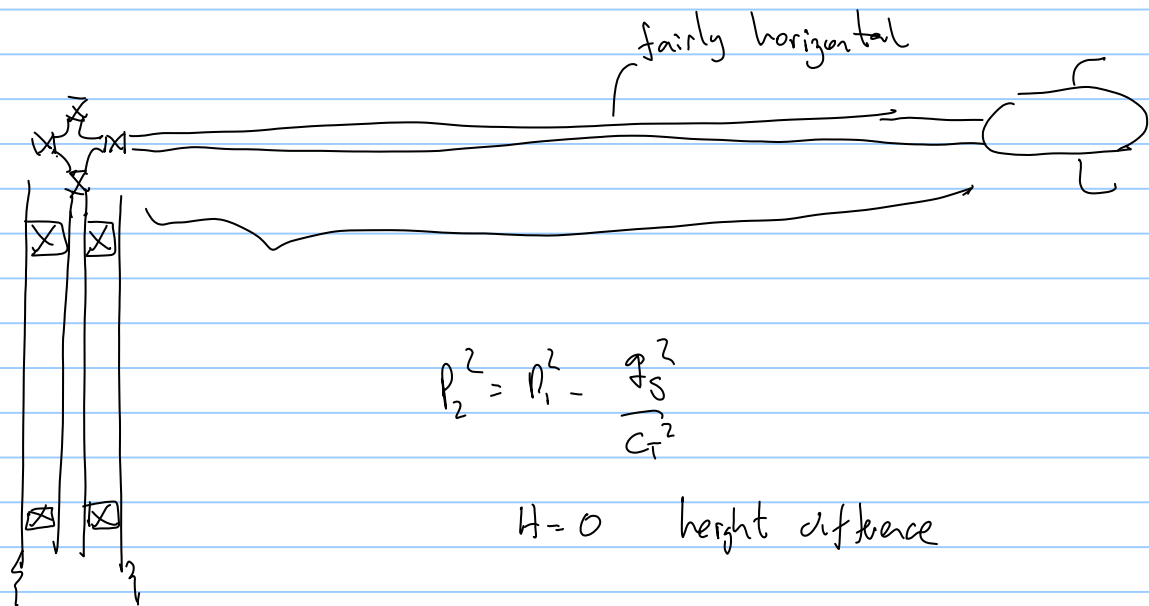


Day 4 :



Tubing flow Equation-Dry gas

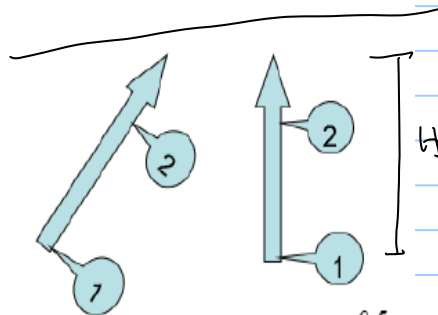
$$q_{sc} = \left(\frac{\pi}{4} \right) \left(\frac{R}{M_{air}} \right)^{0.5} \left(\frac{T_{sc}}{P_{sc}} \right) \left[\frac{D^5}{\gamma_g f_M Z_{av} T_{av} L} \right]^{0.5} \left(\frac{se^s}{e^s - 1} \right)^{0.5} \left(\frac{p_1^2 - p_2^2}{e^s} \right)^{0.5}$$

$$Z_{av} = f(p_{av}, T_{av})$$

$$C_T = f(p_{av})$$

$$\frac{s}{2} = \frac{M_g g}{Z_{av} R T_{av}} H = \frac{(28.97) \gamma_g g}{Z_{av} R T_{av}} H$$

$$q_{gsc} = C_T \left(\frac{p_1^2}{e^s} - p_2^2 \right)^{0.5}$$



$$z_2 - z_1 = H$$

$$H=0$$

$$p_{inlet} = p_1 = e^{s/2} \left(p_2^2 + \frac{q_g^2}{C_T^2} \right)^{0.5}$$

$$p_{wh} = p_2 = \left(\frac{p_1^2}{e^s} - \frac{q_g^2}{C_T^2} \right)^{0.5}$$

$$i \mid H$$

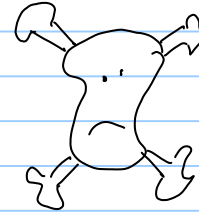
$$S=0$$

$$p_2^2 = \frac{p_1^2}{e^0} - \frac{q_g^2}{C_T^2}$$

$$C_T = \frac{\pi}{4} \left(\frac{R}{m_{air}} \right)^{0.5} \cdot \frac{T_s}{P_{sc}} \left[\frac{D^5}{\gamma_g f \bar{z} \bar{T} L} \right]^{0.5} \left[\frac{s \cdot e^s}{e^s - 1} \right]^{0.5}$$

$$\sqrt{p_1^2 - p_2^2} = q_g$$

$$\lim_{s \rightarrow 0} \left[\frac{s e^s}{e^s - 1} \right]^{0.5} = \frac{0}{0}$$



