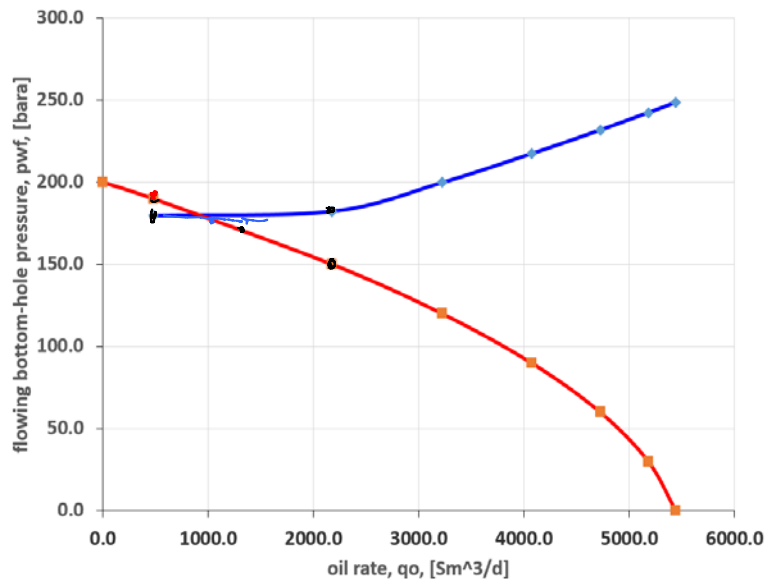
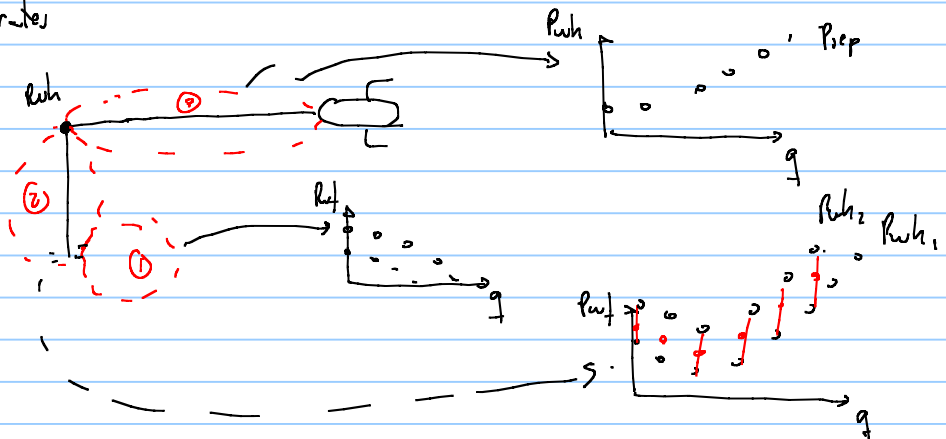


Class 6

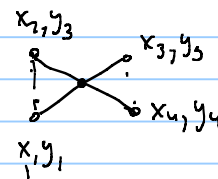
Solution of class exercise - flow equilibrium in a saturated oil well:



in commercial software, performance curves are often precomputed and later the collection of points is used to find operating rates

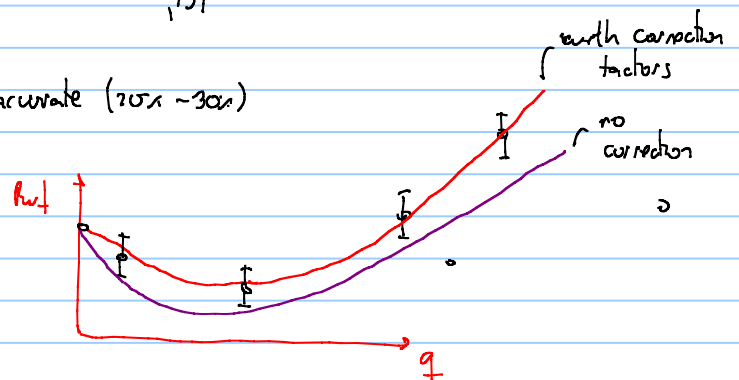


the mixture is found by intersecting two straight lines

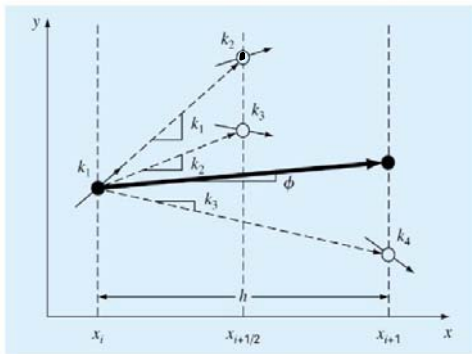


in most cases multiphase dp models are not 100% accurate (20% - 30%)

$$\frac{dp}{dx} = - \rho_{mix} \cdot g \cdot \sin \theta - \rho_{mix} \cdot f \cdot \frac{v_m^2}{2 \cdot D}$$



