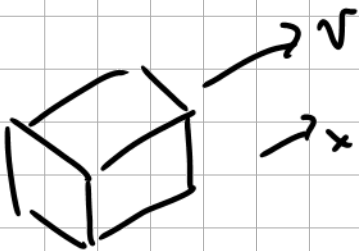
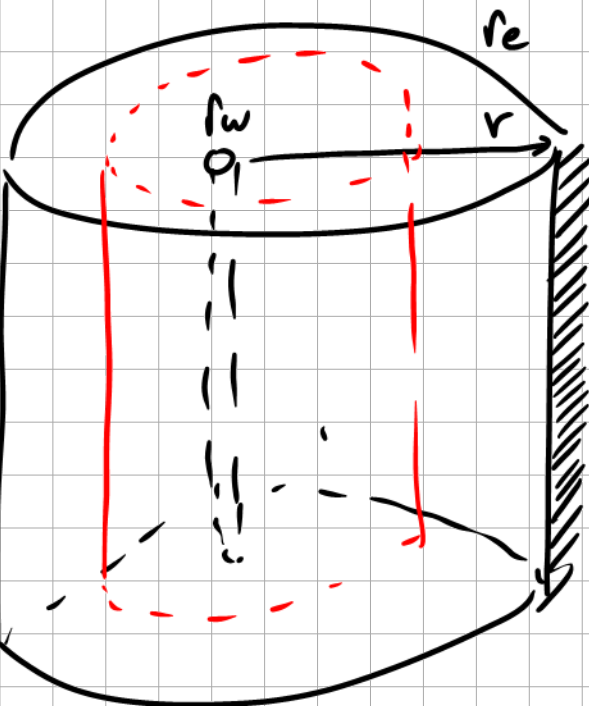


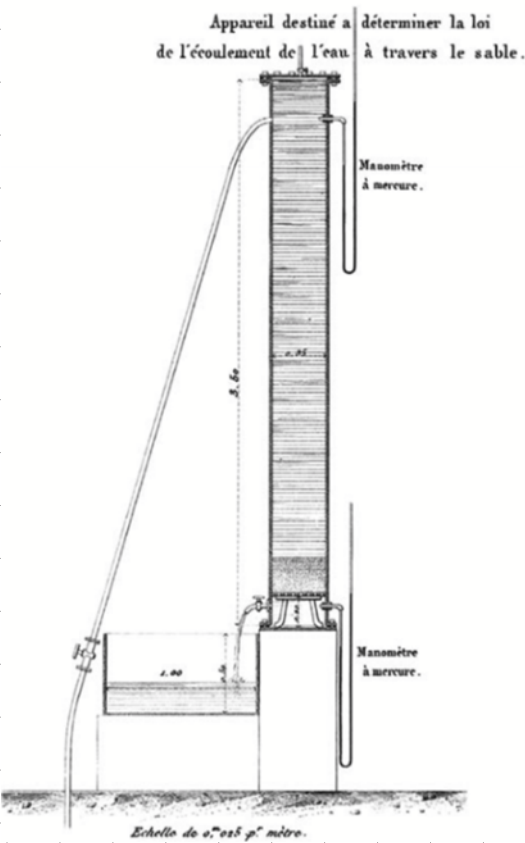
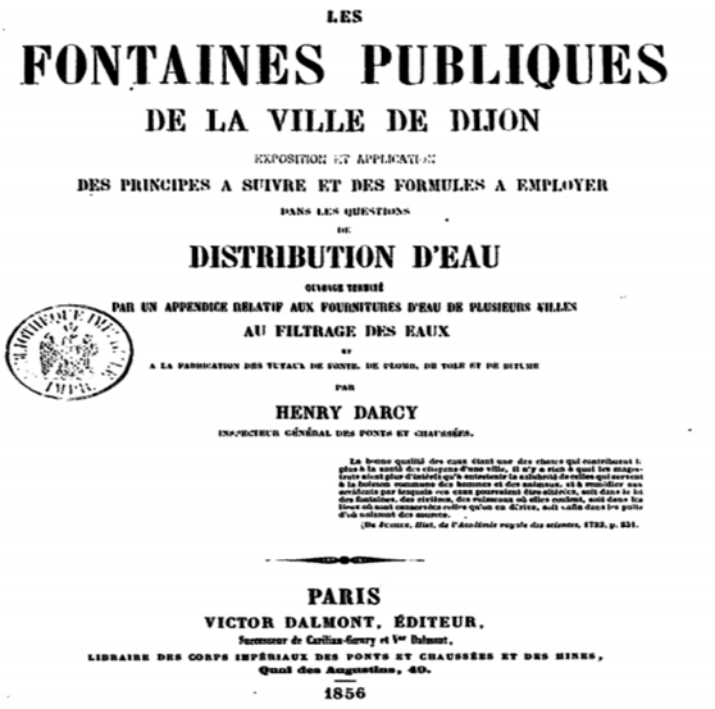
Darcy's law