l'Hopital

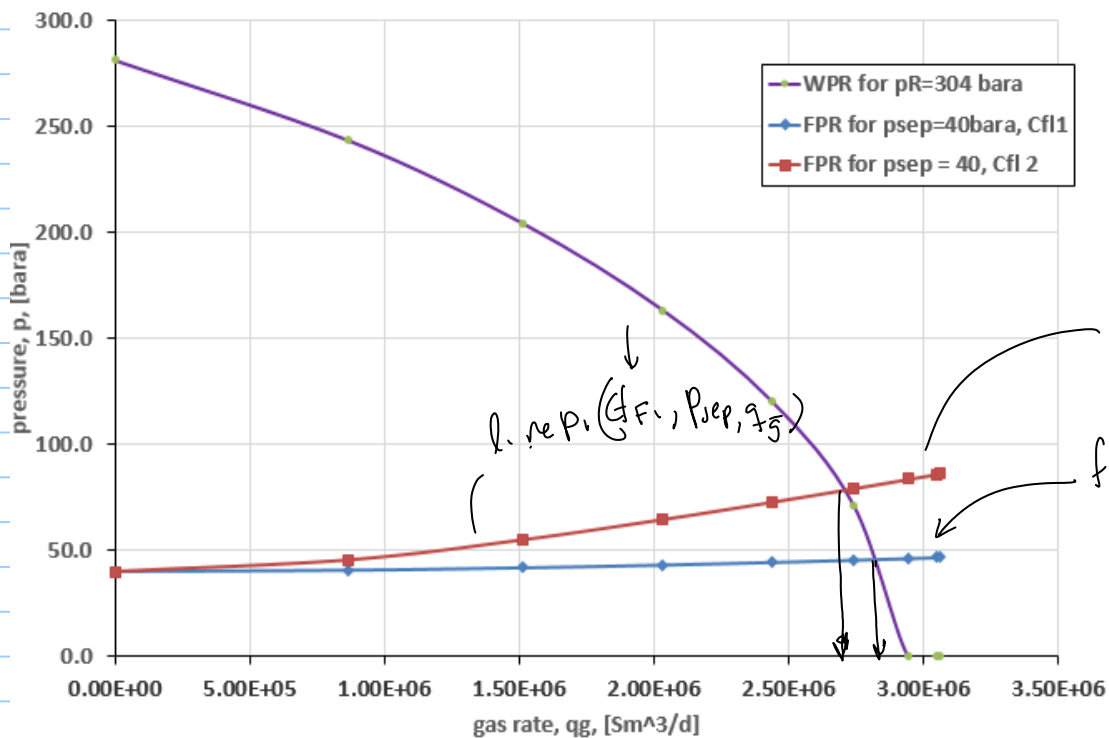
$$\lim_{s \rightarrow 0} \frac{\cancel{e^s} + \cancel{e^s} \cdot 1}{\cancel{e^s} - 1} = 1$$

C_T for horizontal flowline is:

$$C_T = \frac{R}{q} \left(\frac{R}{m_{irr}} \right)^{0.5} \cdot \frac{T_s}{p_{sc}} \left[\frac{Q^5}{R_g \bar{z} \bar{T} L} \right]^{0.5}$$

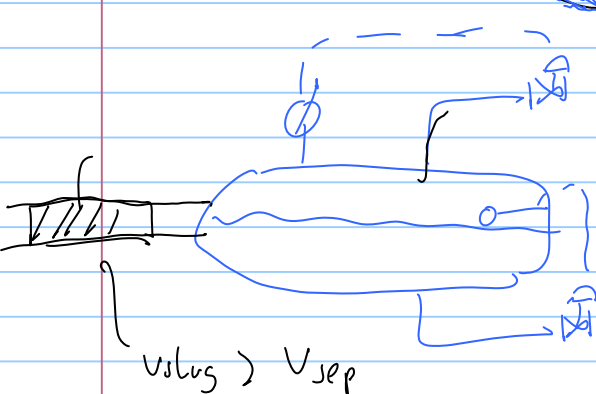
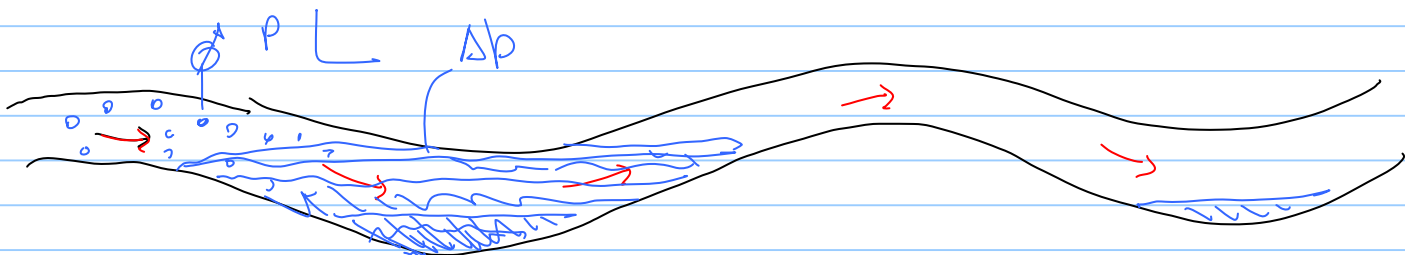
Class exercise WPR vs FPR \rightarrow flowline performance relationship

