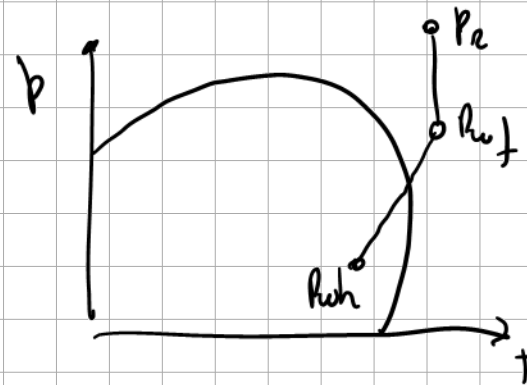
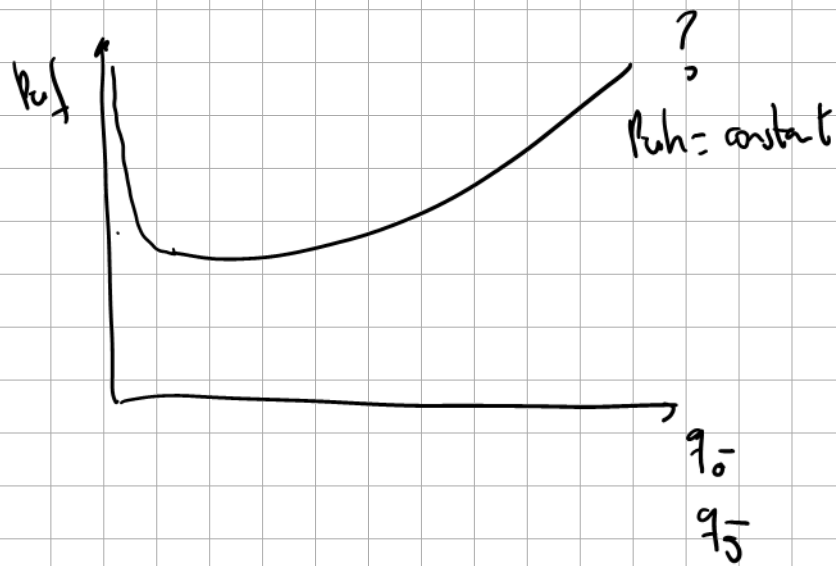
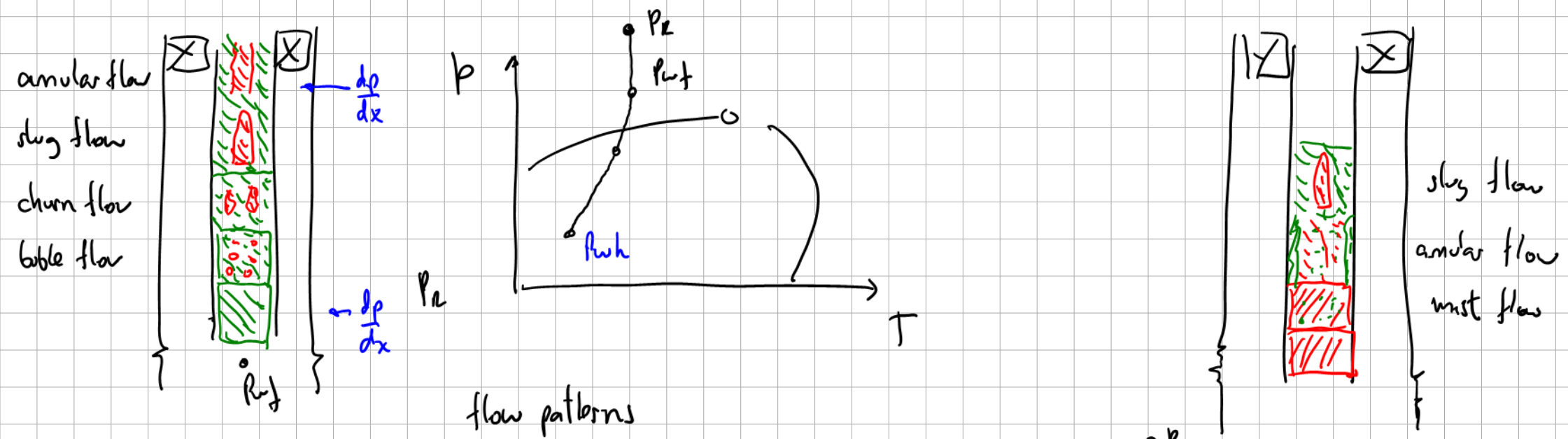




