

PHASE EQUILIBRIUM (K-values)

K_i Equilibrium Ratios

Note Title

2013-09-06

GAS-OIL

Molar Compositions



(P, T)

$$n_g \quad y_i = \frac{n_{i,g}}{n_g}$$

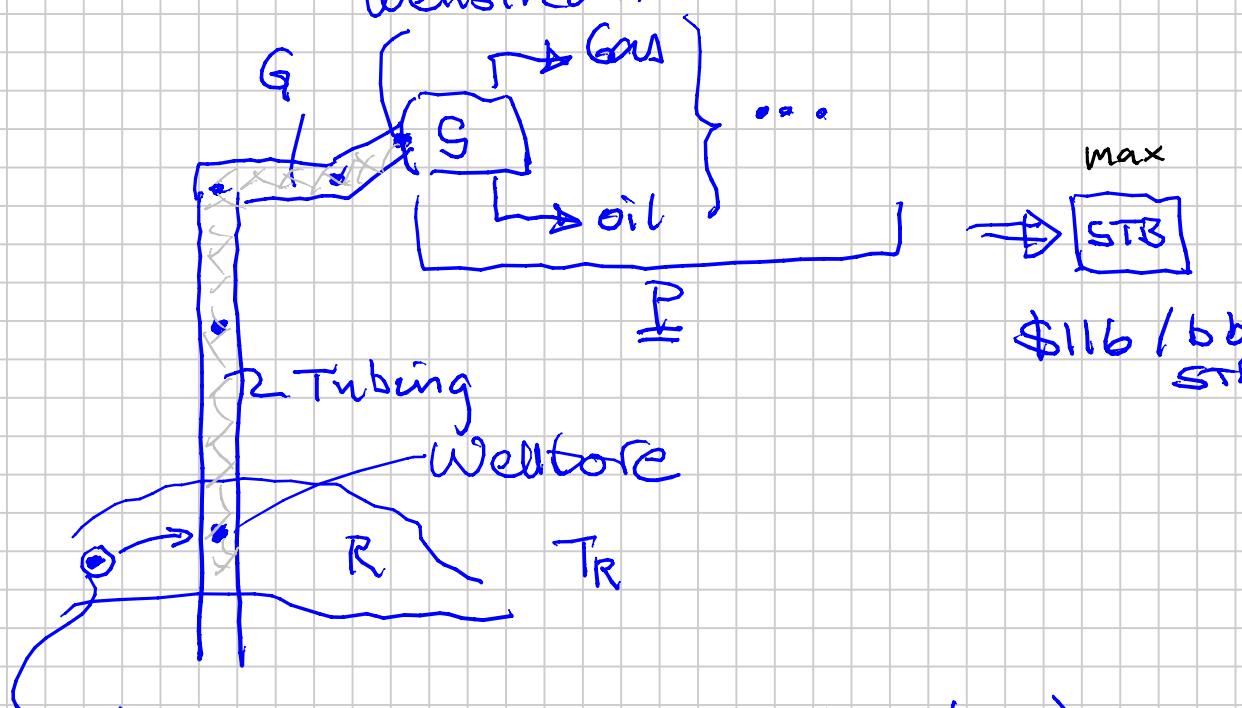
$$n_o \quad x_i = \frac{n_{i,o}}{n_o}$$

$$K_i \equiv \frac{y_i}{x_i}$$

$$K_i(p, T, \bar{z})$$

Know @ Reservoir, Production Pipe,
Surface Gathering Lines,
Separator Unit

"Wellstream"



In-Situ Reservoir \neq Wellstream (Wellbore)

Behavior of K_i

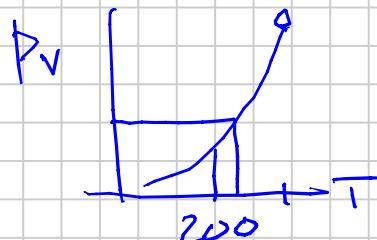
K_i represents (in lay terms) the relative preference of component i to "be" in the gas phase or oil phase:

$$K_i > 1$$

$$K_i < 1$$

We can make more money by selling component i as part of the liquid phase
([↑] ultimate processed surface)