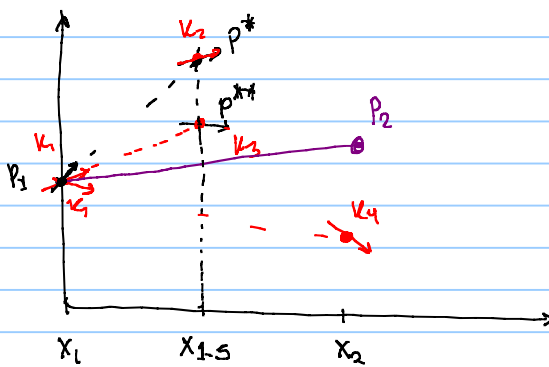
Classic 4th-order Runge-Kutta Method



IMethods
3

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Prof. Jinbo Bi
CSE, UCenn



$$① \left. \frac{dp}{dx} \right|_{p_1, x_1} = k_1 \quad \text{Euler's}$$

$$② \frac{p^* - p_1}{\Delta x \cdot 0.5} = k_1 \rightarrow p^*$$

$$③ \textcircled{2} p^*, x_{1.5} \rightarrow \left. \frac{dp}{dx} \right|_{p^*, x_{1.5}} = k_2$$

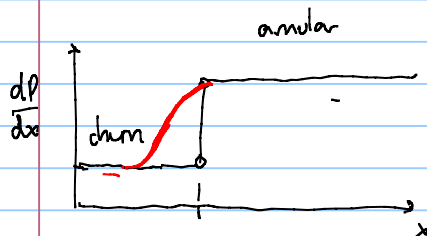
$$④ \frac{p^{**} - p_1}{\Delta x \cdot 0.5} = k_2 \rightarrow p^{**}$$

$$⑤ \textcircled{3} p^{**}, x_{1.5} \rightarrow \left. \frac{dp}{dx} \right|_{p^{**}, x_{1.5}} = k_3$$

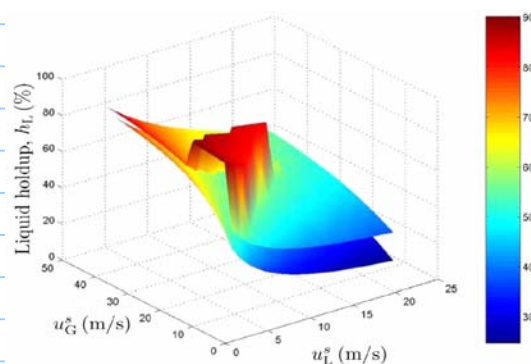
$$⑥ \frac{p_2' - p_1}{\Delta x} = k_3 \rightarrow p_2'$$

$$⑦ \textcircled{4} p_2', x_2 \rightarrow \left. \frac{dp}{dx} \right|_{p_2', x_2} = k_4$$