	IPR	TPR			WPR	PPR for Cf1	PPR for Cf2
pwf_avail	qg	pwf_req	pwf_avail-pwf_req		pwh_avail	pwh_req	pwh_req
[bara]	[Sm ³ /d]	[bara]	[bara]		[bara]	[bara]	[bara]
304	0.00E+00	43.2	260.8		281.3	40.00	40.0
264	8.67E+05	48.5	215.5		243.5	40.60	45.5
224	1.51E+06	57.9	166.1		204.2	41.79	55.1
184	2.03E+06	67.4	116.6		163.4	43.18	64.7
144	2.44E+06	75.6	68.4		120.3	44.50	72.9
104	2.74E+06	82.0	22.0		71.5	45.61	79.3
64	2.94E+06	86.4	-22.4		#VALUE!	46.41	83.7
24	3.05E+06	88.7	-64.7		#VALUE!	46.84	86.0
0	3.06E+06	89.1	-89.1		#VALUE!	46.91	86.4



factors that affect the sizing of gas flowlines:

- Cost $\uparrow \Phi \uparrow$ Cost, \uparrow USD
- pressure drop \downarrow pressure drop $\uparrow \Phi$
- liquid transportation



increased Δp
pipe blockages

- Corrosion
- Hydrates
- Slugging

intermittent production of batches of liquid and gas

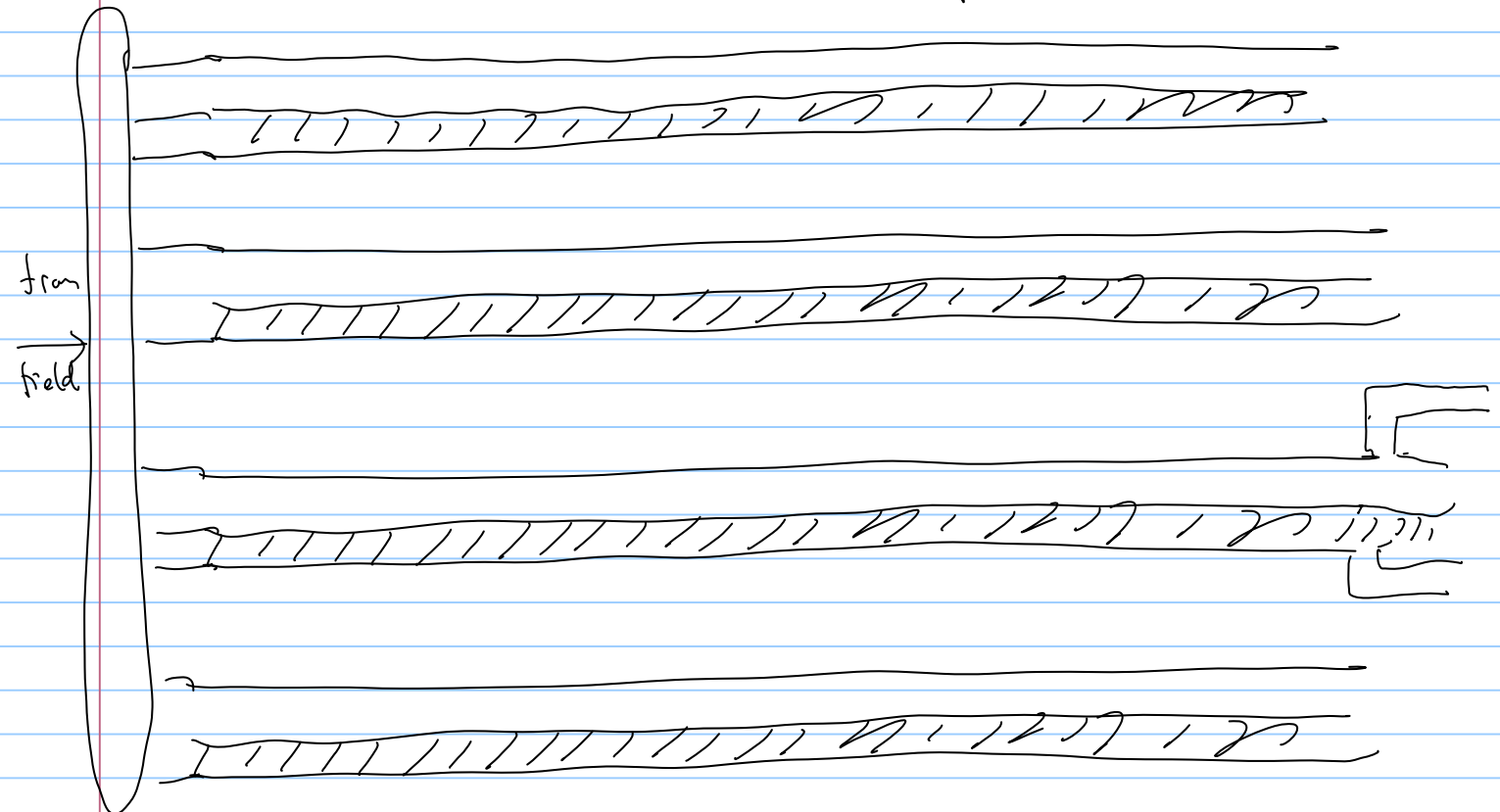
v_{gas} should be high enough to carry liquids and avoid accumulation.