5-10 times the value



$$@P_v(T)$$



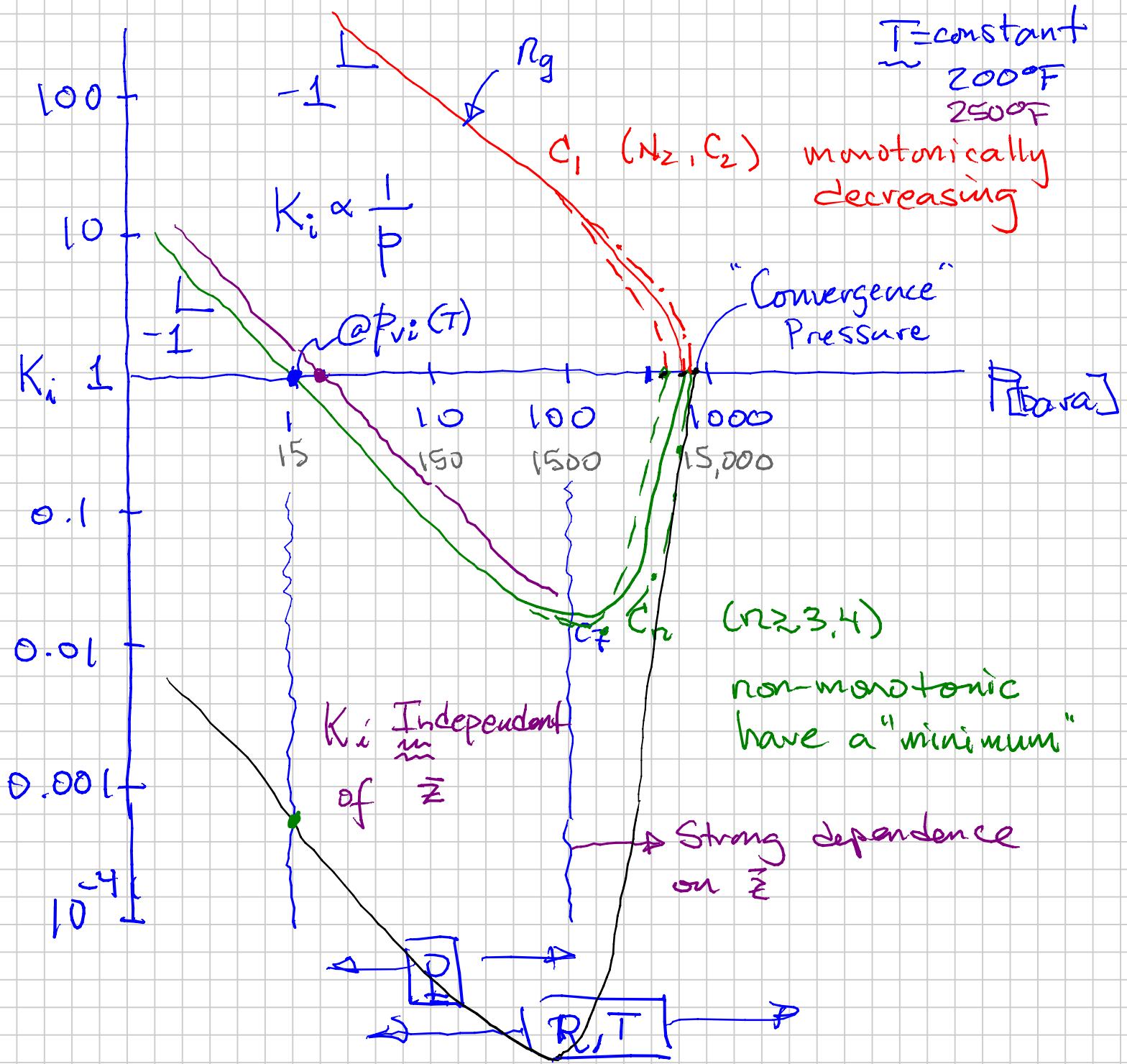
$$K_{H_2O} = \frac{1}{1} = 1$$

100°C

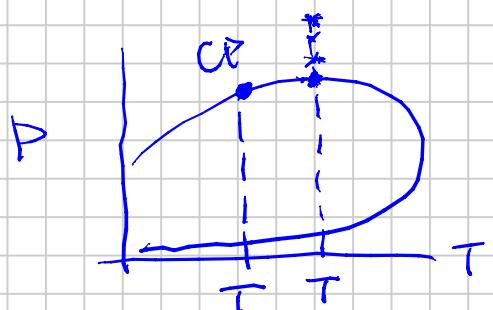
1 atm

$$P_{v,i}(T) \Rightarrow K_i \quad (P \leq 100 \text{ bara}, T)$$

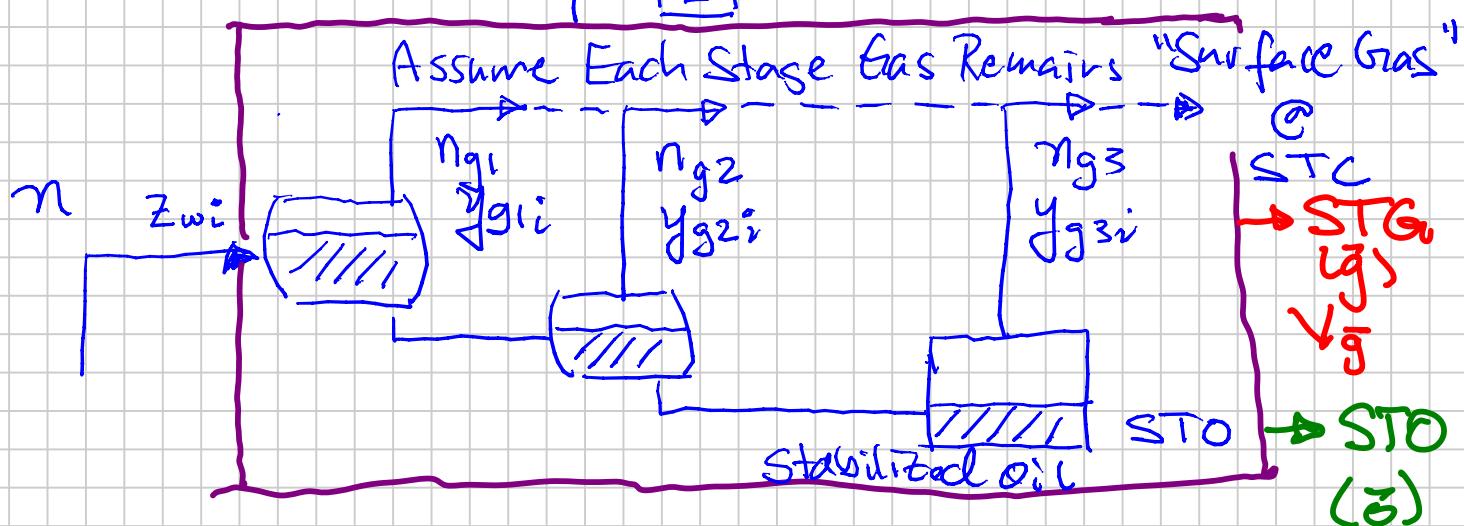
$$K_i = \frac{P_{v,i}(T)}{P}$$



$K_{i\min}$ @ $\sim 50-120$ bara



SURFACE PROCESSING "P"



$$\begin{array}{c}
 \text{Stage 1} \quad \text{Stage 2} \quad \text{Stage N} \\