$$v = \frac{k}{\mu} \cdot \frac{dp}{dr}$$





Dijon
1856 → Retired to Dijon
1858 → died



$$\left. \begin{matrix} ss \\ pss \end{matrix} \right\} \frac{\partial}{\partial t} = 0$$

$$v = \frac{k}{\mu} \frac{dp}{dr}$$

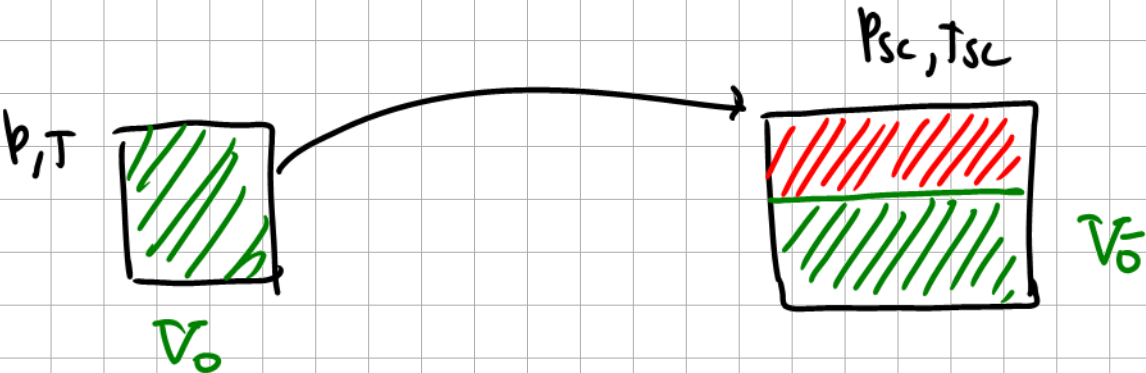
$$v \rightarrow q_o$$

$$v = \frac{q_o}{A} \rightarrow [m^3/d] \quad [m^3/s]$$

$A \sim 2\pi r h$

$$q_o \quad ? \quad q_o \rightarrow q_o$$

Black oil properties



oil volume factor

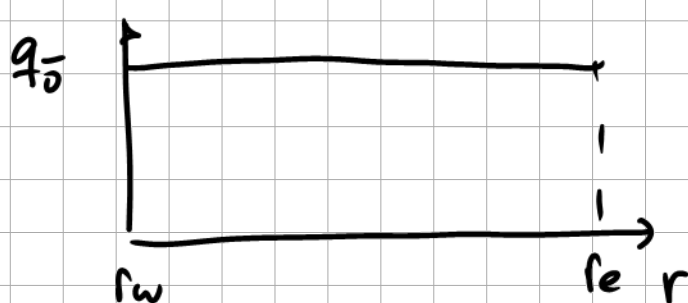
$$B_o(p,T) = \frac{V_o(p,T)}{V_o} > 1$$

$$q_o = B_o(p,T) \cdot q_o$$

$$B_o = [m^3/s^3]$$

$$v = \frac{q_o \cdot B_o}{2\pi r h} = \left(\frac{k}{\mu_o} \right) \frac{dp}{dr}$$

$$q_o = f(r)$$



$$q_o \neq f(r) \quad \left. \begin{array}{l} \\ \end{array} \right\} \text{SS}$$

$$\int_{r_w}^{r @ p_e} \frac{dr}{r} = \frac{2\pi K h}{q_o} \int_{p_w}^{p_e} \frac{dp}{B_o \mu_o}$$

for SS, $r @ p_e = 0.61 r_e$



$$p_e = \frac{\int_V p dv}{V}$$

$$\textcircled{1} \ln\left(\frac{0.61 r_e}{r_w}\right) = \ln(0.61) + \ln\left(\frac{r_e}{r_w}\right) = \ln\left(\frac{r_e}{r_w}\right) - 0.5$$