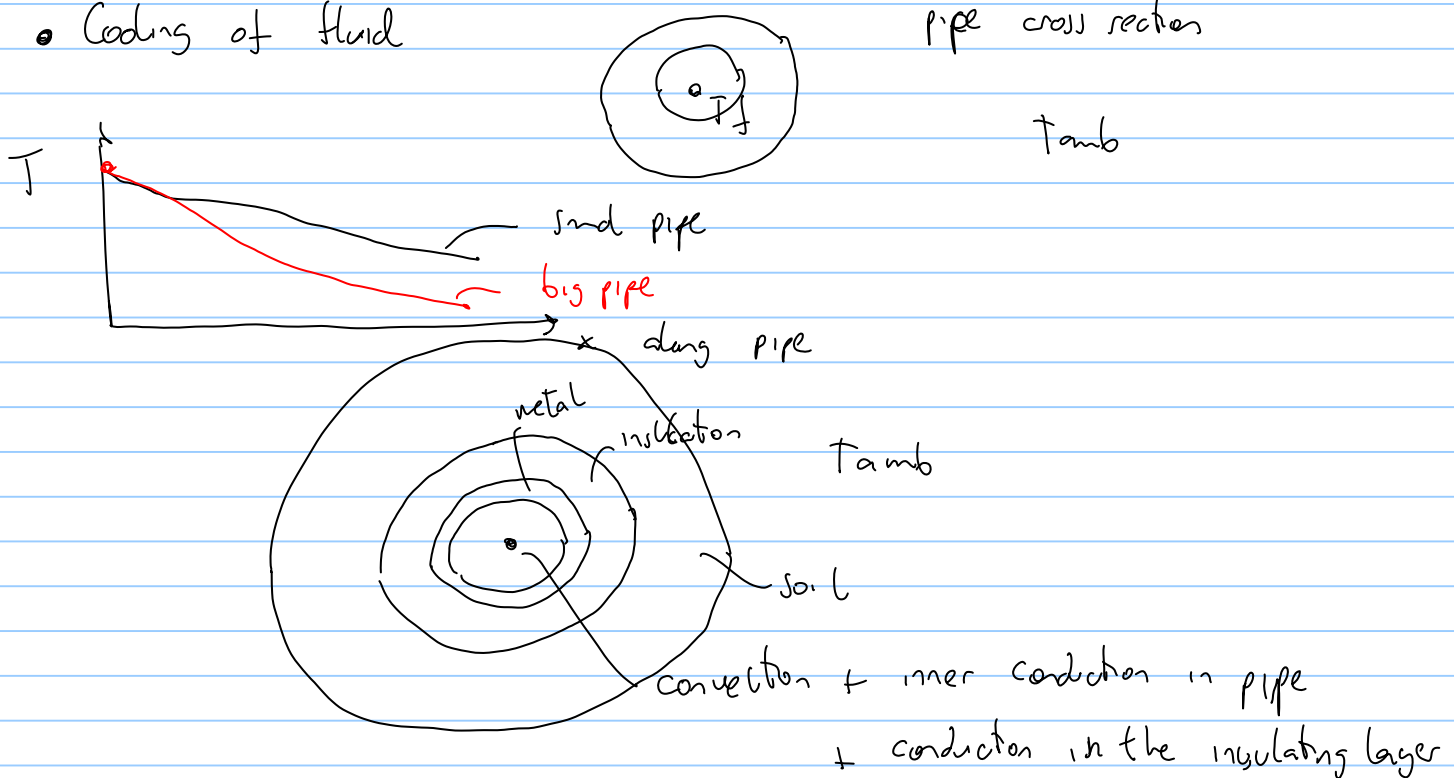
If slugging cannot be avoided

Snowwhite ~ subsea gas field
146 km from
cast
Block-2 Tanzania
Canal

slug catcher a multi pipe long separator



• Cooling of fluid



$$A \cdot U (T_{f, \text{ind}} - T_{\text{amb}}) = \dot{q}$$

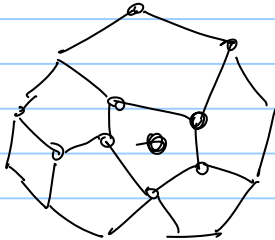
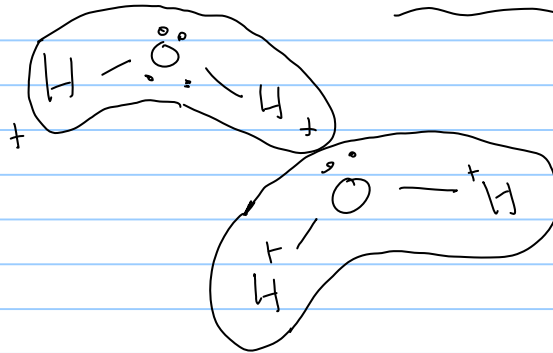
universal heat transfer coefficient
(includes conduction, convection, radiation)