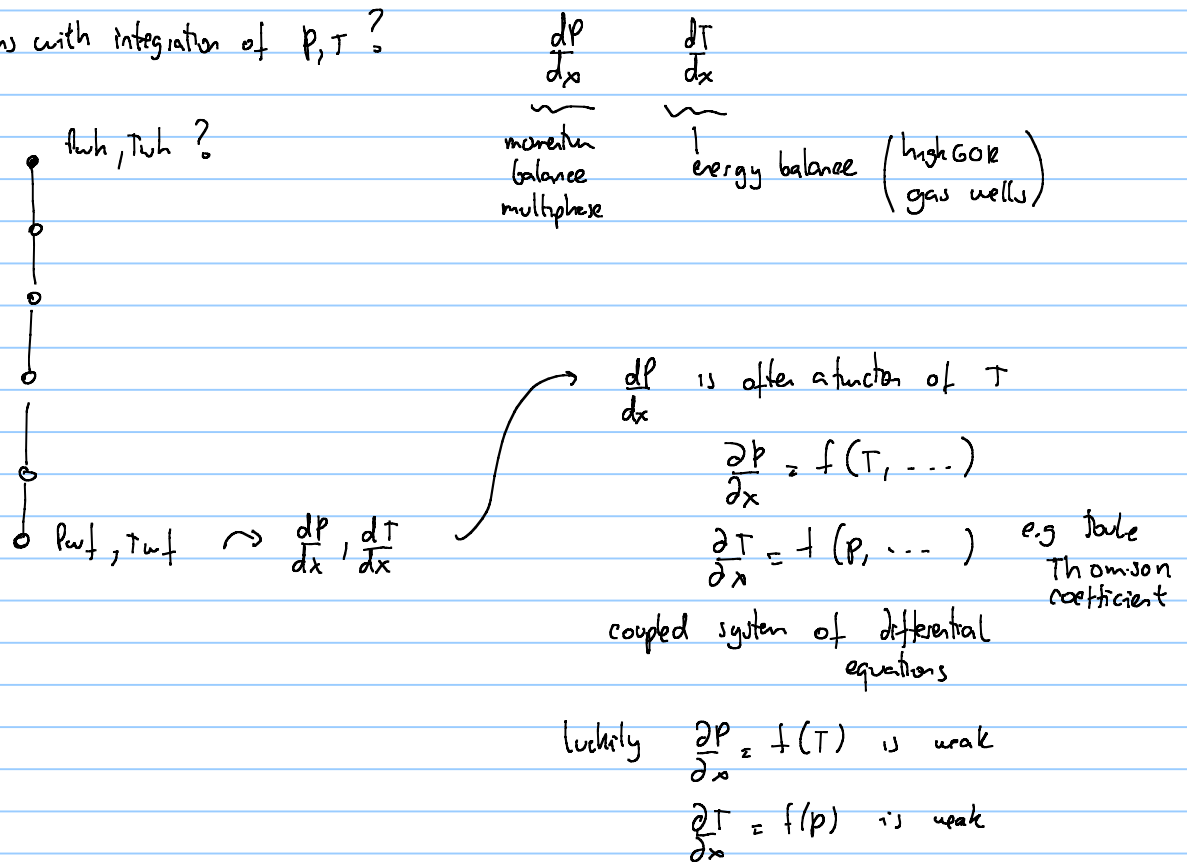
$$⑧ y^*(t_0 + h) = y^*(t_0) + \frac{k_1 + 2k_2 + 2k_3 + k_4}{6} h \rightarrow p_2$$



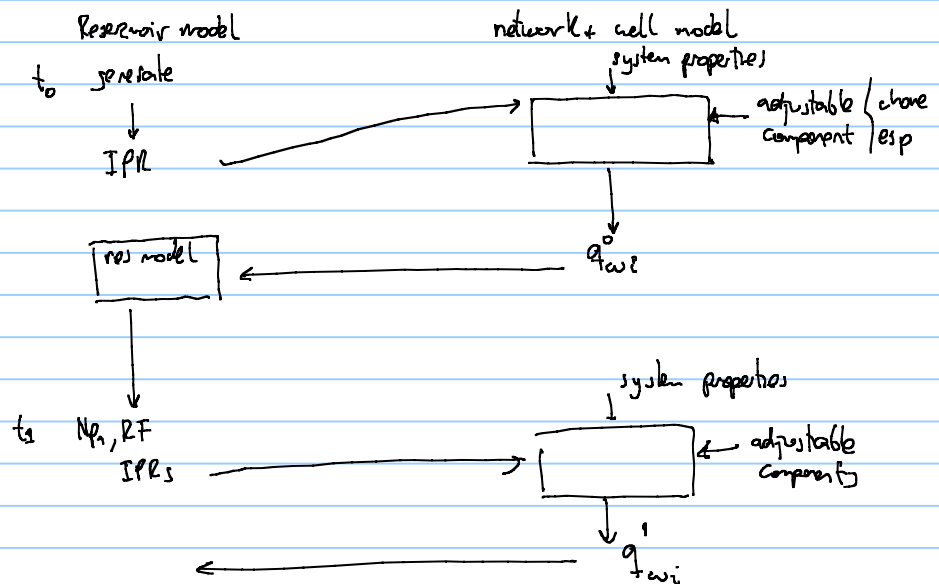
flow pattern based dp model looks like



what happens with integration of p, T ?