Flowing and Gas-lift Well Performance†

W. E. GILBERT*

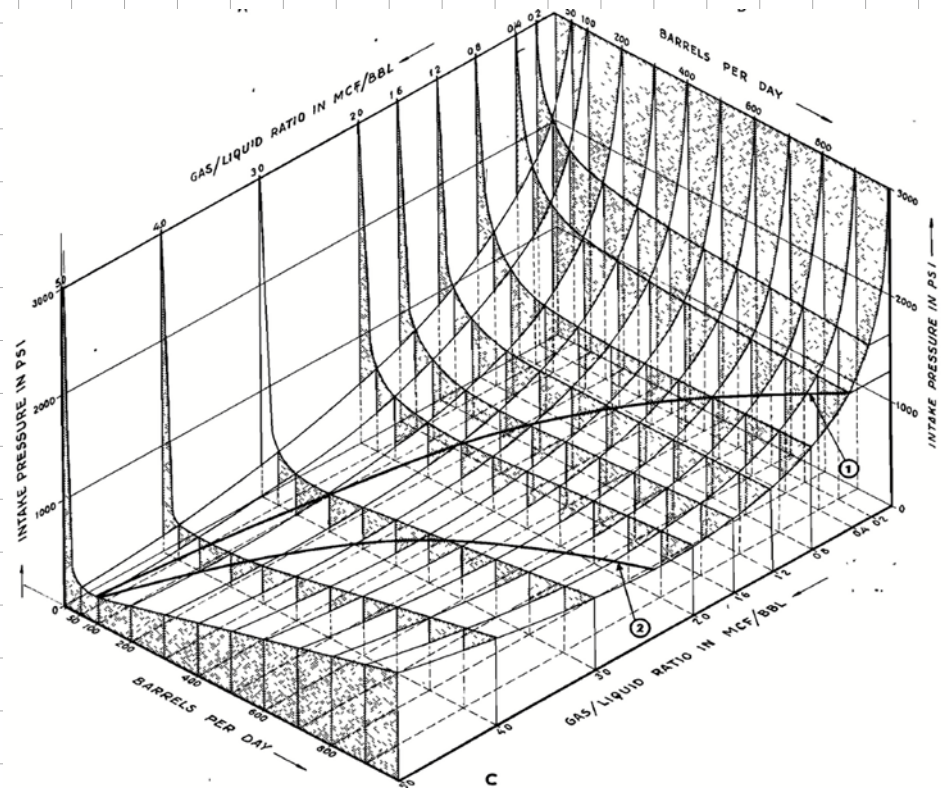
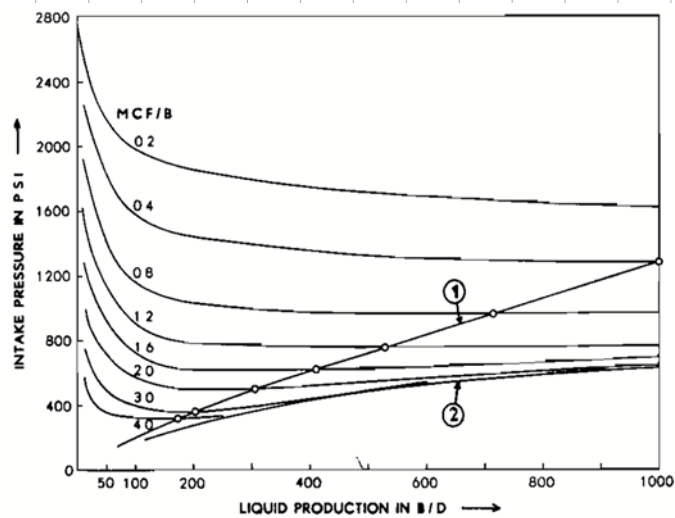
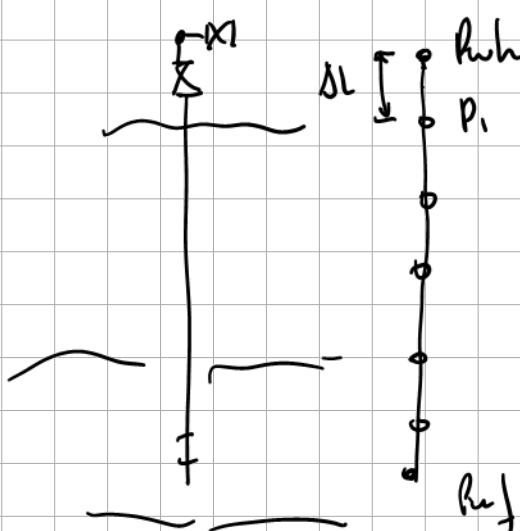


