

$$\ln \frac{f}{p} = \ln \phi = Z - 1 - \ln(Z - B)$$

$$- \frac{A}{2\sqrt{2}B} \ln \left[\frac{Z + (1 + \sqrt{2})B}{Z + (1 - \sqrt{2})B} \right]$$

Ch. 4

and $\ln \frac{f_i}{y_i p} = \ln \phi_i = \frac{B_i}{B} (Z - 1) - \ln(Z - B)$

$$+ \frac{A}{2\sqrt{2}B} \left(\frac{B_i}{B} - \frac{2}{A} \sum_{j=1}^N y_j A_{ij} \right) \ln \left[\frac{Z + (1 + \sqrt{2})B}{Z + (1 - \sqrt{2})B} \right]$$

..... (4.23)

$$\ln \phi_1^L = \frac{b_1}{b^L} (Z^L - 1) - \ln(Z^L - B^L) - \frac{A^L}{2\sqrt{2} B^L}$$

$$\left(\frac{2(x_1 a_{11} + x_2 a_{12})}{a^L} - \frac{b_1}{b^L} \right) \ln \left[\frac{Z^L + (1 + \sqrt{2})B^L}{Z^L + (1 - \sqrt{2})B^L} \right] \quad (8-12.28a)$$

Pransnitz

f ✓

PSU

Pure Substance

$$\ln \phi = Z - 1 - \ln(Z - B) - \frac{A}{2\sqrt{2}B} \ln \frac{Z + (1 + \sqrt{2})B}{Z + (1 - \sqrt{2})B} \quad (16.44)$$

Mixtures

$$\ln \phi_i = (BB)_i (Z - 1) - \ln(Z - B) - \frac{A}{2\sqrt{2}B} ((AA)_i - (BB)_i) \ln \left[\frac{Z + (\sqrt{2} + 1)B}{Z - (\sqrt{2} - 1)B} \right]$$

(16.45)

TERNARY Problem 18 $C_1 - n - C_2 - n - C_{10}$

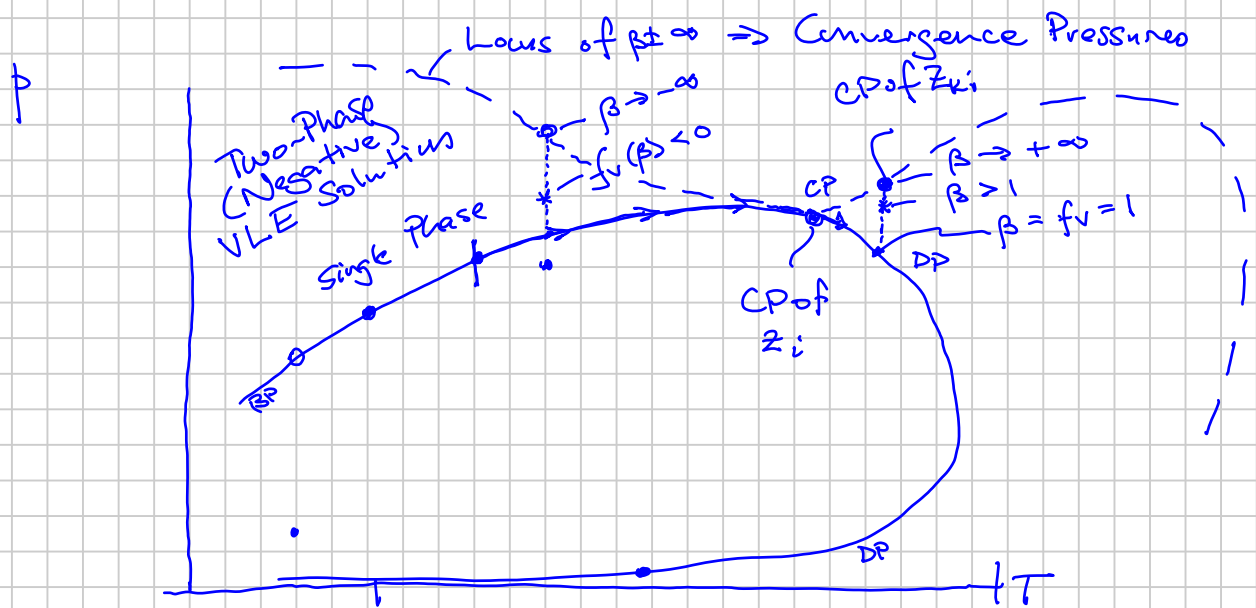
BPS: $k_{ij} \quad C_1 - C_{10} = 0$ in the problem

Any effect on VLE $k_{FC0} = 0$
 $= 0.05$ (Chueh) ?

