

Comments on Sec. 7.4.3 of Phase Behavior Monograph <sup>1/4</sup> regarding "MBO" SGD material balance by Gunnar Borthne.

$$V_b = 1 \text{ bbl}$$

$$V_p = \phi$$

$$V_{ncv} = \phi(1 - S_w) = V_{OR} + V_{GR}$$

The surface product volumes ( $V_b$  and  $V_g$ ) distributed between the two reservoir AC phases ( $S_o$  and  $S_g$ ) are given by

(@ any time):

$$A_o = N_R = V_o = \phi \left[ \frac{V_{oo}}{B_o} + \frac{S_g}{E_{gd}} r_s \right] = N - N_p$$

$$A_g = G_R = V_g = \phi \left[ \frac{S_o}{B_o} R_s + \frac{S_g}{E_{gd}} \right] = G - G_p$$

↑

Current in-place  
surface volumes  
after

$$N_R = N \quad @ \quad p_R = p_{Ri}$$

$$G_R = G \quad @ \quad p_R = p_{Ri}$$

Differential change in surface product volumes during a small pressure drop  $p_{Rk-1} \rightarrow p_{Rk}$ :

$$A_{ok-1} - A_{ok} = N_{Rk-1} - N_{Rk} = \Delta N_{Pk}$$

$$A_{gk-1} - A_{gk} = G_{Rk-1} - G_{Rk} = \Delta G_{Pk}$$

Instantaneous Producing GR Average over  $k-1 \rightarrow k$  period:

$$\bar{R}_{Pk} = \frac{\Delta G_{Pk}}{\Delta N_{Pk}} = \frac{\frac{1}{2}(E_{gk-1} + E_{gk})}{\frac{1}{2}(E_{ok-1} + E_{ok})} \quad ; \quad R_p = \frac{E_g}{E_o}$$

$$\bar{R}_{Pk} = \frac{1}{2}(R_{Pk-1} + R_{Pk}) = \frac{1}{2} \left( \frac{E_{gk-1}}{E_{ok-1}} + \frac{E_{gk}}{E_{ok}} \right)$$

< prove these give the same result >

CBW

# Oil Saturation Equation

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$$\phi \left[ \frac{S_o}{B_o} + \frac{S_g}{B_{gd}} r_s \right] = N - N_p$$

$$N = \phi (1 - S_w) / B_{oi}$$

$$S_g = (1 - S_w) - S_o$$

$$\frac{\phi \left[ \frac{S_o}{B_o} + \frac{(1 - S_w) - S_o}{B_{gd}} r_s \right]}{\phi (1 - S_w) / B_{oi}} = \frac{N - N_p}{N}$$

$$\frac{S_o}{(1 - S_w)} \left( \frac{B_{oi}}{B_o} - \frac{r_s}{B_{gd}} B_{oi} \right) + \frac{r_s}{B_{gd}} B_{oi} = 1 - \frac{N_p}{N}$$

$$S_o = (1 - S_w) \left[ \frac{\left(1 - \frac{N_p}{N}\right) - \frac{r_s}{B_{gd}} B_{oi}}{\frac{B_{oi}}{B_o} - \frac{r_s}{B_{gd}} B_{oi}} \right] \cdot \frac{B_o B_{gd}}{B_o B_{gd}}$$

$$S_o = (1 - S_w) \left[ \frac{\left(1 - \frac{N_p}{N}\right) B_o B_{gd} - r_s B_o B_{oi}}{B_{oi} (B_{gd} - r_s B_o)} \right]$$