Fig. 6—The Two-phase Vertical-lift Function for 2.875-in. Tubing Set at 8,000 Ft (Tubing Pressure = Zero Psi Gage)

$$\Delta p_{\text{tubing}} = \Delta p_{\text{hydrostatic}} + \Delta p_{\text{friction}}$$

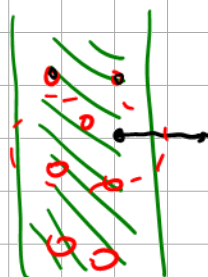


$$\frac{dp}{dx} \bigg|_{P_{wh}} \rightarrow P_i$$

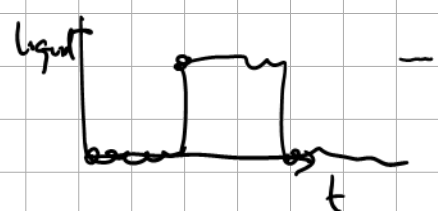
$$P_1 = P_{wh} + \frac{dp}{dx} \bigg|_{P_{wh}} \cdot \Delta L$$

$$P_2 = P_1 + \frac{dp}{dx} \bigg|_{P_1} \cdot \Delta L$$

integration
marching algorithm



$$\frac{d}{dt} \neq 0$$



$$\bar{x} = \frac{\int_1 x \, dA}{A}$$

$\frac{dp}{dx} \rightsquigarrow$ PVT properties ($\rho, \rho_g, \mu, \mu_g, \sigma, x_g$)
 $\rightsquigarrow$ velocity (q_g, q_l)
 $\rightsquigarrow$ A, ϕ, θ, e
 $\uparrow$ roughness
 new data

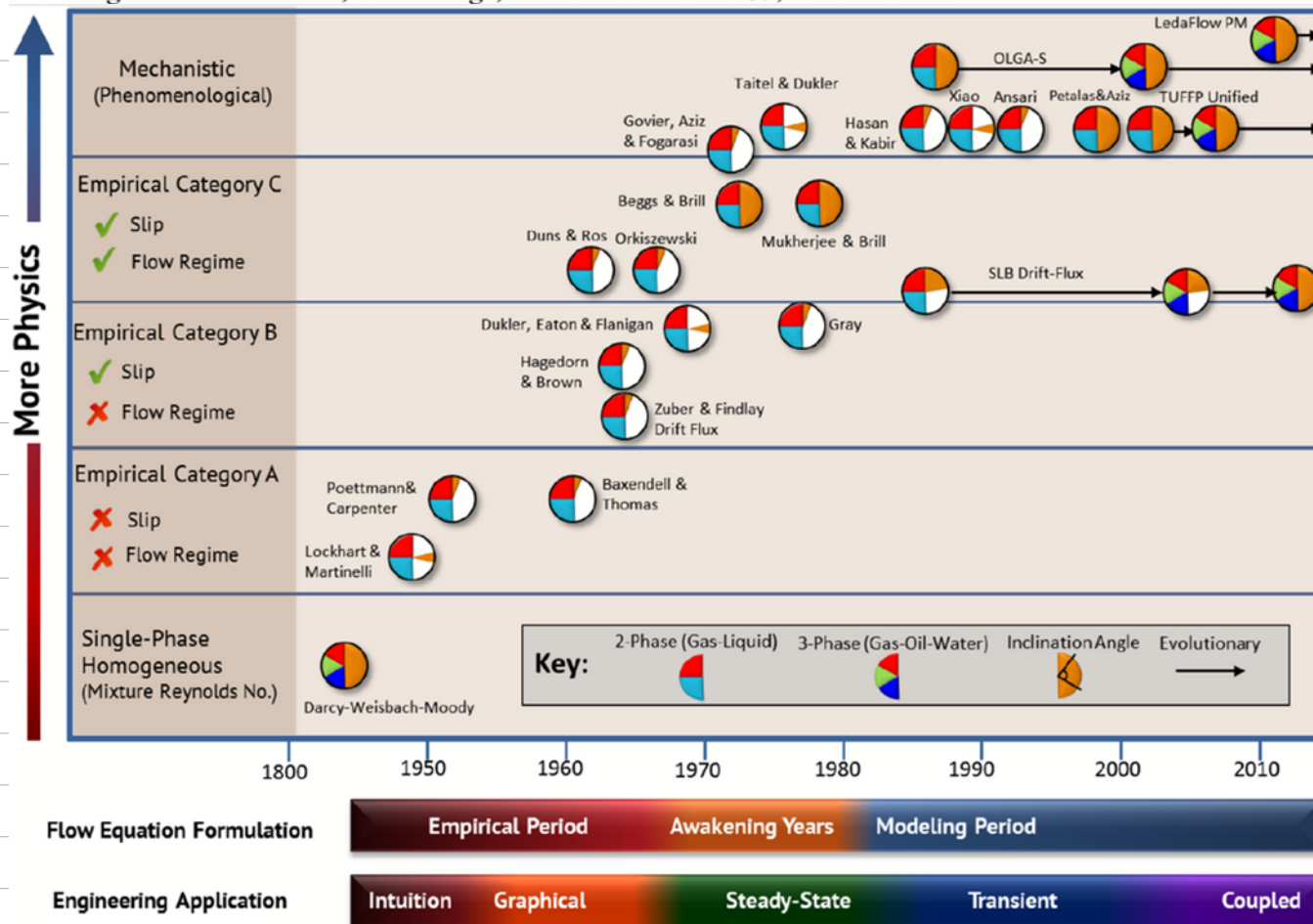
Steady-State Multiphase Flow—Past, Present, and Future, with a Perspective on Flow Assurance

