**Solution proposal Exercise 3**

**Task 1**

In the compendium is shown that to obtain equal pressure drop in gas- and liquid channels, the following must be fulfilled:

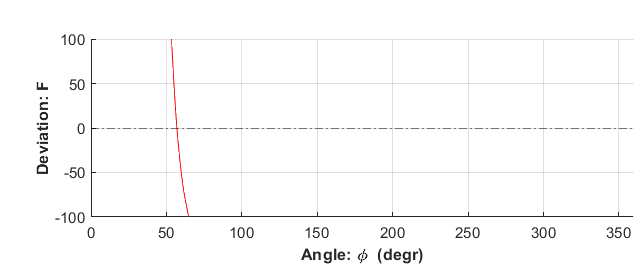
 (2-11)

Shear tensions, wetted surfaces and liquid- and gas-filled areas can all be related to flow rates and opening angle: .

F( ) is calculated by: funF, script attached. The angle that come closest to: F=0 is used, done by script Oving 3, attached. (This is a crude approach, more robust than gradient searches.)

1. **Liquid layer heigh : horizontal pipe**

The figure below illustrates: F as function of opening angle, showing that F=0 is fulfilled for opening angle a bit above 50o.

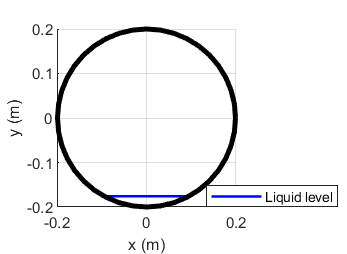


Print-out from the script:

Angle estimate: 56.9369 (degr) Remaining error: F=0.68365(Pa/m)

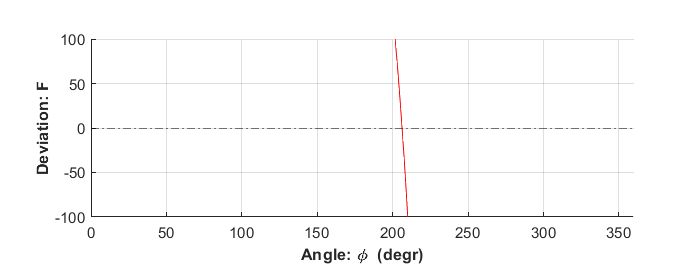
Liquid level height: hl: 0.024184 (m)

The figure below(made by the script) illustrates liquid level for assumed stratified flow.



1. **Liquid layer heigh : upward sloping pipe**

The figure below shows that F=0 is fulfilled for opening angle a bit above 200o.

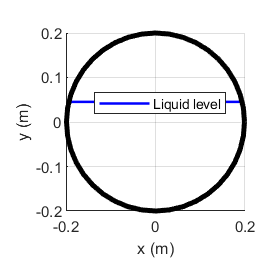


Print-out from the script:

Angle estimate: 206.1261 (degr) Remaining error: F=2.7804(Pa/m)

Liquid level height: hl: 0.2452 (m)

The figure below illustrates liquid level calculated.



**Scripts Task 1**

% Exercise 3

clear

clf

r=0.2;

A=pi\*r^2;

vsg=3;

lam=0.01;

vsl=vsg\*lam/(1-lam);

rhl=900;

rhg=100;

slope=0; % pipe slope

g=9.81;

gx=g\*sind(slope);

% calculate F

minang=0;

maxang=360;

nr=1000;

oangle=linspace(minang,maxang,nr)\*pi/180; % opening angle range: [ minang,maxang]

for i=1:nr

[Sg(i),Sl(i),Si(i),taug(i),taul(i),taui(i),yl(i),hl(i),F(i)] = funF(oangle(i),r,rhg,rhl,vsg,vsl,gx);

Fo(i)=0;

end

% pick index "m" making F closest to zero

[Fm,m]=min(abs(F));