Walsh Eq. 2

< What is the range of  $S_o$ ? Can be  $< 0$ ? Can be  $> 1 - S_w$ ? >

< Derive similar relation if initially only

Reservoir gas condensate:  $S_o = 0$ ,  $S_g = 1 - S_w$  @  $P_r = P_{ri}$

< Derive general relation if initially containing  
Reservoir Gas & Reservoir Oil:  $S_o > 0$ ,  $S_g > 0$  @  $P_r = P_{ri}$

$$N = \left[ \frac{S_{oi}}{B_{oi}} + \frac{S_{gi}}{B_{gdi}} r_{si} \right] \phi$$

elka

# Producing Gas-Oil Ratio Equation

$$R_p = \frac{q_{\bar{g}}}{q_o} = \frac{q_{\bar{g}g} + q_{\bar{g}o}}{q_{o0} + q_{og}}$$

$$R_s = \frac{q_{\bar{g}o}}{q_{o0}}, \quad r_s = \frac{q_{og}}{q_{\bar{g}g}}$$

$$q_{\bar{g}o} = R_s q_{o0}, \quad q_{og} = r_s q_{\bar{g}g}$$

$$R_p = \frac{q_{\bar{g}g} + R_s q_{o0}}{q_{o0} + r_s q_{\bar{g}g}}$$

$$q_{gr} = q_{\bar{g}g} B_{gd} = C \int_{P_{wf}}^{P_R} \frac{k_{rg}}{\mu_g B_{gd}} dp \approx C \left( \frac{k_{rg}}{\mu_g B_{gd}} \right) (P_R - P_{wf})$$

$\overline{\lambda_{\bar{g}}}$

$$q_{or} = q_{o0} B_o = C \int_{P_{wf}}^{P_R} \frac{k_{ro}}{\mu_o B_o} dp \approx C \left( \frac{k_{ro}}{\mu_o B_o} \right) (P_R - P_{wf})$$

$\overline{\lambda_o}$

< What are the "correct" averages of surface product mobilities  $\overline{\lambda_{\bar{g}}}$  and  $\overline{\lambda_o}$ ? >

$$R_p = \frac{\cancel{C \Delta P} \overline{\lambda_{\bar{g}}} \Delta P + \cancel{C \Delta P} \overline{\lambda_o} R_s}{\cancel{C \Delta P} \overline{\lambda_o} + \cancel{C \Delta P} \overline{\lambda_{\bar{g}}} r_s} \cdot \frac{\frac{1}{\overline{\lambda_o}}}{\frac{1}{\overline{\lambda_{\bar{g}}}}}$$

$$R_p = \frac{(\overline{\lambda_{\bar{g}}}/\overline{\lambda_o}) + R_s}{1 + (\overline{\lambda_{\bar{g}}}/\overline{\lambda_o})}$$

$$R_p = \frac{\left[ \frac{k_{rg}}{k_{ro}} \left( \frac{\mu_o B_o}{\mu_g B_{gd}} \right) + R_s \right]}{\left[ 1 + \frac{k_{rg}}{k_{ro}} \left( \frac{\mu_o B_o}{\mu_g B_{gd}} \right) r_s \right]} = \frac{[E_g]}{[E_o]} = \frac{\Delta G_p}{\Delta N_p}$$

Borthne nomenclature

# $\frac{k_{rg}}{k_{ro}}(p)$ Equation

$$\frac{k_{rg}}{k_{ro}} = f(R_p; P, T(p))$$

$$\frac{k_{rg}}{k_{ro}}(p) = \frac{\mu_g \beta_{gd}}{\mu_o \beta_o} \left( \frac{R_p - R_s}{1 - r_s R_p} \right)$$

where  $\mu(p)$ ,  $\beta(p)$ ,  $R_s^{(p)}$  &  $r_s(p)$

The  $R_p$  eq. and the  $k_{rg}/k_{ro}$  eq. are only valid ~~at~~ in the reservoir where "steady state" flow exists, meaning that the flowing mixture has a GOR =  $R_p$ .

- For SGD oil reservoirs, Muskat shows that the SS flow assumption is valid throughout the drainage volume  $r_w < r < r_e$ .
- For Gas Condensates, Fevang (and Whitson) show that the SS flow assumption is only valid from  $p_{wf} < p < p^*$  where  $p^* = p_d$  of the produced wellstream.