(1) At 500 psia same effect on all 3 components
 mostly C_1 & C_{10} , little C_4
 10%

(2) At low p (15 & 0.15 psia) same result
 except no effect on C_4 & C_{10}
 10%

What about near critical condition?



$$z_i = \beta y_i + (1 - \beta) x_i$$

$$\beta \rightarrow \pm \infty, \quad y_i \rightarrow x_i \Rightarrow z_{k_i} \neq z_i$$

Convergence

VLE (Vapor-Liquid Equilibria) Calculations

• Flash Calculation

- Specify z_i, p, T

- Determine: (1) # Phases [2 or 1 | ...]

(2) Phase Amounts (molar) f_v, F_v, F_g, β

(3) Equilibrium molar compositions y_i, x_i

- Level of Difficulty finding the thermodynamically-correct answer

99% { (i) Easy at low p (≤ 1000 psia)
(ii) Challenge
1% (*) Very difficult - near critical point

- (RR/MM): Some extreme low- p calculations

$$z_i \rightarrow \epsilon$$

$$K_i \rightarrow \epsilon \text{ or } 1/\epsilon$$

- More than 2-phase solutions

• Saturation Pressure: Orientation "Data" 1-phase

2-phase Type:
BP: y_i
DP: x_i

- Specify: z_i, T

- Calculate: $\underline{p_s}$, incipient phase compositions

- Special case of Flash where $f_v \rightarrow \begin{matrix} 1-\epsilon \\ 0 \end{matrix} \epsilon$

- Level of Difficulty

✓ • Easy for lower dewpoints (usually)

✓ • Difficult many cases - mostly not knowing if a solution exists

✓ • Very Challenging near critical point

• Phase Stability Test (Gibbs)

- Given z_i P T

- Calculate - Will a new phase lower the total mixture chemical energy from the current total mixture energy that we have in our current equilibrium state.

The Current Equilibrium State is (probably) Stable

no - current equilibrium state is the correct state (Maybe)

The Current Equilibrium State is UNSTABLE (for sure)

yes: -⁽¹⁾ a new equilibrium state with one more phase from our current state EXISTS and will lead to a lower total system energy. (Guaranteed)

(2) identify the v nature (composition) of the new phase.

Level of Difficulty:

- Assuming a reasonable guess of the new phase composition (\hat{u}_i) (\hat{u}_i^H, \hat{u}_i^L) (guesses)

→ Easy to Challenging (Easier than a Flash Calculation)

First State: Single Phase

$$z, p, T \Rightarrow (Z \sigma p) \Rightarrow (f_i \mu_i) \Rightarrow \mu_t = \sum z_i \mu_i$$

Test Phase is introduced in an ϵ amount

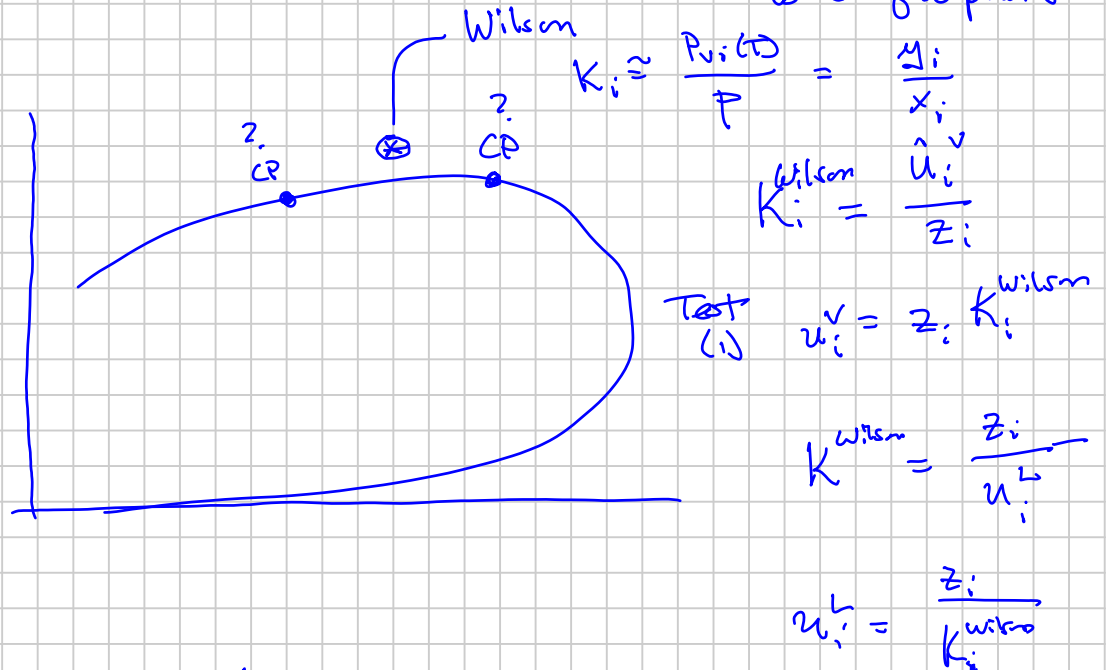
$$\mu_t' = (1-\epsilon) \sum z_i \mu_i(z_i) + \epsilon \sum u_i \cdot \mu_i(u_i)$$

