

# SURFACE SEPARATION PROCESSING

Note Title

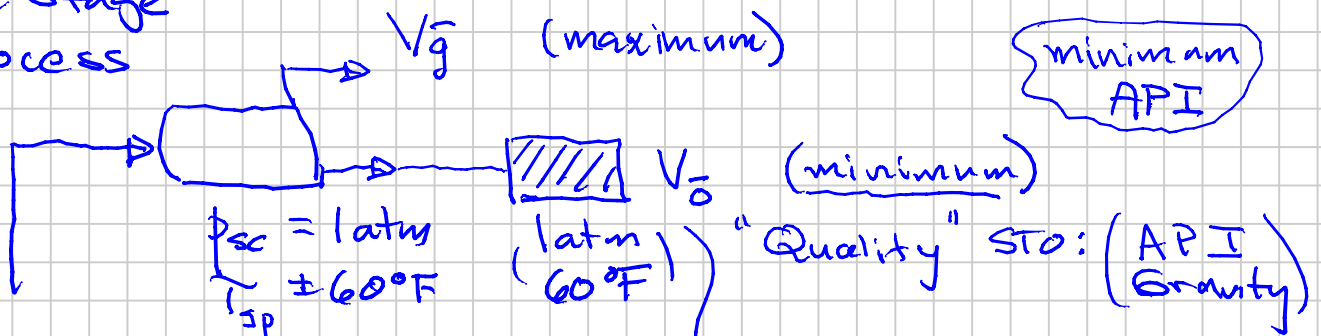
2013-09-20

Maximize the resulting Stock Tank Oil Volume from a produced stream (well, manifold, pipeline)

Reason: Any component mole in STO has more value than that component mole being sold as part of the gas.

$\{C_3 - C_7\}$  ↑ Subs Gas (low \$)  
STO (high \$)

Single Stage Process



Lowest STO Density:

$$\sim 650 \text{ kg/m}^3$$

$$\gamma_o = 0.65$$

$$\gamma_{API} = \frac{141.5}{0.65} - 131.5$$

$$= 86 \text{ }^\circ\text{API (Upper Limit)}$$

60-70

$\rho_o \Rightarrow \gamma_o = \frac{\rho_o}{\rho_w}$   
Liquid Specific Gravity  
Relative Density

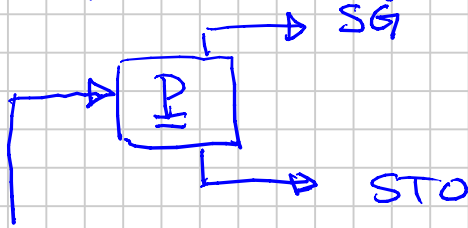
$$\gamma_{API} = \frac{141.5}{\gamma_o} - 131.5$$

STOs:

10 (\$/STB →) 70

i-Butane  $i-C_4$

$$n_{iC_4} = 1234 \text{ kg-moles/D}$$



35.31 scf/cm<sup>3</sup> gas  
6.28 STB/cm<sup>3</sup> STO

Prices:  
\$2-10 / Mscf    \$3.50 / Mscf  
\$100 / STB

$$n \rightarrow V_g = 23.68 \frac{\text{cm}^3}{\text{kg-mole}} \times n \quad \text{cm}^3 \text{ SG}$$

$$n \rightarrow V_o = n \times M_{iC_4} \frac{\text{kg}}{\text{kg-mole}} \times \frac{1}{(\rho_{iC_4})_{\text{surface liquid @ STC}}} \quad \text{cm}^3 \text{ STO}$$

App. A  
560.7 kg/m<sup>3</sup>

$$\text{Value as SG} : 1234 \times 23.68 \times 35.31 \times \frac{1}{1000} \times 3.50 = \$3610$$

