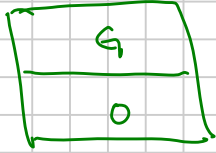


Two Phase Equilibrium

P, T



If in equilibrium

\Rightarrow G is saturated at (P, T)

$$P = P_G(T)$$

\rightarrow O is saturated at (P, T)

$$P = P_O(T)$$

$$\text{Initial } \rho_0 = V_0 \cdot \rho_{oi} / M_{oi}$$

HCPV₀

$$M_0 = \sum x_i M_i / \sum x_i$$

$$\rho_0 = \frac{\rho_0 + \rho_g R_s}{B_0} \quad \text{Table 6.7}$$

Job

Exam #4 P1 Data

use Job = 1 / spec. volume

$$= \frac{m_{ob}}{V_{ob}} = \rho_{Job} \rightarrow \rho_{oi} = \frac{m_{oi}}{V_{oi}}$$

@ 1270 @ 3015

$$\rho_{oi} = \rho_{Job} \cdot \left(\frac{V_t}{V_{ob}} \right)^{CCE}$$

$$\frac{m_0}{V_{ob}} \cdot \frac{V_{ob}}{V_t @ P_i}$$

Theoretical AOFD

- ① $P_{wf} = 0$
- ② $\Delta P_{+inlet} = 0$

: $P_{wf} = 0$

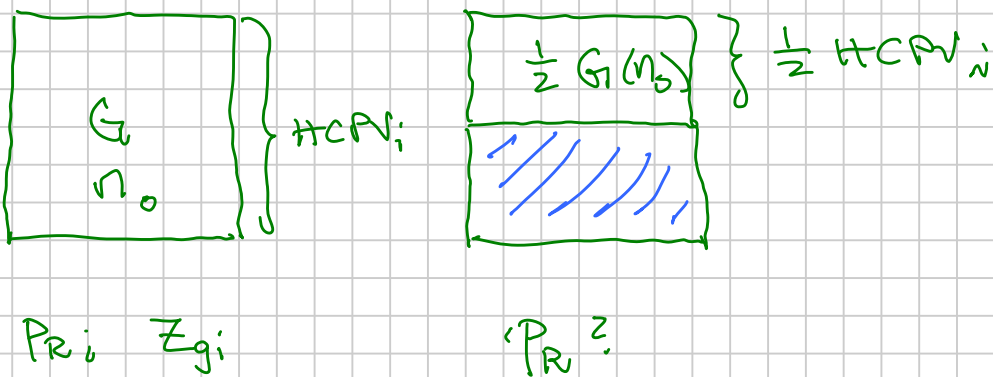
Wellhead Deliverability Curve

True AOFD : $q_g =$

$$B_{wh} q_g^2 + A_{wh} q_g - (P_c^2 - P_t^2) = 0$$

$$P_t = 0 \text{ or } P_{tmin}$$

2013: Prob. 1-3

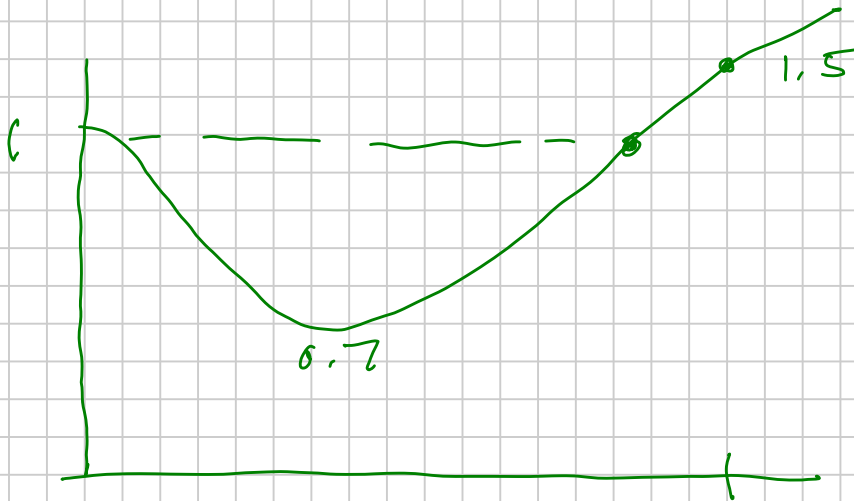


$$P_i V_i = n_i RT Z_i; \quad P_R \left(\frac{1}{2} V_i \right) = \frac{1}{2} n_i RT Z_R$$