lower temperature \rightarrow more condensation of liquid

Risk forming Hydrates

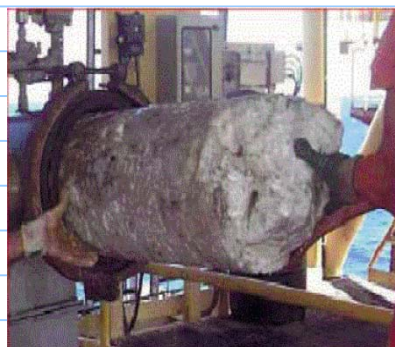
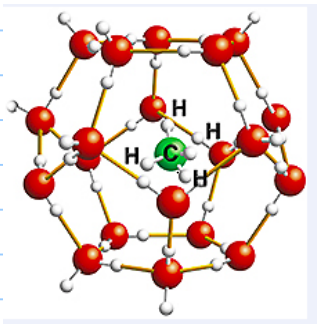
Short comment on Hydrates

at $p = 12 \text{ bara}$
 $T = 4^\circ \text{C}$



CH_4 CO_2
 C_2H_6 N_2
 C_3H_8
 C_4H_{10}

Ice with HC

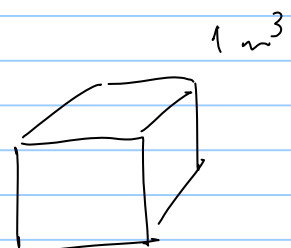


necessary conditions:

- low T
- liquid water (free water)
- small HC molecules

$$\underbrace{4 \text{ CH}_4}_{\sim} \underbrace{23 \text{ H}_2\text{O}}_{\sim} \sim \text{MW} = 478 \frac{\text{kg}}{\text{kmol}}$$

$$\rho \approx 900 \text{ kg/m}^3$$



How much methane in a 1 m^3 of hydrate methane clathrate

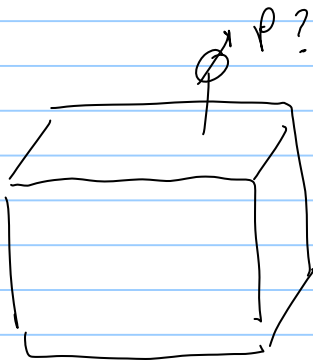
$$M_{\text{hyd}} = \rho \cdot V_{\text{ol}} = 900 \cdot 1 = 900 \text{ kg}$$

$$n = \frac{900 \text{ kg}}{478} = 1.88 \text{ kmol hydrate}$$

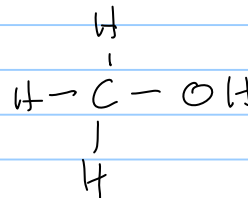
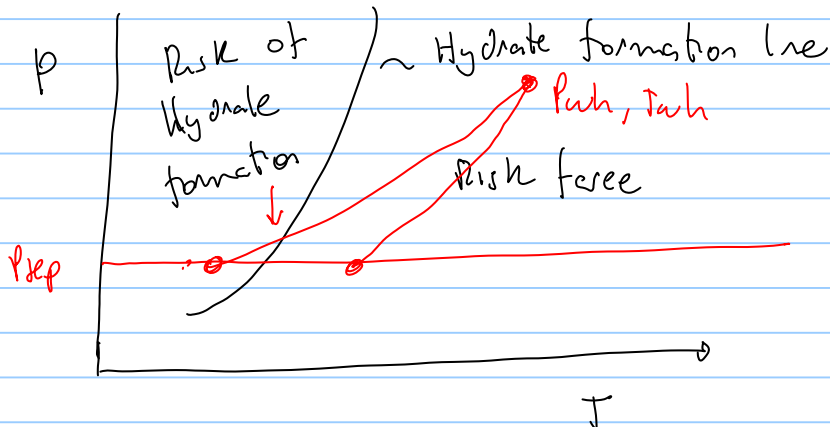
$$n_{\text{CH}_4} = 7.53 \text{ kmol}$$