Mack Shippen*

Schlumberger SIS, Houston, Texas 77056, United States

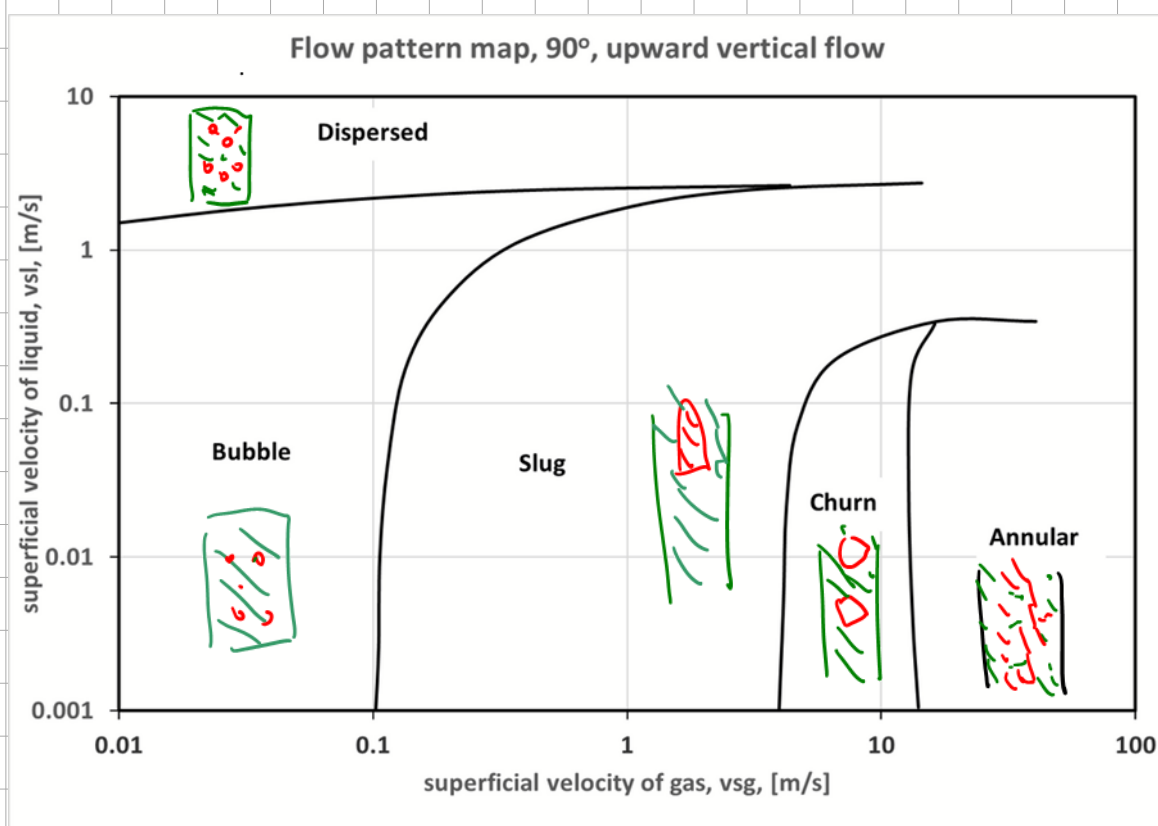
William J. Bailey

Schlumberger—Doll Research, Cambridge, Massachusetts 02139, United States



flow pattern map

for given fluid, pipe, inclination, etc



$$u_{sl} = \frac{q_l}{A}$$

$$u_{sg} = \frac{q_g}{A}$$

