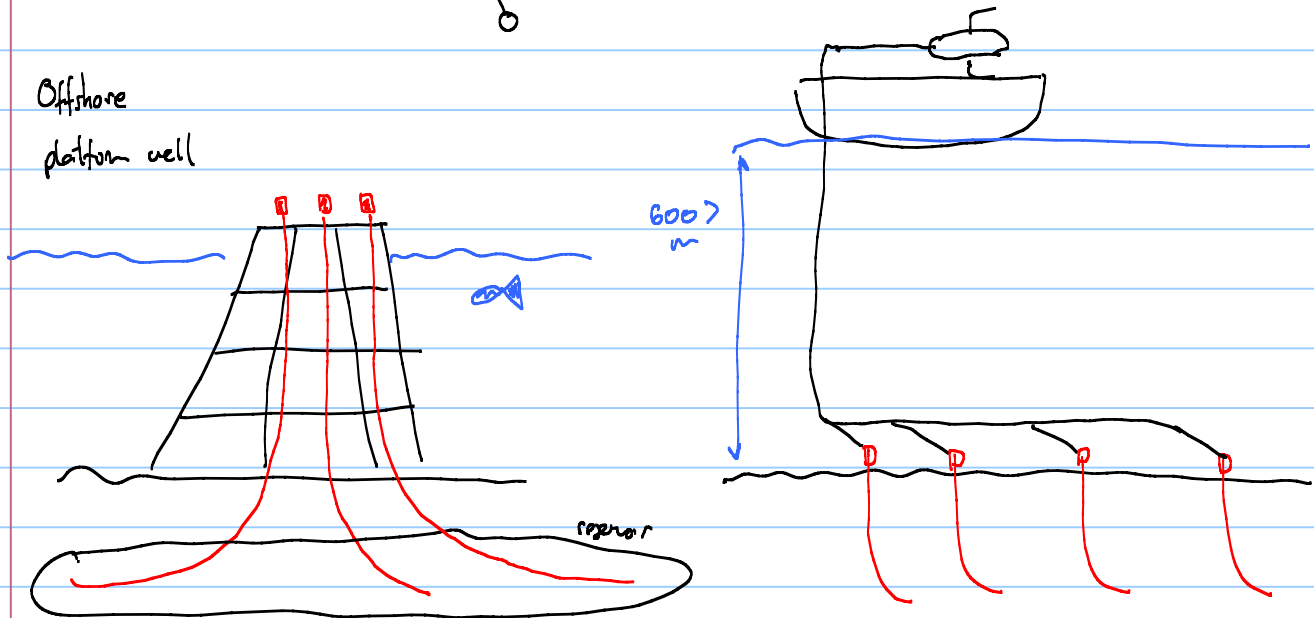
two types of wells : standalone → producing close to a separator
or pipeline is very short
such that $p_{header} \approx p_{sep}$



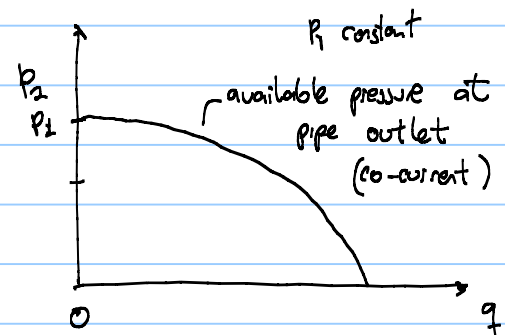
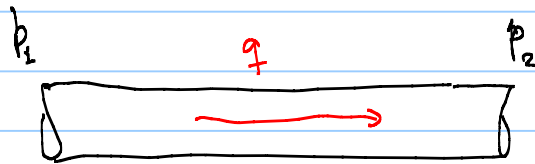
Wells in network \rightarrow separator is far away from wells
 \rightarrow pipeline collects production from many wells and transports to processing facilities



