

	GOR →					
	Oil	Volatile	(Near Critical)	Rich	Lean	Dry
	Black					
CCE	✓ (Blind Cell)	✓	✓	✓	✓	✓
	Windowed Cell					
SEP	✓	✓	✓	✓	$GOR \geq 15000 scf/STB$ x	$3,000 \text{ sm}^3/\text{km}^3$ x
DLE						
CVD						

✓ All sample types (BHS, "MDT", SEP)

DLE test ~ SEP test procedurally, except:

- $T_{spk} = T_R$
- 6-8 stages
- Final "residual" oil @ 1 atm, cooled to 60°F is NOT an oil we sell!

$$h(F_v) = \sum_{i=1}^N \left( \frac{z_i}{c_i + F_v} \right) = 0$$

N-1 solutions

Right solution:  $F_{\min} < F_v < F_{\max}$

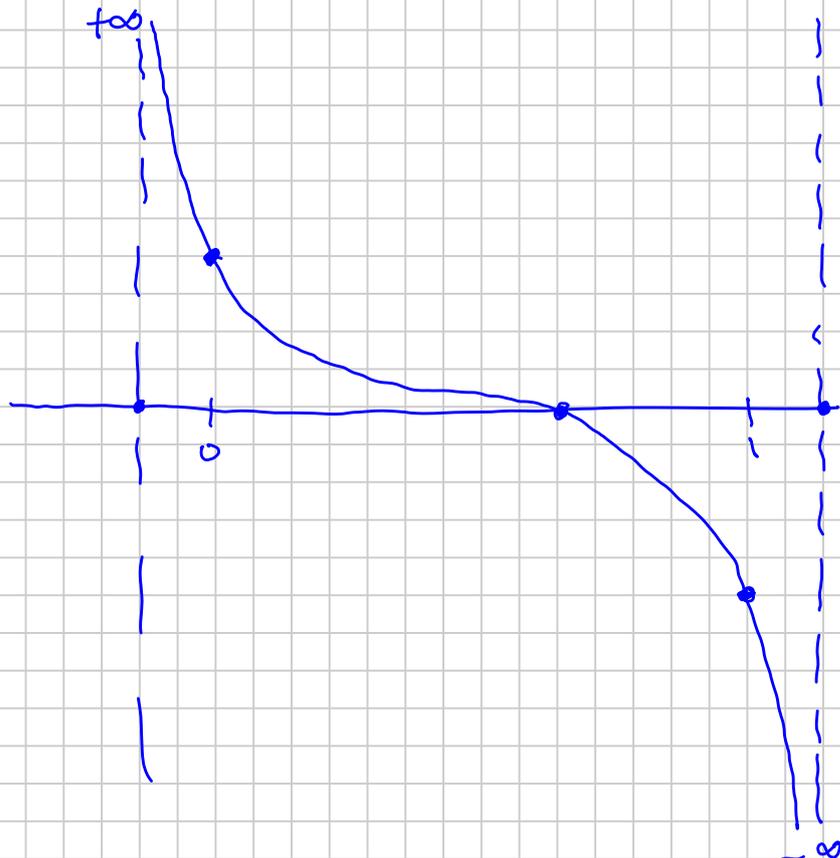
$$F_{\min} = \frac{1}{1 - K_{\max}} < 0$$

$$F_{\max} = \frac{1}{1 - K_{\min}} > 1$$

NR: 
$$F_v^{n+1} = F_v^n - \frac{h(F_v^n)}{\frac{dh}{dF_v}(F_v^n)}$$

$n = \text{iteration}$

Bisection fallback



Solve 
$$\frac{d^2 h}{dF_v^2} = 0$$
  
to get  
a better  
initial  
guess

Flash @ STC

$$\frac{n_g}{n_g + n_o} = F_v \rightarrow \text{GOR} = \frac{V_g}{V_o}$$

$$V_g = n_g \cdot \left( \frac{RT_{sc}}{p_{sc}} \right)$$

23.68  $\text{Sm}^3 / \text{kg-mole}$

$$V_o = n_o \cdot \frac{M_o}{\rho_o}$$

Let  $n = 1$       $n_g = F_v \cdot 1$       $n_o = (1 - F_v) \cdot 1$

Flash @ STC:

$$\text{GOR} = \frac{F_v \cdot 23.68}{(1 - F_v) \left( \frac{M}{\rho} \right)_o}$$

$F_v$   
 $y_{gi}$       $x_{oi}$

✓  $x_{oi}$

$$M_o = \frac{\sum_{oi} x_{oi} M_i}{\sum_{oi} x_{oi}} = \frac{(\sum x_{oi} M_i) (1 - F_v)}{(\sum x_{oi}) (1 - F_v)}$$

$$\rho_o = \frac{m_o}{V_o} = \frac{\sum_{oi} x_{oi} M_i}{\sum_{oi} \frac{x_{oi} M_i}{\rho_i}} = \frac{\sum (\sum x_{oi} M_i) (1 - F_v)}{\sum_{oi} \frac{x_{oi} M_i}{\rho_i} (1 - F_v)}$$