[Sgm,Slm,Sim,taugm,taulm,tauim,ylm,hlm,Fm] = funF(oangle(m),r,rhg,rhl,vsg,vsl,gx);

oam=oangle(m);

disp(['Angle estimate: ',num2str(oangle(m)\*180/pi),' (degr) Remaining error: F=',num2str(Fm),'(Pa/m)'])

disp([' Liquid level height: hl: ',num2str(hl(m)), ' (m)'])

subplot(2,1,1)

hold on

plot(oangle\*180/pi,F,'r-')

plot(oangle\*180/pi,Fo,'k-.')

hold off

axis([minang,maxang,-100,100]);

grid

xlabel('\bf Angle: \phi (degr) ')

ylabel('\bf Deviation: F ')

% Illustration

t=0:pi/20:2\*pi;

subplot(2,1,2)

hold on

plot([-Sim/2,Sim/2],[-r+hlm,-r+hlm],'b-','LineWidth',1.5)

plot(r\*cos(t),r\*sin(t),'k-','LineWidth',3)

hold off

axis square

legend('Liquid level')

xlabel('x (m)')

ylabel('y (m)')

grid

function [Sg,Sl,Si,taug,taul,taui,yl,hl,F] = funF(oangle,r,rhg,rhl,vsg,vsl,gx)

%

fg=0.02;

fi=0.04;

fl=0.012;

% oangle: opening angle

hl=r-r\*cos(oangle/2);

Si=2\*r\*sin(oangle/2);

Sl=oangle\*r;

Sg=r\*(2\*pi-oangle);

yl=1/pi\*(oangle/2-cos(oangle/2)\*sin(oangle/2));

yg=1-yl;

vg=vsg/yg;

vl=vsl/yl;

taui=1/8\*fi\*rhg\*(vg-vl)\*abs(vg-vl);

taug=1/8\*fg\*rhg\*vg^2;

taul=1/8\*fl\*rhl\*vl^2;

F=(rhl-rhg)\*gx+(taul\*Sl-taui\*Si)/(yl\*pi\*r^2)-(taug\*Sg+taui\*Si)/(yg\*pi\*r^2);

end

**Task 2**

Pressure gradient in the gas channel was expressed

 (2-12)

(Pressure loss in the liquid channel will be the same, assumed for the calculation of : F=0)

Acceleration due to gas expansion when pressure drops will be small and has here been neglected, assuming constant superficial velocities. This simplifies the gradient



The variables needed have already been computed. So pressure drop calculation may made by adding the following lines to the script “Exercise 3” above.

% Pressure loss

L=15000; % length of pipe section

disp(['Length : ',num2str(L),' m Slope:',num2str(slope),' degr'])

Ag=(1-ylm)\*pi\*r^2;

dpdx=rhg\*gx+(taugm\*Sgm+tauim\*Sim)/Ag; % gradient

disp(['Gradient: ',num2str(dpdx),' Pa/m'])

disp(['Pressure drop: ',num2str(dpdx\*L\*1e-5),' bar'])

1. **Pressure drop along the horizontal section**

Print-out:

Length : 15000 m Slope:0 degr

Gradient: 23.0934 Pa/m

Pressure drop: 3.464 bar

1. **Pressure drop the upward sloping section**

Print-out:

Length : 5000 m Slope:5 degr

Gradient: 598.6193 Pa/m

Pressure drop: 29.931 bar

1. **Discussion**

For the horizontal section, low liquid level is estimated. The assumption of stratified flow do not appear unreasonable. Thus, the pressure loss prediction seems not to violate basic assumption. (Stability predictions may be made and friction factor estimates may be considered with sound suspicion)

For the upwardly slowing section, high liquid level was estimated. This reduces the gas filled area causing higher gas velocity and lower liquid velocity. It seems doubtful that stratified flow is maintained. (Stability predictions will probably verify this). Thus, pressure loss prediction assuming stratified flow should not be trusted if the flow is not stratified.