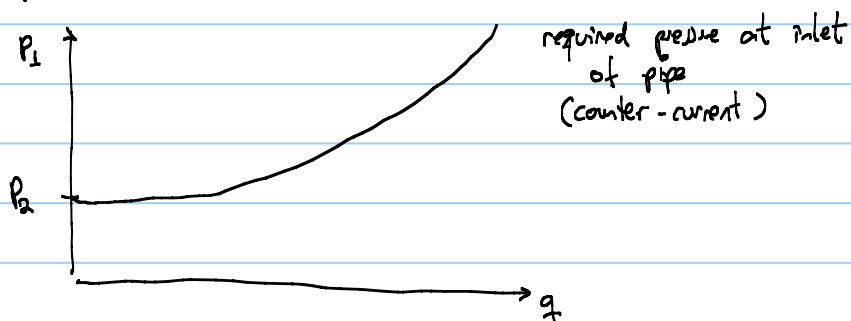
Offshore platform well

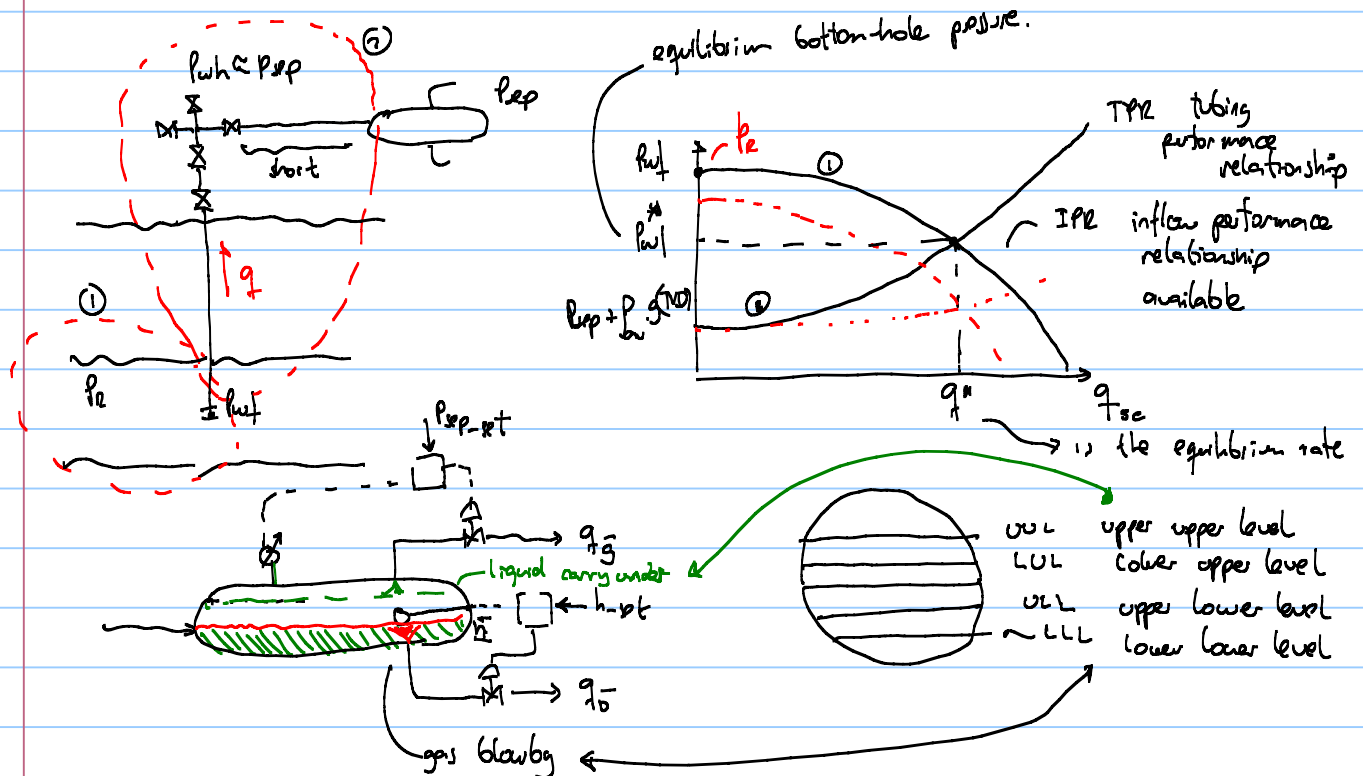


flow equilibrium (nodal analysis, inflow-outflow analysis)