$$V_{\text{sc}} = n \cdot 23.67$$

$$V_{\text{sc}} = 178 \text{ Sm}^3 \text{ of CH}_4$$



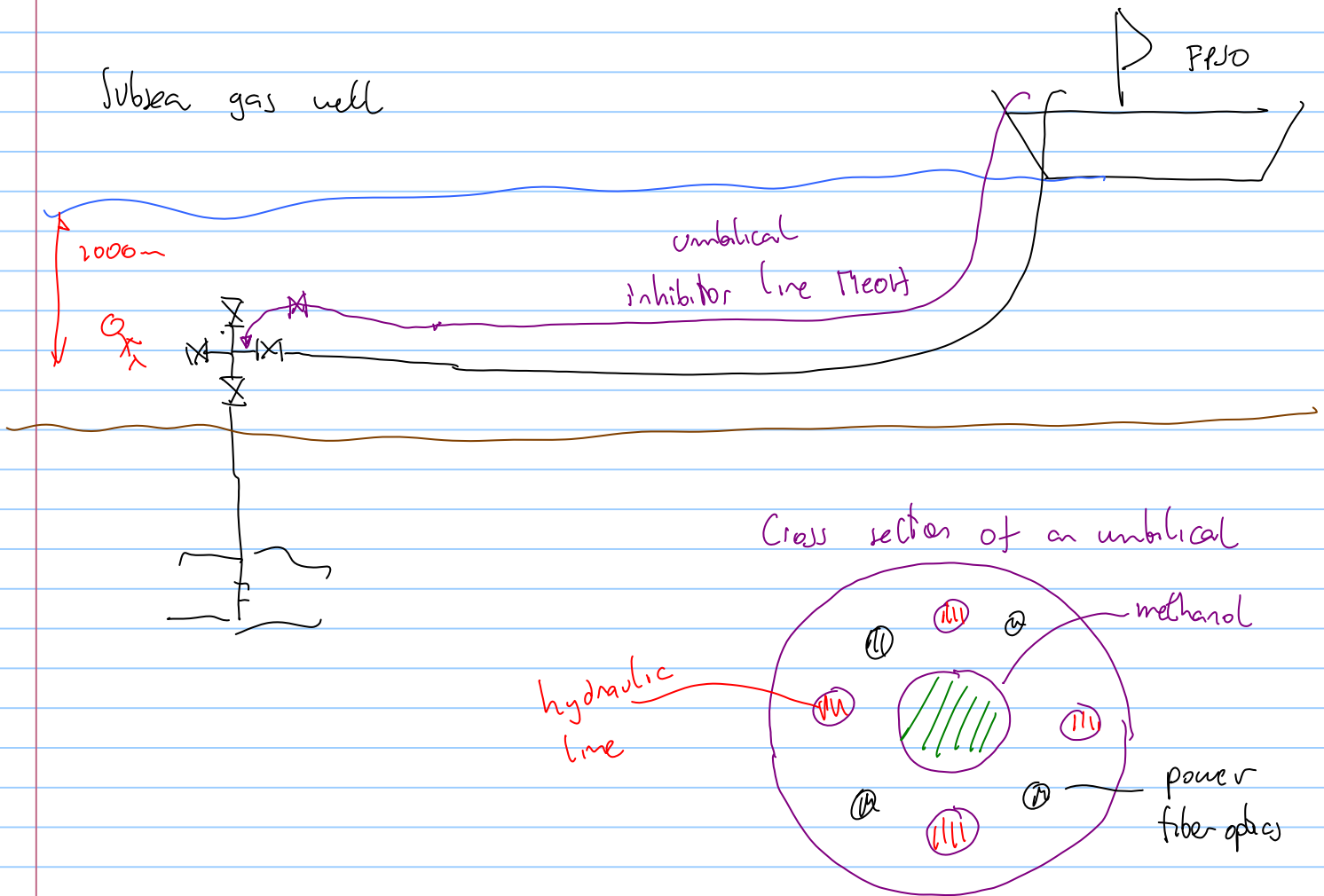
$$p = \frac{7.53 \cdot R \cdot T_{\text{sc}}}{1 \text{ m}^3} \approx 180 \text{ bara}$$