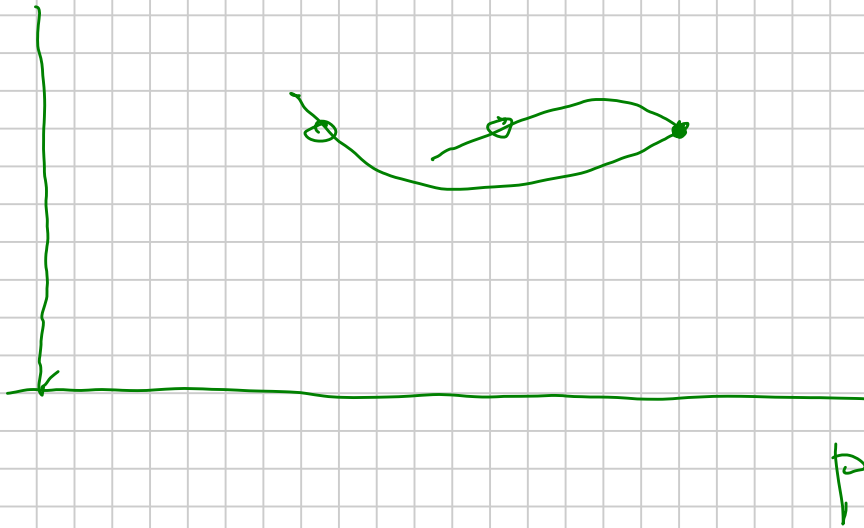
$$RT = \frac{P_i V_i}{n_i Z_i} = \frac{P_R \frac{1}{2} V_i}{\frac{1}{2} n_i Z_R}$$

$$\frac{P_i}{Z_i} = \frac{P_R}{Z_R}$$

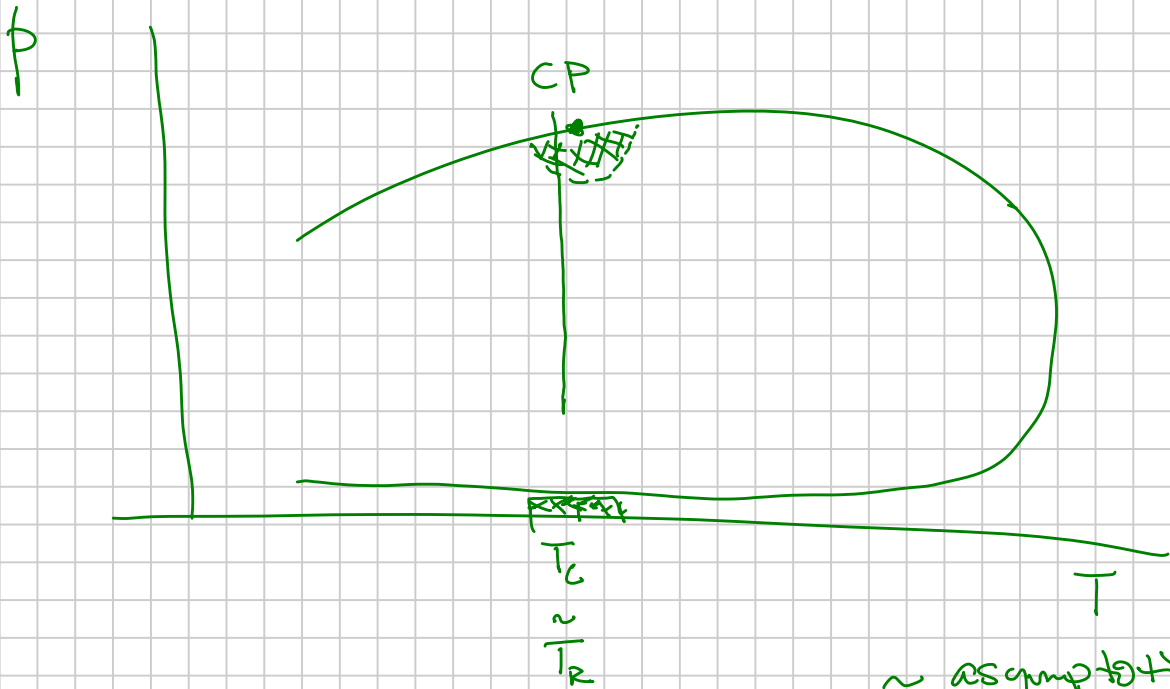
Very Large Ag.
→
Infinite Size Ag.