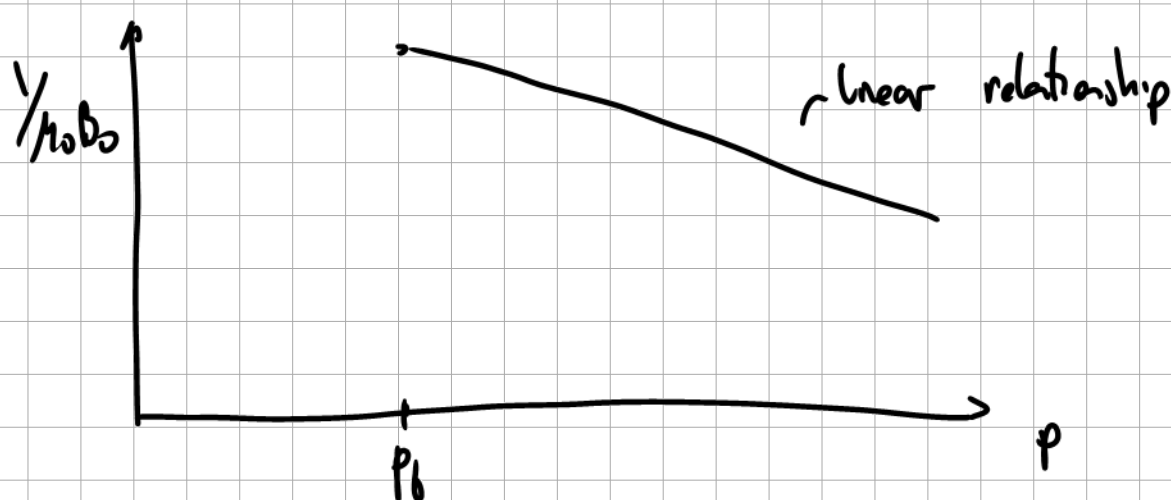
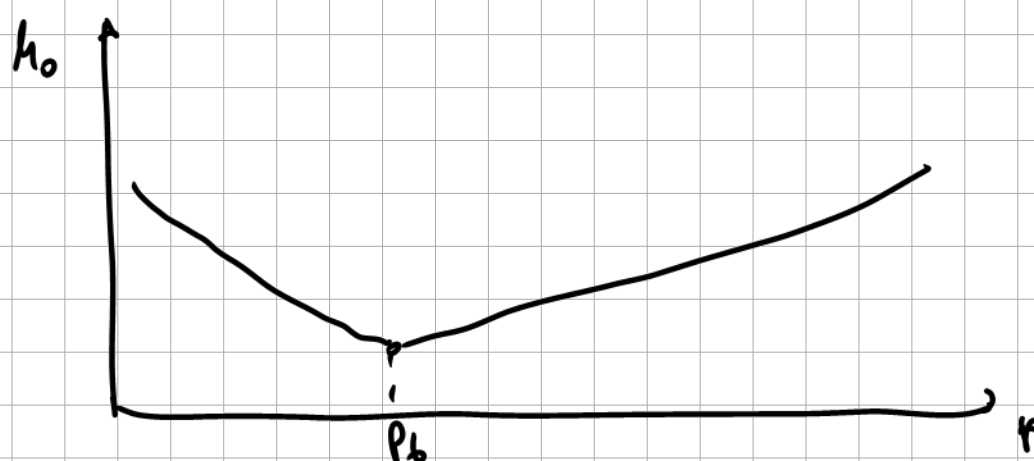
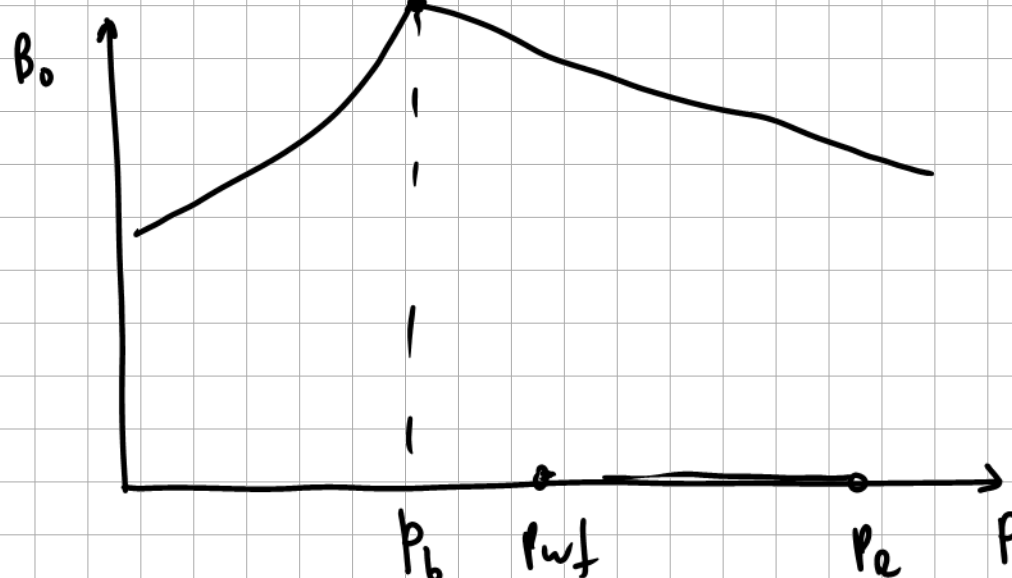
$$\textcircled{2} \int_{p_w}^{p_e} \frac{1}{\mu_o B_o} dp$$