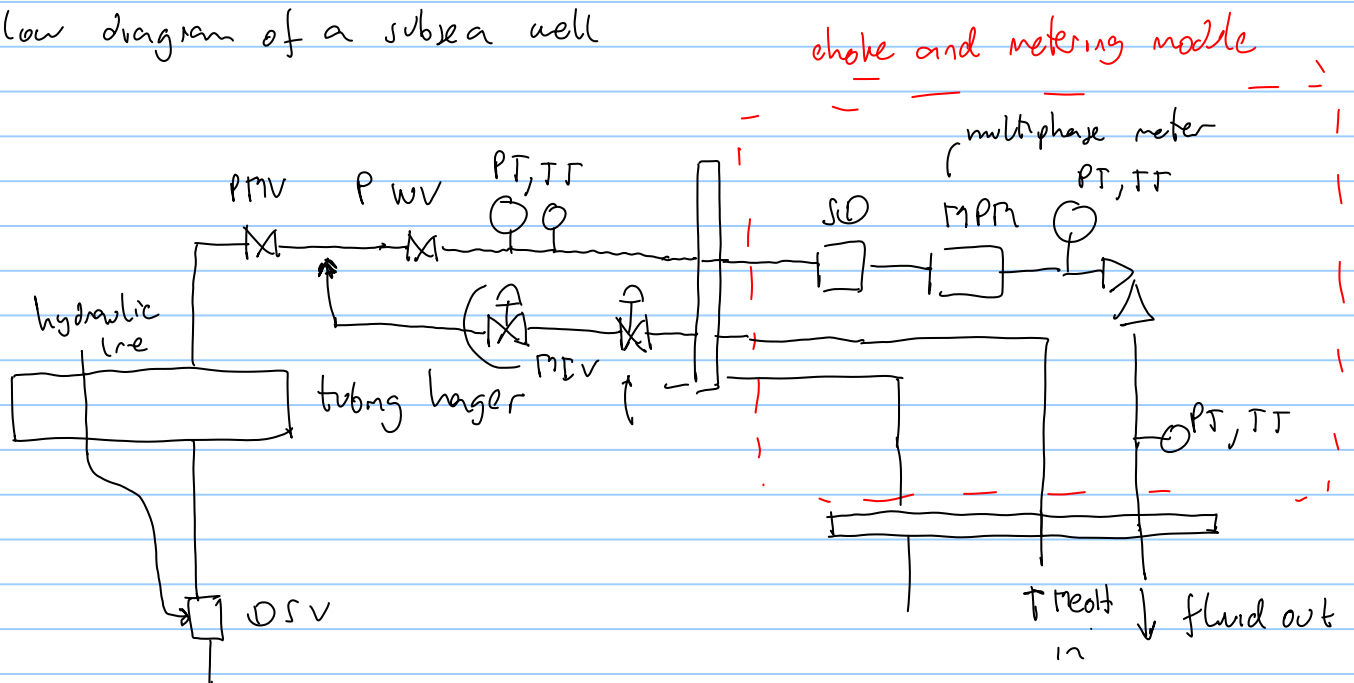
methanol
TEG
MEG

Using hydrate inhibitors to change the hydrate formation line





flow diagram of a subsea well



PwV production wing valve

PT pressure transducer

TT temperature transducer

SD .. Sand detection

PMV ... production master valve

MPV .. Methanol injection valve

- Better estimation of C_T

when using P_R as P_{in} to estimate P_{av} , $\frac{304+40}{2}$

we obtain $C_T = 42500 \text{ Sm}^3/\text{d}/\text{bar}$

$$S = 0.155$$

the equilibrium P_{wf} is actually 84.378 bar way different

than $P_R = 304 \text{ bar}$.

Using this $P_{av} = \frac{84.378 + 40}{2}$ we obtain $C_T = 41900 \text{ Sm}^3/\text{d}/\text{bar}$

$$S = 0.151$$

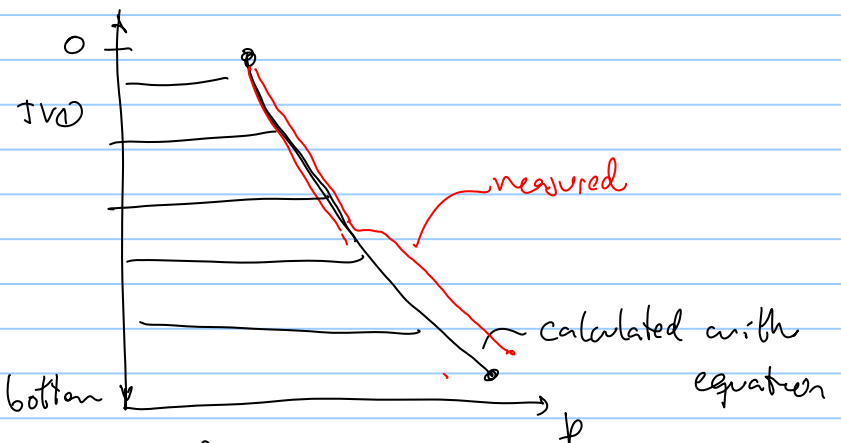
However the equilibrium point is not affected dramatically!

Pressure traverse
calculation

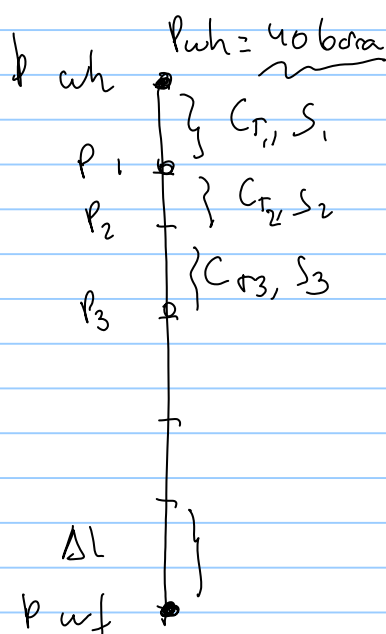
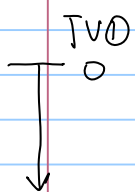
pressure distribution
along tubing

example .. traverse calculation

can help diagnose a well with scaling.



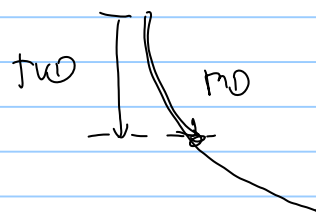
true vertical
depth

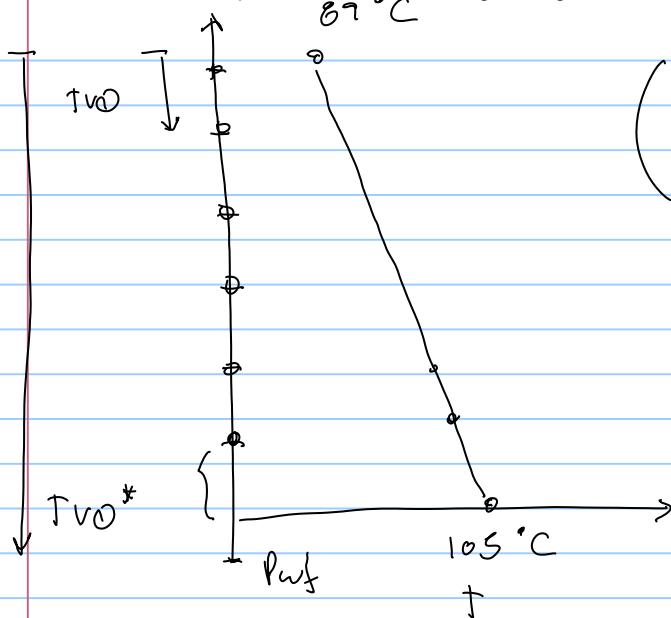


$P_{wh} = 40 \text{ bar}$ $2.85 \text{ cm}^3/\text{d}$

Calculate p distribution along tubing
for equilibrium rate

MO measured depth





$$\left(\frac{105^\circ\text{C} - 39}{TVD^* - 0} \right) = \left(\frac{105 - T}{TVD^* - TVD} \right)$$

