Technology used to Quantify Oil Released in Deepwater Horizon (Macondo) Blowout

Curtis Hays Whitson

Professor (reservoir engineering) Institutt for petroleumsteknologi (IPT), NTNU

> March 25, 2014 NTVA Trondheim Section



Deepwater Horizon Blowout



About me

- Born & raised: Oklahoma, USA
- BSc: Stanford U. (1978)
- Arrived Trondheim Aug. 1978
- Taught 1st NTH course, 1980.
- NAVF Research scholarship, 1980-83.
- Dr.techn. NTH, 1984
- Professor, NTH, 1985-90, 1992-present
- Thermodynamics & flow of petroleum reservoir fluids.

About the Lecture

- April 20, 2010: Macondo (Deepwater Horizon) blowout.
 - Eleven workers die.
 - 3-5 million barrels stock-tank oil (STO) released into Gulf of Mexico during a period of 87 days.
- July 15, 2010: Macondo blowout stopped.
- Jan. 2012 I was engaged by BP as a technical expert.
 - Provided comprehensive fluid analysis and PVT models.
 - Analysis used in quantifying amount of STO released.
 - Oct. 14, 2013: Provided testimony (2 hours) to the U.S. District Court in New Orleans, Judge Carl Barbier presiding.

DEEPWATER HORIZON VICTIMS

Jason C. Anderson, 35. Midfleid, Texas. father of two

Aaron Dale Burkeen, 37. Philadelphia, Miss., married, father of two (14-year-old daughter Aryn and 6-year-old son Timothy), died four days before his 38th birthday

Donald Clark, 49, Newellton, La., married to Shella Clark

Stephen Ray Curtis, 39, Georgetown, La., married and had two teenagers. Taught his son to funt and play baseball and was active church

Roy VVyatt Kemp, 27, Jonesville, La., married to Courtney Kemp.

Karl D. Kleppinger Jr., 38, Natchez, Miss., U.S. Army veteran of Operation Desert Storm, enloyed NASCAR and cooking barbecue. Married with one son. Aaron

Gordon L. Jones, 28, Baton Rouge, Wife Michelle Jones was hine months pregnant with their second son when he died.

Keith Blair Manuel, 56, Gonzales, La., father of three (Kelli Taquino, Jessica Manchester and Ashley Jo Manuel). Engaged to Melinda Becnel. Had season tickets to Louisiana State University baseball and football games.

Dewey A. Revette, 48, State Line, Miss., married with two daughters. Had been with Transocean for 29 years.

Shane M. Roshto, 22, Liberty, Miss., married to Natalle Roshto, father of 3-year-old Blain Michael

Adam Weise, 24, Yorktown, Texas. During time off, the former high school football hunted deer and fished from his boat

Adam

Jason

March 27, 1980

123 (workers) died

Aleksander L. Kielland drilling rig collapse

(owned by Stavanger Drilling Company)

Aaron

Donald

Stephen

Roy

Keith

Dewey

Shane

Karl

Gordon





Why Quantify Barrels Oil Released?

- USA Cleanwater Act Section 311.
- Penalty: \$1,100 \$4,300 per barrel of oil at stock tank conditions.
 - Released into federal waters.
 - \$1,100: "accidents do happen" (no negligence)
 - \$4,300: if gross negligence found
- Estimated release 3.2–5.0 million stock-tank oil barrels.
- Range of possible penalty: ~4-20 billion USD (25-125 millard NOK).
- Penalty revenue distributed between states and federal governments.





Judge Carl Barbier United States District Court for the Eastern District of Louisiana Appointed by President Bill Clinton, 1998.





How to Quantify Barrels Oil Released?

- Technical experts hired.
 - US Government.
 - BP (& Anadarko)
 - Halliburton
- Data made available.
 - Geology.
 - Rock properties.
 - Fluid properties.
 - Pressures, volumetric rates.
 - Massive number of reports related to blowout.