 \left\{ \begin{array}{l} P_{sp1} \\ T_{sp1} \end{array} \right\} \quad \left\{ \begin{array}{l} P_{sp2} \\ T_{sp2} \end{array} \right\} \quad \left\{ \begin{array}{l} P_{sp3} \\ T_{sp3} \end{array} \right\} \\
 K_{1i}(P_i, T) \quad K_{2i}(P_i, T) \quad K_{3i}(P_i, T)
 \end{array}$$

Stage N

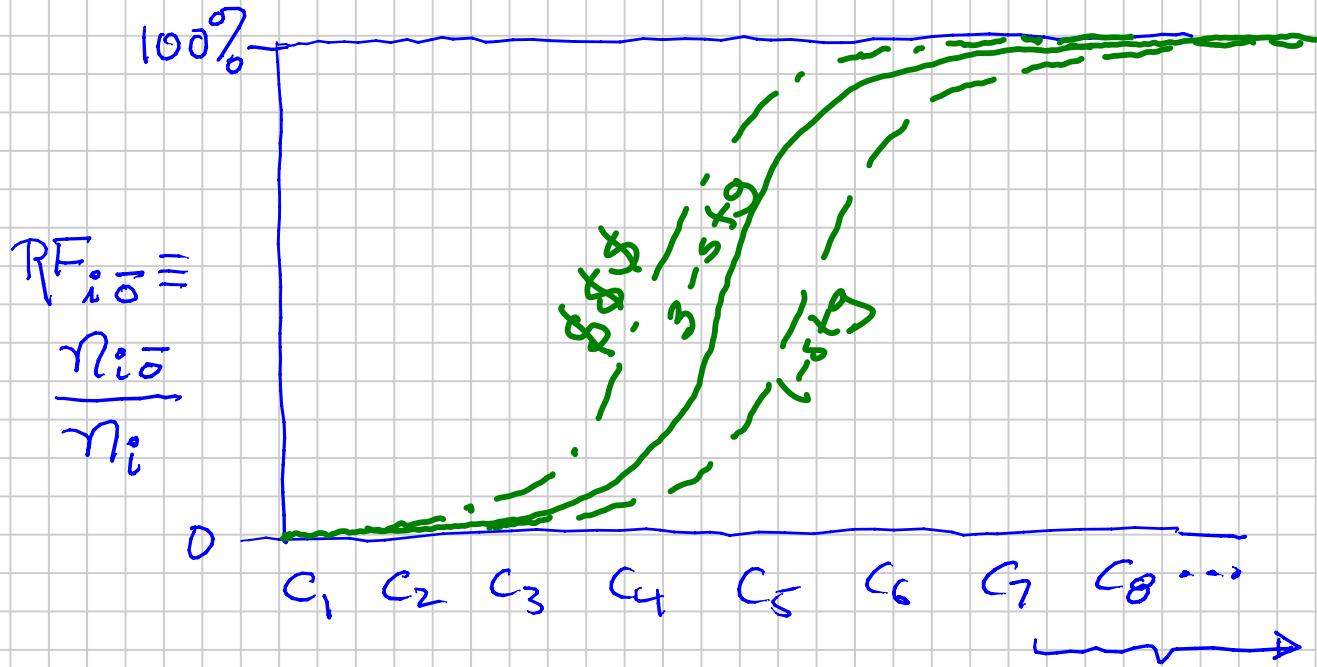
$$\left\{ \begin{array}{l} P_{sp3} \\ T_{sp3} \end{array} \right\}$$