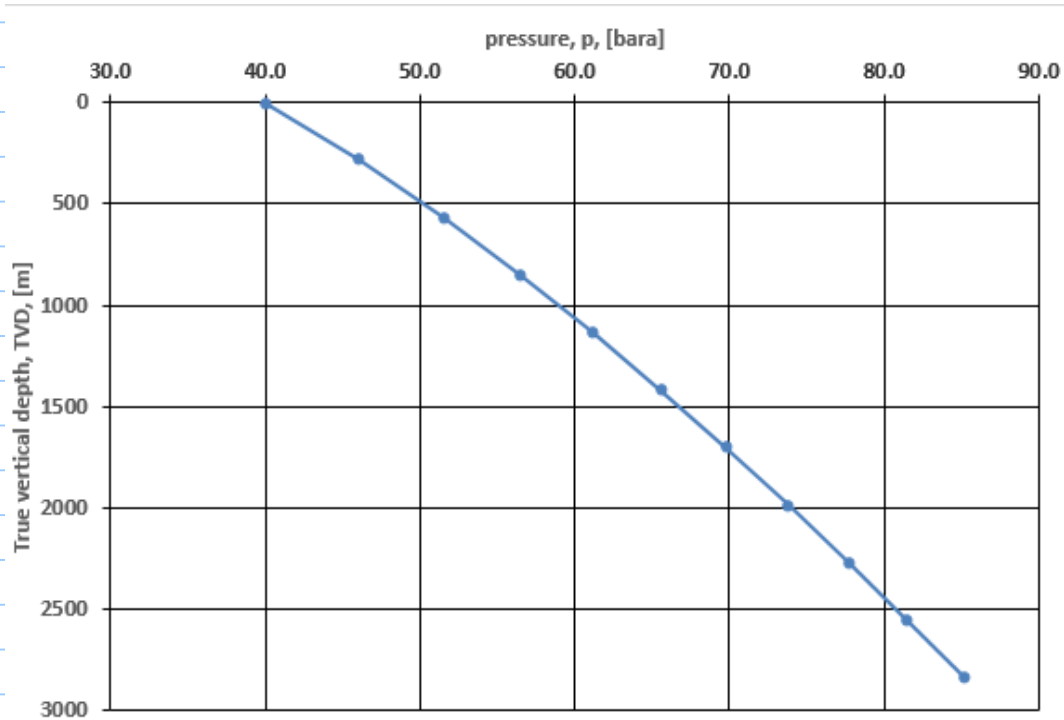
from equilibrium analysis $P_{wf_{eq}} = 84.378 \text{ bara}$

$P_{wh} = 40 \text{ bar}$

i assume $\Delta p = \text{const}$ for every section.

$$\Delta p = \frac{(P_{wf_{eq}} - P_{wh})}{N_{\text{section}}} = \frac{84.378 - 40}{10}$$

Tubing MD [m]	2837							
Tubing TVD [m]	2837							
Tubing ID [m]	0.157							
Tubing Cross section A [m ²]	0.019							
Wellhead pressure [bara]	40							
Gas gravity	0.55							
Twf [K]	378	104.85						
Twh [K]	360	86.85						
pR [bara]	304			DP	4.4378			
friction factor [-]	0.012							
qg [Sm ³ /d]	2.85E+06							
liquid density [kg/m ³]	8.97E+02							
TVD	T	Tav	passumed	Pav	Zav	S	Ct	p
[m]	[K]	[K]	[bara]	[bara]	[-]	[-]	[Sm ³ /bar]	[bara]
0	360.0	360.9	40.0	42.2	0.967	0.015	1.3E+05	40.0
284	361.8	362.7	44.4	46.7	0.964	0.015	1.3E+05	46.0
567	363.6	364.5	48.9	51.1	0.962	0.015	1.3E+05	51.5
851	365.4	366.3	53.3	55.5	0.960	0.015	1.3E+05	56.5
1135	367.2	368.1	57.8	60.0	0.959	0.015	1.3E+05	61.1
1418	369.0	369.9	62.2	64.4	0.957	0.015	1.3E+05	65.6
1702	370.8	371.7	66.6	68.8	0.956	0.015	1.3E+05	69.8
1986	372.6	373.5	71.1	73.3	0.955	0.015	1.3E+05	73.8
2269	374.4	375.3	75.5	77.7	0.954	0.015	1.3E+05	77.7
2553	376.2	377.1	79.9	82.2	0.954	0.015	1.3E+05	81.4
2837	378.0		84.4					85.1



• Homework Solve this exercise by yourself at home

Find p vs TVD for the well studied in class ⚡
 for $p_{wh} = 40 \text{ bara}$ and $\bar{q}_g = 2.85 \text{ E}6 \text{ Sm}^3/\text{d}$