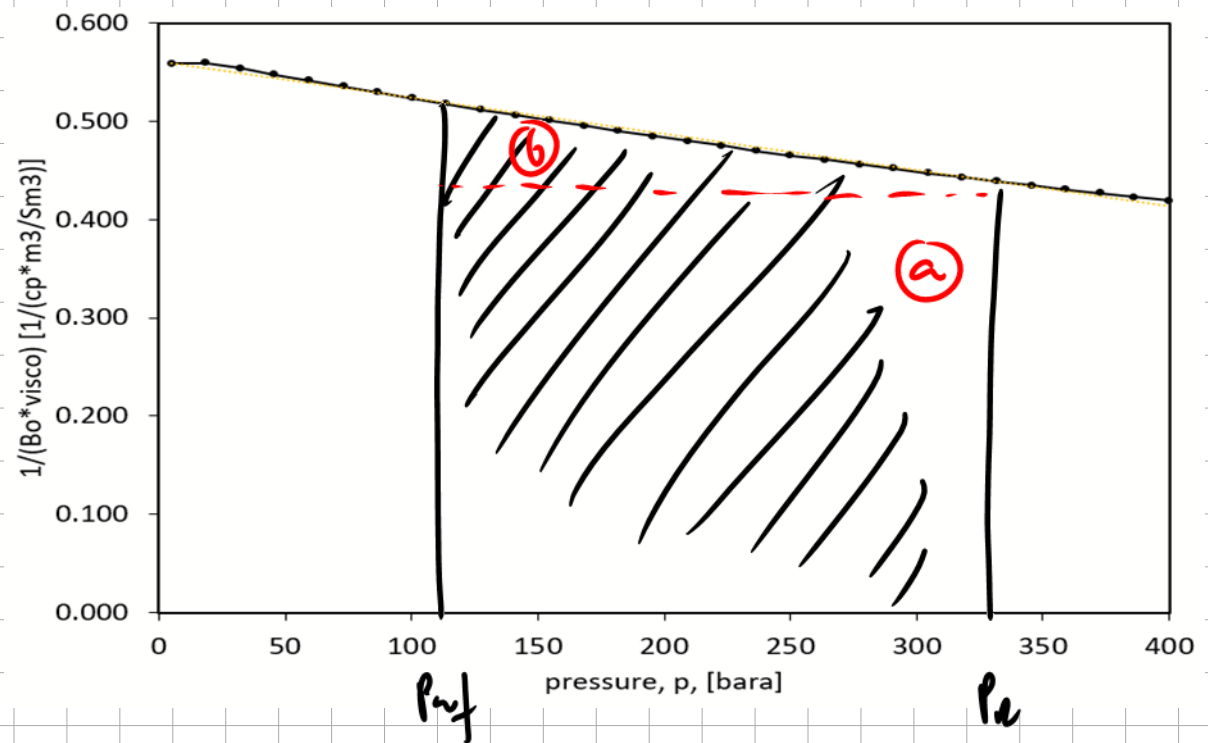
$$\mu_o = f_1(p, T)$$

$$B_o = f_2(p, T)$$

@ reservoir $T = \text{constant} = T_R$

sat \longleftrightarrow undersaturated





$$② \int_{p_{wf}}^{p_e} \frac{1}{\mu_o b_o} \cdot dp \approx (p_e - p_{wf}) \cdot \left[\frac{1}{\mu_o b_o} \right]_{p_{wf}}^{p_e} \cdot 0.5$$

$$\frac{1}{\mu_o b_o} \bigg|_{p_{av}} = \frac{(p_e + p_{wf})}{2}$$

$$② = \frac{(p_e - p_{wf})}{(\mu_o b_o)_{p_{av}}}$$

$$\ln\left(\frac{r_e}{r_w}\right) - 0.5 = \frac{2\pi K h}{q_o} \frac{(p_e - p_{wf})}{(\mu_o b_o)_{p_{av}}}$$

$$q_o = \frac{2\pi K h (p_e - p_{wf})}{(\mu_o b_o)_{p_{av}} \left[\ln\left(\frac{r_e}{r_w}\right) - 0.5 \right]}$$

$J \approx \text{constant}$