Prof. Martin Blunt Stanford U. (previously) Imperial College (currently) PhD, Cambridge (Physics) BP Expert



Prof. Robert Zimmerman Imperial College PhD, UC Berley (Rock Mechnics) BP Expert



Prof. Alain Gringarten Imperial College PhD, Stanford U. (Petroleum Eng.) BP Expert



Dr. Robert Mott MA Mathematics, Cambridge U. PhD, London U. (Physics) BP expert **(working with me)**

... and many others



Prof. Leif Larsen Prof. II, U. Stavanger PhD, UC Irvine (Mathematics) US Government expert

How to Quantify Barrels Oil Released?

- Fundamental engineering principles.
 - Volumetric material balance.
 - Initial volume containing reservoir hydrocarbons (V_{Ri}).
 - Shrinkage of reservoir volume to oil volume at stock tank conditions (S).
 - Pore volume compressibility (c_p).
 - Fluid compressibility (c_f).
 - Initial reservoir pressure (p_{Ri}).
 - Final producing rate prior to end of blowout (q_f).
 - Hydrostatic pressure conversion.
 - Surface pressures measured after blowout (p_s(t)).
 - Density spatial and time variations ($\rho(z,t)$).
 - Thermal convection in wellbore after blowout (T(z,t)).
 - Darcy flow in porous media.
 - Final reservoir pressure after blowout (p_{Rf}) by model extrapolation.





Volumetric Material Balance

$$c_R = -\frac{1}{V_R} \frac{dV_R}{dp_R} = \text{constant}$$

$$c_{R} = c_{pore} + c_{fluid} = \text{constant}$$
$$\Delta V_{p} = V_{Ri} \cdot c_{R} \cdot \Delta p$$
$$\Delta p = p_{Ri} - p_{Rf}$$



Shrinkage Factor

- Reservoir fluid produced must be expressed as a stock-tank oil (STO) volume, to levy the Clean Water Act penalty.
- The term "shrinkage factor" (SF) is used to describe the ratio of STO volume to the reservoir volume from which it comes.
 - For example, taking all of the original reservoir fluid at initial pressure (V_{Ri}) to surface (stock tank) conditions, the resulting STO volume would be N, and "initial" SF_i is:
 - $SF_i = N / V_{Ri}$ or $N = V_{Ri} SF_i$
 - Likewise, taking all of the produced reservoir fluid during the blowout (ΔV_p) to surface (stock tank) conditions, the resulting STO volume would be N_p and "final" SF_f is:
 - $SF_f = N_p / \Delta V_p$ or $N_p = \Delta V_p SF_f$

Material Balance Equation

 Rewriting the volumetric material balance in terms of stock tank oil volumes,

Reservoir Pressure After Blowout

• Hydrostatic Pressure Conversion.

$$p_w(t) = p_{cs}(t) + g \int_{s}^{w} \rho(T(z,t), p(z,t)) dz$$

• Thermal convection in wellbore after blowout ceased (T(z,t)).



$$\frac{1}{r}\frac{\partial}{\partial r}\left(r\frac{\partial T}{\partial r}\right) = \alpha_T \frac{\partial T}{\partial t}$$

$$\frac{1}{\alpha_T} = \frac{\kappa_s}{\Gamma_T} = \frac{\kappa_s}{\phi \rho_w C_w + (1 - \phi) \rho_s C_s}$$

Thermal Convection



Figure B.5. Predicted temperatures at the well-bore as a function of depth, at different times. To a good approximation, at any given time the temperature varies linearly with depth from some (decreasing) value at the sea bed to 243°F at the reservoir. After around 1 day (100,000 s) we see the onset of convective mixing. This may locally distort the temperature profiles, giving regions of constant temperature with depth. However, conservation of energy prevents the average temperatures varying significantly from what is shown here.

Reservoir Pressure After Blowout

• Hydrostatic Pressure Conversion.

$$p_w(t) = p_{cs}(t) + \int_{s}^{w} \rho(T(z,t), p(z,t)) dz$$

• Empirical equation derived, based on rigorous solution:

$$p_w = p_{cs} + 3210 + \frac{7}{120}(p_{cs} - 6600) + \frac{5}{4} \left[8 + 55.7 \log_{10} \left(\frac{\Delta t}{100,000} \right) \right]$$

Reservoir Pressure After Blowout

- Interpret p_w(t) with analytical flow model with several unknown parameters, including final reservoir pressure after infinite shut-in time (following blowout).
 - Use a least-squares model regression with pressures and pressure derivatives as data.