field performance



coupling of reservoir and network models

SPE 65159

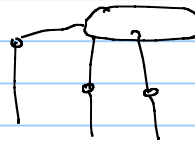
Linking reservoir and surface simulators: how to improve the coupled solutions

C. C. Barroux, Institut Francais du Pétrole, P. Duchet-Suchaux, TotalFinaElf S.A., P. Samier, TotalFinaElf S.A., R. Nabil, Gaz de France

- undersaturated oil reservoir strong aquifer support \rightarrow no multiphase flow in the formation during life of field
- field produced with ESPs



- well are standalone (no surface network)



- well are identical

Reservoir model

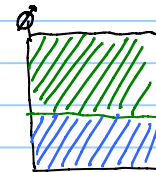
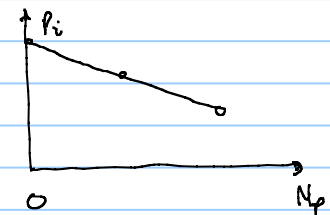
$$\frac{1}{A} = \frac{\left(N \cdot B_{oi} \cdot c_o + N \cdot B_{oi} \cdot \frac{c_w \cdot S_w + c_f}{S_o} + V_a \cdot \phi_a \cdot (c_w + c_f) \cdot B_w \right)}{B_o(p)}$$

initial oil in place
compressibility

$$P_R = P_i - A \cdot N_p$$

B_o, c_e, V_a, V_h

Material balance



well model

$$q_o = J \cdot (P_R - P_{wf})$$

ESP can operate down to a minimum bottomhole pressure $P_{suc} > P_b(T_R)$

P_{wfmin}

$$q_{omax} = J (P_R - P_{wfmin})$$

for " N_w " number of identical wells

$$q_{field} = N_w J (P_R - P_{wfmin})$$

$$q_f = N_w J (P_i - A \cdot N_p - P_{wfmin})$$

$$q_f = -N_w \cdot J \cdot A \cdot N_p + N_w \cdot J (P_i - P_{wfmin})$$

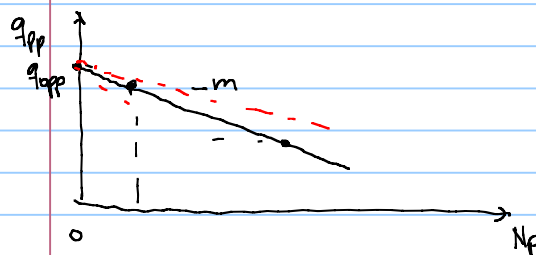
initial maximum production

$$q_f = -N_w \cdot J \cdot A \cdot N_p + q_{of}$$

max field rate @ N_p

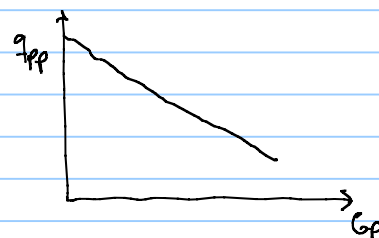
$q_f = q_{pp}$ field production potential

$$q_{pp} = -m N_p + q_{pp0} \quad \text{field production potential @ initial reservoir pressure}$$



for other cases

• dry gas and network



production potential is calculated by,

@ a given N_p , run model to obtain maximum production

→ open choke

→ ESP, lift pump, frequency

→ gas lift → optimization

→ multiphase booster → new frequency

$$\left\{ \begin{array}{l} q_{pp} = -m N_p + q_{pp0} \\ \int_0^t q_{pp} dt \end{array} \right\} \quad \text{— lift pump, initial conditions}$$

→ A → reservoir (size, structure, fluid properties)

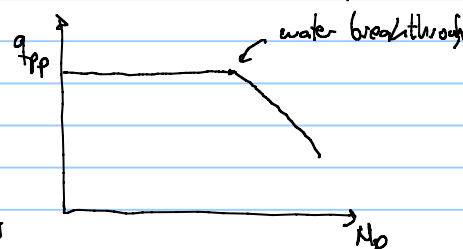
→ N_w → number wells

→ J → well productivity

• saturated + undersaturated



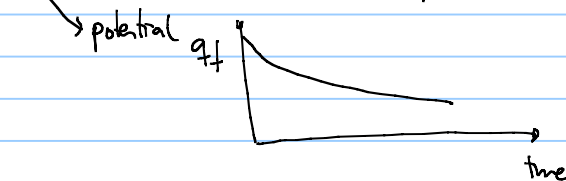
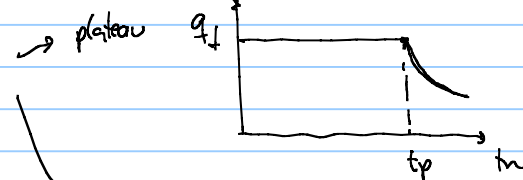
• undersaturated + water injection $P_e \approx \text{constant}$