$\frac{P}{Z}$

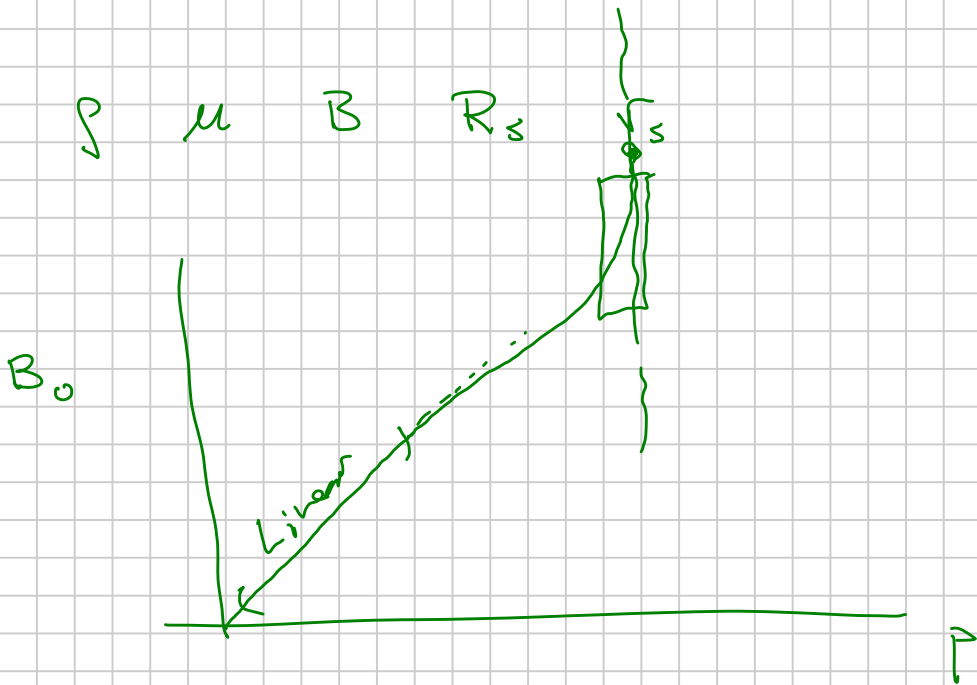


"Near Critical"



~ asymptotic
highly non-linear

(Two-Phase Properties) have "large" changes
with small pressure changes



2016 ~ 24d

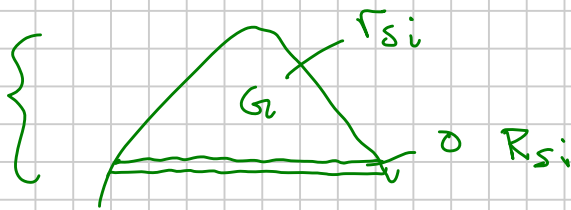
$$P_g = \frac{P M_g}{R T Z_g}$$

Calc ✓

① ⇒ Back out Z_g
~~0.83~~ 0.935

② Calc M_g
 ⇒ T_{pc} P_{pc}
 ⇒ SK
 ⇒ ~~0.83~~ 0.88

2009 2h



$$R_t (V_g, V_o, r_{si}, r_{so})$$

Total GOR

$$\boxed{(Z_{C10})_t}$$

$$\sim \frac{Z_{C7} + 510}{C_{C7}}$$

$$T_R > T_C$$

$$P_d @ T_R$$

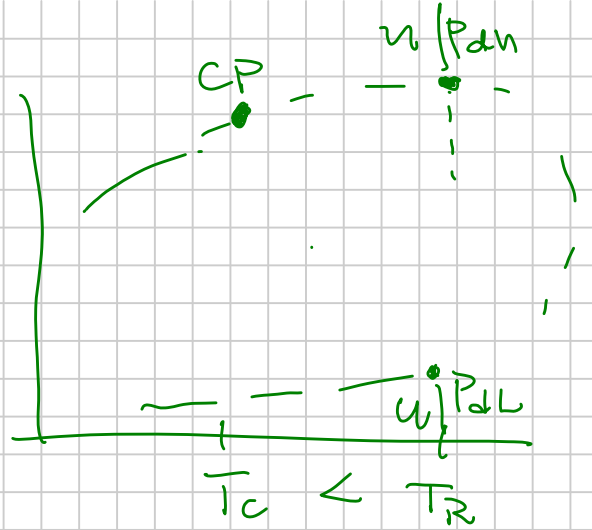
$$R_G : Z_{m+} \approx 15 \text{ mol-}\%$$

$$T_R < T_C$$

$$P_b @ T_R$$

$$R_D : \underbrace{\approx 15 \text{ mol-}\%}$$

RGC: $(y_i) = (z_i)$



$P > P_{du}$: Under-sat. G.C.