$$0 = \sum_{i=1}^{n} w_i \left(p_i - p_t(t_i) \right)^2 + \sum_{i=2}^{n-1} w_i \left(\frac{p_{i+1} - p_{i-1}}{\ln(t_{i+1}) - \ln(t_{i+1})} - \frac{dp_t}{d\ln(t)} \Big|_{t_i} \right)^2$$

D.1. Parameter matches, sensitivities and model comparisons

D.1.1 Definitions and best-match values. Table D.1 summarizes the properties that we can derive from the pressure analysis. They are all introduced in Appendix C. Table D.2 provides my values of these properties using the methods presented in Appendices C and E and Section 4.3.

Parameter	Defining equation	Meaning	Found from
η	μQ_0	Draw-down in radial flow. Uses height	Value of pressure
	$\eta = \frac{1}{4\pi Kh}$	h at the well (93 ft), and final flow	derivative
	(C.11)	rate.	
τ_w	αW^2	Time for pressure to see channel	End of radial flow
	$\tau_W = \frac{16}{16}$	width	regime
	(C.15)		
τ1	$\tau_1 = \alpha L_1^2$	Time for pressure to reach channel	Match to channel flow
	(C.59)	end	pressure build-up
τ2	$\tau_2 = \alpha L_2^2$	Time for pressure to reach the other	Match to channel flow
	(C.59)	channel end	pressure build-up
β	$\beta = \frac{2\mu Q_o}{2\mu Q_o}$	Draw-down in linear flow	Slope of channel flow
	$\rho = KhW\sqrt{\pi\alpha}$		pressure regime
	$= \frac{\mu Q_o}{\mu Q_o}$		
	$2\sqrt{\pi\tau_W}Kh$		
	(C.38)		
Δp	Δp	Pressure decline	Final stabilized
	$\sqrt{\pi}$ β		pressure
	$=\frac{1}{2}\frac{1}{(\sqrt{\tau_1}+\sqrt{\tau_2})}t_p$		
	(C.66)		



Flow Rate Variation in Time

- US government claims that the final rate was the culmination of a continuously, monotonically decreasing rate from the onset of the blowout.
 - This would assume unchanged flow resistance in the pipes to the discharge point at the seabed.
 - BP argues that erosion continuously changed pipe flow conditions, with rate increasing gradually as erosion "cleaned" the flow path, then eventually reached a condition with stable pipeflow resistance and a rate that declined naturally because of declining reservoir pressure.
 - The material balance method is independent of the rate-time history, only dependent on the cumulative production at the end of the blowout.
 - Only the flow model used to estimate final reservoir pressure depends on the flow rate – and only at the end of the blowout (measured).







Macondo Fluid Issues

- A complex, near-critical reservoir fluid with unusual critical behavior over a wide range of temperatures.
- Four accurate reservoir fluid samples collected.
 - Two samples exhibit dewpoints over the entire range of temperature from 100-243°F.
 - Two samples exhibit bubblepoints over the entire range of temperature from 100-243°F.
- Near-critical behavior only important in two-phase region, i.e. flowing in pipe during blowout.

Near-Critical Fluid Behavior at All Temperatures (100-243°F)





Figure 4. Experimental data and EOS results for CL 68379, relative liquid volume in CCE at 100 F.







Figure 10. Experimental data and EOS results for Intertek, relative liquid volume in CCE at 100 F.





Conversion to Stock Tank Barrels

- Estimated quantities of reservoir fluid released also require PVT to convert to stock tank oil barrels.
- Shrinkage Factor:
 Final stock tank oil volume

Reservoir fluid volume

• Can be very dependent on process going from reservoir to stock-tank conditions.

SF expressed as a % (=STB per 100 initial reservoir barrels).

Sources of Shrinkage Factors

 Measured by three independent laboratories on four samples

- 1-Stage Separator Process (43 STB/bbl)

- 4-Stage Separator Process (47 STB/bbl)

Calculated by EOS model

- Oceanic Process (~43 STB/bbl)

- 130 stages.
- Water solubility & Mixing Assumptions