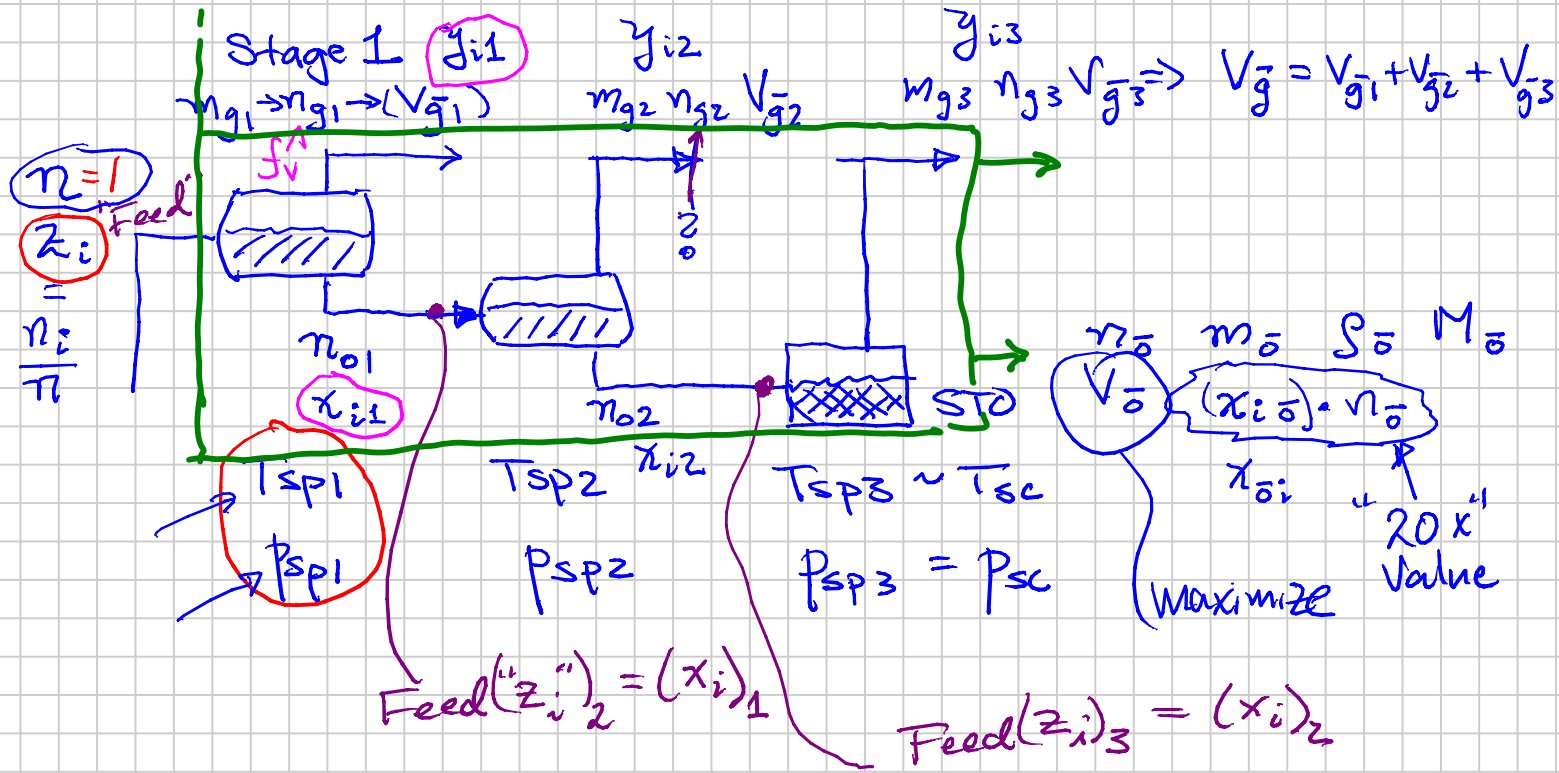
~~kg-moles~~     $\frac{\text{cm}^3}{\text{kg-mole}}$      $\frac{\text{scf}}{\text{cm}^3}$      $\frac{\text{Mscf}}{\text{scf}}$      $\frac{\text{USD}}{\text{Mscf}}$

$$\text{Value of STO} : 1234 \times 58.12 \times \frac{1}{560.7} \times 6.28 \times 100 = \$80,300$$

~~kg-moles~~     $\frac{\text{kg}}{\text{kg-mole}}$      $\frac{\text{m}^3}{\text{kg}}$      $\frac{\text{bbl}}{\text{m}^3}$      $\frac{\$}{\text{bbl}}$

22x

# Traditional Multi-Stage Separator Process



## Rachford-Rice (Muskat-McDowell) : FLASH Calculation

$$z_i(\phi, T) \Rightarrow K_i$$

$$f_v = \frac{n_g}{n} \quad \begin{matrix} y_{i_v} \\ x_{i_v} \end{matrix}$$

$$n_{g2} = n_{o1} \times (f_{v2})$$

Feed moles into Stage 2

$$n_{g3} = n_{o2} \times (f_{v3})$$

$$n_{g1} = f_{v1}$$

$$n_{g2} = (1 - f_{v1}) \cdot (f_{v2}) =$$

$$n_{g3} = (1 - f_{v1})(1 - f_{v2})(f_{v3})$$

$$n_{o1} = (1 - f_{v1})$$

$$n_{o2} = (1 - f_{v1})(1 - f_{v2})$$

$$\rightarrow n_{o3} = (1 - f_{v1})(1 - f_{v2})(1 - f_{v3})$$

Assuming  $\eta=1$

Book-keeping of moles

# Component "STD" Recovery Factor $RF_{\sigma_i}$

$$RF_{\sigma_i} = \frac{n_{\sigma_i}}{n_i} = \frac{n_{\sigma} x_{i3}}{n_i} \%$$