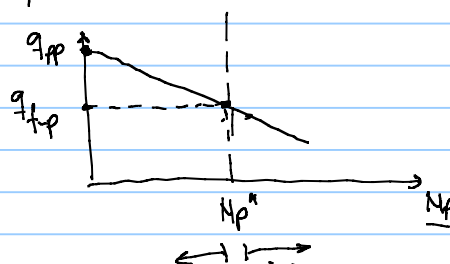
field are typically produced in two modes

$$q_f = f(t) ?$$

$$q_f = \begin{cases} q_{fp} & \text{if } t \leq t_p \\ q_f = q_{pp} & \text{for } t > t_p \end{cases}$$



plateau will end when $q_{fp} = q_{pp}$



for $N_p > N_p^*$ I cannot maintain desired plateau

for $N_p \leq N_p^*$ I can produce plateau

$$N_p^* \text{ [Sm}^3\text{]} \quad q_{f-p} \text{ [Sm}^3\text{/d]} \quad 0 \rightarrow N_p^*$$

$$t_p = \frac{N_p^* \text{ [Sm}^3\text{]}}{q_{f-p} \text{ [Sm}^3\text{/d]}} \cdot \frac{1}{\text{uptime}} \quad (1) \quad \text{uptime ; number of operational days in a year} \quad \left[\frac{\text{day}}{\text{year}} \right]$$

$$q_{p-f} = q_{pp} = -m N_p^* + q_{ppo}$$

$$N_p^* = \left[\frac{q_{ppo} - q_{pf}}{m} \right] \quad (2)$$

$$t_p = \frac{q_{ppo} - q_{pf}}{m \cdot q_{f-p} \text{ uptime}} = \frac{1}{m} \cdot \frac{1}{\text{uptime}} \left(\frac{q_{ppo}}{q_{f-p}} - 1 \right)$$

for $t > t_p$

$$t_p = \frac{1}{N_w \cdot A \cdot J} \left[\frac{N_w J (R_i - R_{w, \min}) - 1}{q_{f-p}} \right]$$

$$q_f = q_{pp} = -m \int_0^t q_f dt + q_{ppo}$$

$$t_p = \frac{1}{A \cdot J} \left[\frac{J (R_i - R_{w, \min})}{q_{f-p}} - \frac{1}{N_w} \right]$$

$$q_f = -m \int_0^{t_p} q_{p-f} dt - m \int_{t_p}^t q_f dt + q_{ppo}$$

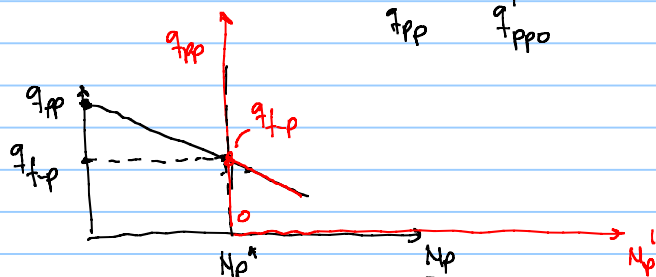
$$q_f = -m q_{p-f} t_p - m \int_{t_p}^t q_f dt + q_{ppo}$$

$$q_f = -m \frac{1}{N_p^*} (q_{ppo} - q_{pf}) - m \int_{t_p}^t q_f dt + q_{ppo}$$