$$\begin{array}{c}
 V_0 \\
 \text{max} \\
 \{ n_0 \}
 \end{array}$$

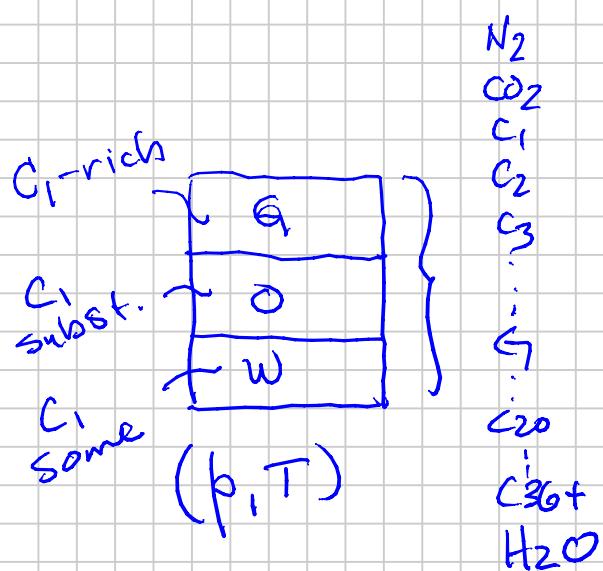
Controls the ultimate MOLES of $i \Rightarrow \text{STO}$

$$\begin{aligned}
 K_i &\rightarrow K_i \\
 &\downarrow R_{all} \\
 n_{ig} &= (n_g) \cdot y_i \\
 &\uparrow \text{max} \quad \uparrow \text{max } K_i \\
 V_0 &\propto \left(1 - \sum_{k=1}^3 n_{ik} \right)
 \end{aligned}$$

1949



Water-Gas-Oil Phase Equilibria



- Pore In-Situ
- Production Pipes
- Separator
- Ocean (Leakage, Blowout)

In general

$$\text{Gas-Oil } K_i(p, T, \bar{z}) \approx K_i(p, T, \bar{z}^*)$$

↑
No H₂O

Rigorous

H₂O
Included

Engineering guideline

⇒ We can ignore H₂O component and aqueous phase when doing gas-oil phase equilibria calculations.

$$K_{wg_i} = \frac{y_i}{x_{wi}} \stackrel{i}{\gg} 1$$

all i except H₂O

$$K_{wo_i} = \frac{x_i}{x_{wi}} \stackrel{i}{\gg} 1$$

Limited Solubility
in the Aqueous Phase

$$\stackrel{i}{\ll} 1 \quad \text{for H}_2\text{O} \Rightarrow$$

CO₂

Methane

:

HCS

Decreasing
Solubility

$$K_{wgC_1} < K_{wgC_2}$$

H₂O - G - O

When is solubility important?

① Gas production \Rightarrow water production

0.1-5 mol-% wellstream H₂O



- T_R $\geq 300^{\circ}\text{F}$

- P_{wf} < 500 psia

② When oil & gas "sees" (mixes) with larger amounts of water that has not yet equilibrated ("seen") oil & gas yet.

- Injecting water (water flood)
- Offshore blowout situations

- Active Aquifer