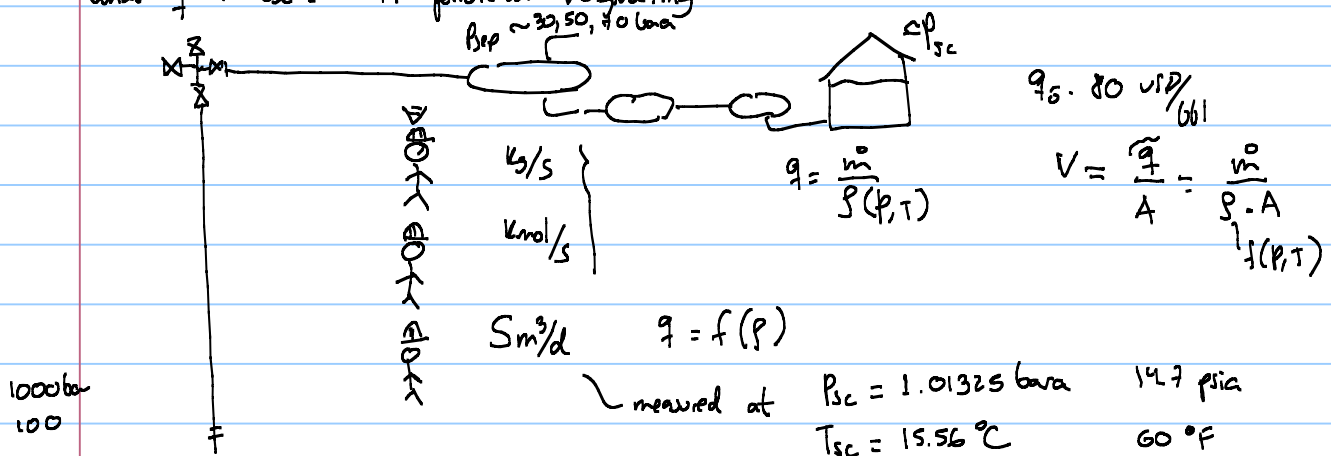


keep p_2 constant





what q to use? in petroleu reengineering
1 ~ 30, 50, 70 loca



with gas

$\dot{m}_{sc} = \dot{m}(p, T)$ — need to calculate pressure drop!