Find u_i where $\mu_t' < \mu_t$
and where

$$\Rightarrow \mu_i(z_i) = \mu_i(u_i) + \frac{C}{\text{same final } i}$$

$C > 0$: $\mu_t' > \mu_t$ STABLE currently as single phase

$C \leq 0$: $\mu_t' < \mu_t$ UNSTABLE currently as single phase

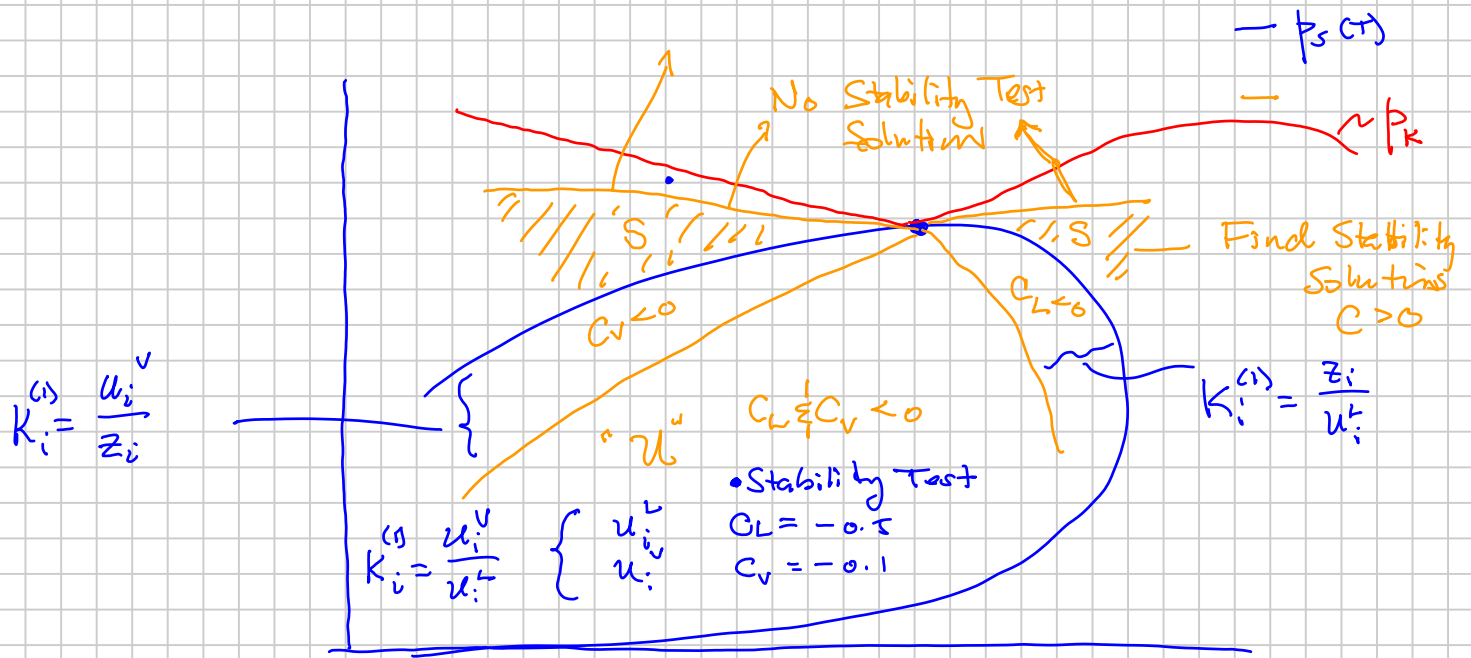


Test 1 : $C_V \quad u_i^V$

Test 2 : $C_L \quad u_i^L$

C_v and/or $C_L < 0 \Rightarrow$ UNSTABLE

Both C_v & $C_L > 0 \Rightarrow$ STABLE



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