$P < P_{du}$: " "

Gas MB w/ Aquifer

B_{gd} :

G.C or Wet Gas
 B_{gdi}

When is correct to use:

①

②

$n_{gR} \neq n_g$
 $n_{gR} = n_g + n_o$
 B_{gd}
Gas Cond
Wet Gas

vs " B_g "

B_{gd}

$B_{gd} = \frac{P_{sc} T_R z_g}{P}$

Dry Gas

$n_{gR} = n_g$
 $n_o = 0$

i.e. IF surface condensate is produced

i.e. IF surface condensate is NOT produced



$$V_{ro} = \frac{V_o}{V_d} \quad @ p = p_d \quad \text{from } \underline{BOPUT}$$

$\left. \begin{array}{l} - \rho_{oi} \\ - \rho_{oi} \\ B_o \quad B_{gd} \\ R_s \quad r_s \end{array} \right\} (\varphi)$

Basis Unit $\underline{V_{og,i} = 1 \text{ Sm}^3}$

$$V_o =$$

$$V_d = V_{gd} @ p_d = V_{gg} \cdot B_{gd,d}$$

$$V_{gg} = \frac{V_{og,i}}{r_{sd}}$$

$$\boxed{V_d = V_{og} \cdot \frac{1}{r_{sd}} \cdot B_{gd,d}} = \frac{B_{gd,d}}{r_{sd}}$$

$$V_o = V_{oo} \cdot B_o = \left(1 - \left(\frac{1}{r_{si}} - \frac{R_s}{B_o} V_o \right) r_s \right)$$

$$\Rightarrow V_o$$

$$V_{\bar{o}o} = V_{\bar{o}g,i} - V_{\bar{o}g}$$

initial
remaining
surface oil
in gas

$$V_{\bar{o}g} = \underbrace{V_g / B_{gd}}_{V_{\bar{g}g}} \cdot r_s$$

$$V_{\bar{o}g} = V_{\bar{g}g} \cdot r_s = \left(\frac{1}{r_{s,i}} - \frac{R_s}{B_0} V_0 \right) r_s$$

$$V_{\bar{g}g} = V_{\bar{g}g,i} - V_{\bar{g}o} \quad \text{M.B.}$$

$$= \frac{V_{\bar{o}g,i}}{r_{s,i}} - \underbrace{\left(\frac{V_0}{B_0} \right)}_{V_{\bar{o}o}} R_s$$

$$= \frac{1}{r_{s,i}} - V_0 \left(R_s / B_0 \right)$$

$$V_0 = V_{\bar{o}o} \cdot B_0 = \left(1 - \left(\frac{1}{r_{s,i}} - \frac{R_s}{B_0} V_0 \right) r_s \right)$$

$$\Rightarrow V_0$$

$$V_0 = 1 - \frac{r_s}{r_{s,i}} + \frac{R_s}{B_0} r_s V_0$$

$$V_0 \left(1 - \frac{R_s}{B_0} r_s \right) = 1 - \frac{r_s}{r_{s,i}}$$

$$V_0 = \frac{1 - r_s / r_{s,i}}{1 - \frac{R_s}{B_0} r_s}$$

$$V_{r0} = \frac{V_0}{V_d} = \left[\frac{1 - r_s/r_{si}}{1 - \frac{R_s}{B_0} r_s} \right] \cdot r_{si}$$

$$\frac{B_{gd,d}}{r_{si}}$$

$$V_{r0} = \frac{(r_{si} - r_s)}{\left(1 - \frac{R_s}{B_0} r_s\right) B_{gd,d}}$$

Mat. Bal.

on

$$V_g^-$$

$$V_0^-$$

$$=$$

$$=$$

$$V_{fg}^- + V_{g0}^-$$

$$V_{og}^- + V_{o0}^-$$