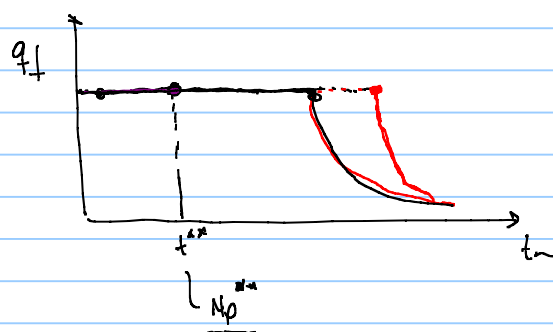
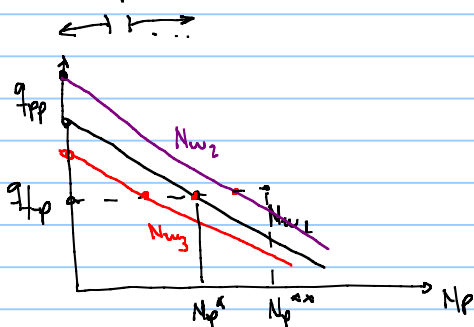
$$q_f = q_{p-f} - m \int_{t_p}^t q_f dt$$

https://en.wikipedia.org/wiki/Integrating_factor

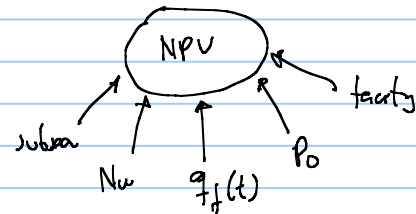
a solution is:



$$q_f = q_{f-p} \cdot e^{-m(t-t_p)} \quad A \cdot J \cdot N_w$$



in the field development process decision \rightarrow NPV



time expenditures revenue

- 0
- 1
- 2
3
4
5

Cash Flow
Revenue - expenditure

DCF

$$PV = \frac{FV}{(1+i)^n}$$

\sim year counter
interest rate

$$COEF = NPV$$

find q_{fp} such as NPV is maximum $\uparrow q_{fp}$ increase revenue \uparrow CAPEX $r = f(q_{fp})$?

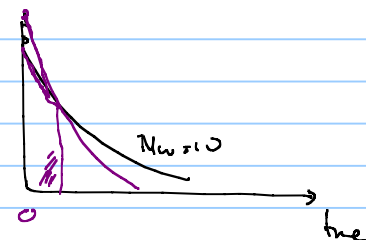
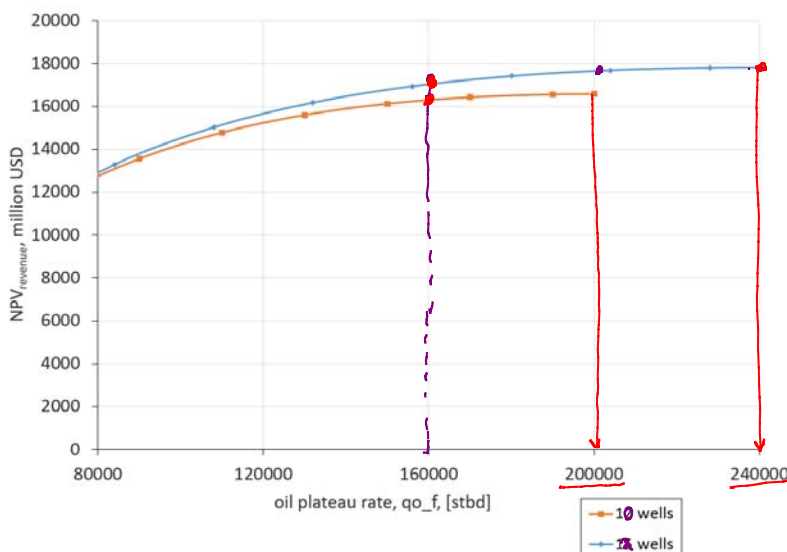
$$PV \text{ Revenue} = \int_0^t \frac{P_0 \cdot q_{fp}}{e^{it}} dt$$

discrete discounting $\frac{1}{(1+i)^n}$

continuous discounting $\frac{1}{e^{it}}$

$$PV_{\text{revenue}} = P_0 \left[\int_0^{t_p} \frac{q_{fp}}{e^{it}} dt + \int_{t_p}^t \frac{q_{fp} e^{-m(t-t_p)}}{e^{it}} dt \right]$$

$$PV_{\text{revenue}}(t) = q_{fp} \cdot P_0 \left[\frac{m + i - m e^{-\left(\frac{q_{p0}}{q_{fp}} - 1\right) \frac{i}{m}}}{i(m+i)} - \frac{(m+i)t + \left(\frac{q_{p0}}{q_{fp}} - 1\right)}{-ie} \right]$$



$$\frac{1}{e^{it}}$$