$$q_{sc} \cdot p_{sc} = q_{(p,t)} \cdot p_{(p,t)}$$

the one measured and sold

$$q(p, T) = q_{sc} \left(\frac{p_{sc}}{p(p, T)} \right)$$

$$\frac{q(p,T)}{q_{sc}} = b_g(p,T) \quad \text{gas volume factor}$$

$$B_g(p_i) = \frac{p_{sc}}{p(p_i)} \quad \text{then } FVF \quad T = T_R$$

Boyle



Hooke



Charles



Gay-Lussac



Avogadro

ideal gas law

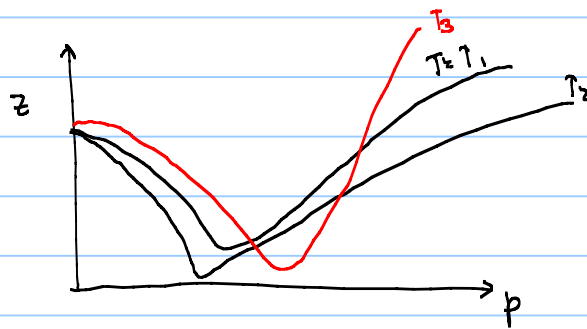
$$PV = R T$$

$$R = \frac{R_u}{MW_{gas}}$$

Real gas law

deviation factor

$$PV = Z R T$$

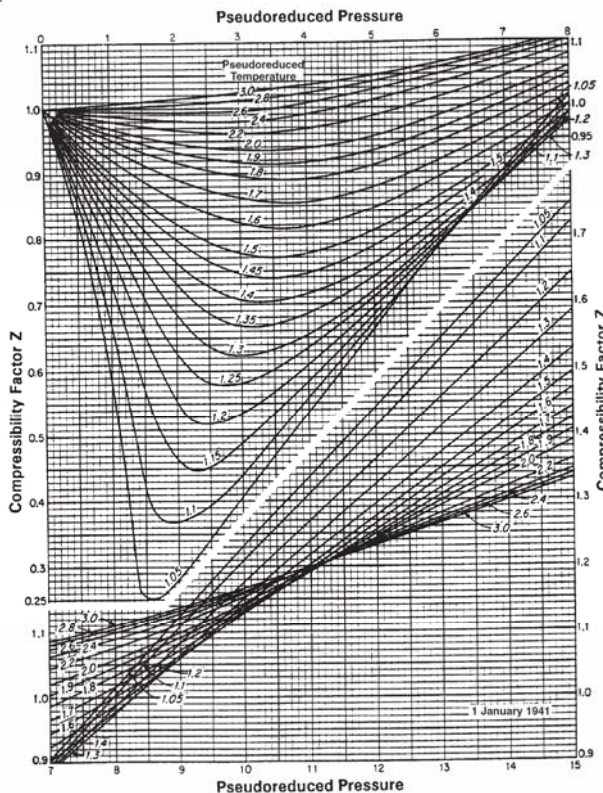


law of corresponding states

$$\underline{p} = \frac{p}{p_c} \quad \underline{T} = \frac{T}{T_c}$$

reduced pressure

Z in production/reservoir between [0.7 - 2]

Fig. 3.6—Standing-Katz⁴ Z-factor chart.

in reality we have a mixture of components

C_1	x_{c1}	MW_{c1}
C_2	x_{c2}	MW_{c2}
C_3	x_{c3}	MW_{c3}
C_4	x_{c4}	
C_5	x_{c5}	
C_{6+}	x_{c6}	

number of components

$$MW_m = \sum_{i=1}^N x_i MW_i$$

Solution

$$\gamma_g = \frac{MW_m}{MW_{air}} = \frac{MW_m}{28.97}$$

$$T_{cm} = f(\gamma_g)$$

$$P_{cm} = f(\gamma_g)$$

$$B_g(p,T) = \frac{p_{sc}}{T_{sc}} \cdot \frac{T}{p} z$$

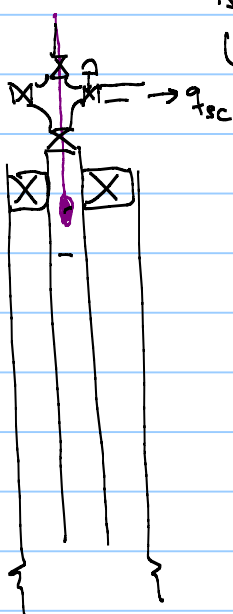
$$p_{sc} V_{sc} = R \cdot T_{sc} z_{sc} \quad \overset{z_{sc} \approx 1}{p_{sc}} = \frac{1}{V_{sc}}$$

$$p_{sc} = \frac{p_{sc}}{R T_{sc}}$$

$$B_g(p,T) = \frac{p_{sc}}{T_{sc}} \cdot \frac{T}{p} z$$

bara
p_{sc}

$$p(p,T) = \frac{p}{R T z}$$



TVD	p	T	v?
TVD ₁			
TVD ₂			
TVD ₃			

www.ept.ntnu.no/~stanko/files/courses/POPE-UM/2018/Exercises

qg [Sm ³ /d]	2.85E+06				
Gas gravity	0.7				
d [m]	0.1143				
A [m ²]	0.0103				
pressure	Temp	z	Bg	qg	vg
[bara]	[C]	[-]	[m/Sm ³]	[m ³ /d]	[m/s]
40	87	0.948259	3.00E-02	8.54E+04	96
46	89	0.942349	2.60E-02	7.41E+04	84
51	90	0.9376	2.32E-02	6.63E+04	75
56	92	0.933712	2.12E-02	6.04E+04	68
61	94	0.9305	1.96E-02	5.59E+04	63
66	96	0.92784	1.83E-02	5.23E+04	59
70	98	0.925643	1.73E-02	4.92E+04	56
74	99	0.923842	1.64E-02	4.67E+04	53
78	101	0.922386	1.56E-02	4.45E+04	50
81	103	0.921234	1.49E-02	4.26E+04	48

UDF user defined function
VBA visual basic applications

z for Standing (p, T, p_g, unit)

B_g(p, T, z, unit)

q_{sc} - B_g

$$\frac{q_g}{A} \left[\frac{m^3}{d} \right] \left[\frac{1d}{24hr} \frac{1hr}{3600s} \right]$$

homework !