$\rho_o$

$\rho_{API}$

ST Liquid density  
App. A

$$H = \frac{\sum y_i H_i}{\sum y_i}$$

DLE: Only for OHS (i.e.  $p_s$ , a bubblepoint)

Designed to get phase & volumetric properties

at reservoir conditions ( $T_R$ ;  $p_R = p_b \rightarrow 10 \text{ bar}$   $\downarrow$   $1 \text{ atm}$ )

$p = p_b$

$$\left. \begin{matrix} p_0 & M_0 & V_0 & \text{Gas Released from Solution} \end{matrix} \right\} = R_{sb} - R_s(p)$$

$$p_b \rightarrow p$$

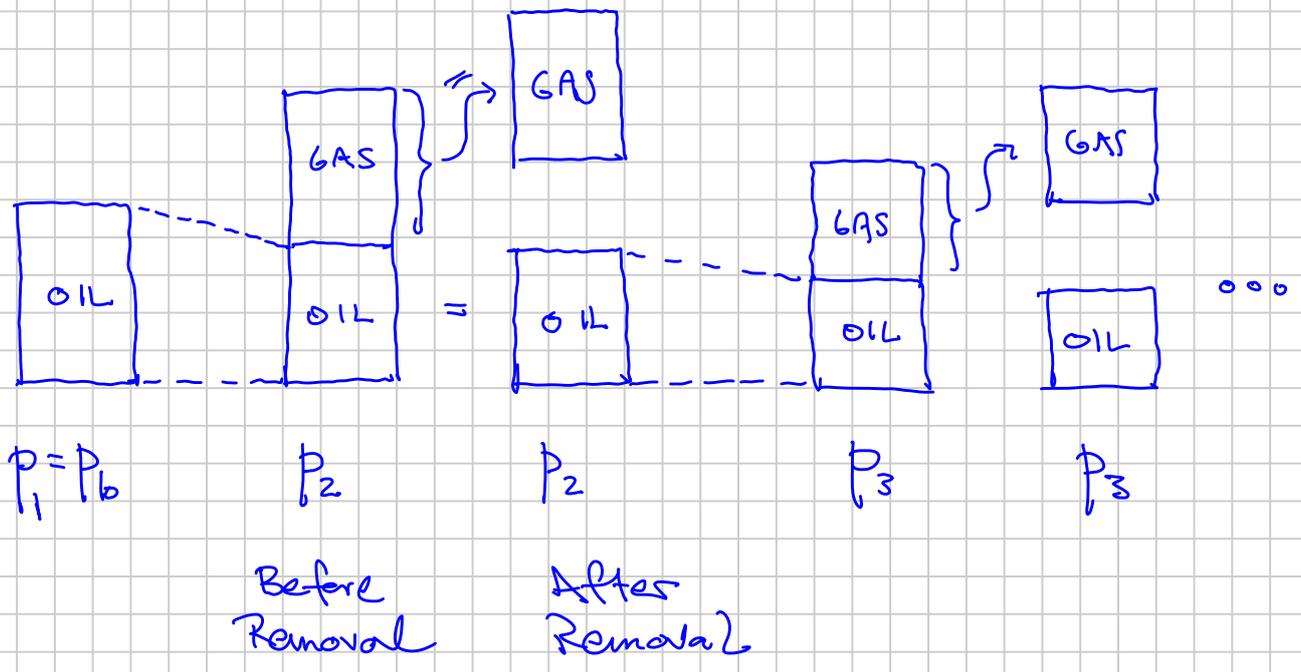
Strongly related

by Lee, Gonzalez, Calc.

$p < p_b$

$$p_g^* (Z_g) \quad \gamma_g^* (M_g) \quad M_g (p_g, T) \quad y_i (\pm \text{ for } C_{st})$$

$$p_g = \frac{p M_g}{RT Z_g}$$



Does the DLE process mimic the actual depletion process in a reservoir?

No

Does it matter?

No, or good enough (95%)

What is reported in DLE test

Stage	P	$B_{od} = \frac{V_o(P)}{V_{o\text{residual}}}$ Shrinkage	Calc	DLE test #1	DLE test #2
			$\rho_o$	$\Delta R_{sd}$	$M_o$
1	$P_b$			0	
2	⋮				
3	⋮				
4	⋮				
5	⋮				
6	⋮				
N-1	~10 bar				
N	1 atm				

$$\Delta R_{sd} = \frac{\Delta V_{g\text{ removed}, k}}{V_{o\text{residual}}}$$

$$R_{sd} = R_{sd,b} = \sum_k \Delta R_{sd}$$

Correct Cum. Released

left in Solution

$$\overline{(\sum \Delta R_{sd})} = R_{sd,b}$$

Total Released Gas = Initial Solution Gas } "R<sub>sd,b</sub>"

"R" GOR

\* At 1 atm, 60°F