

**EXAM IN COURSE
TPG4145 RESERVOIR FLUIDS**

Monday December 17, 2007

Time: 0900 – 1300

Permitted aids:

C:
ONLY (1) SPE *Phase Behavior* monograph volume 20 in original book form; handwritten notes written within the original book allowed. (2) Project Solution, up to maximum of six (6) single sided pages.

Problem 1: Calculate all missing numbers in Table 1. Write answers within Table 1.

TABLE 1 – Problems 1&2 – Gas-Oil Reservoir.

Component	Molecular Weight M_i	Liquid Specific Gravity
C1	16.04	
N-C5	72.15	0.6375
N-C10	142.28	0.7329

$\rho_{LSC} = C_{SF} = 0.6375 \cdot 1000 \text{ kg/m}^3 = 637.5 \text{ kg/m}^3$
 $\bar{M}_g = \frac{\sum y_i \cdot M_i}{\sum y_i}$

Two Phases at Temperature = 100 C, Pressure = 100 bar:

K

Molar Amounts: z_i x_i y_i Mole Fractions

Component	Overall	Liquid	Vapor	K-Value
C1	0.5	0.34291	0.94748	2.763
N-C5	0.20000	0.25350	0.04759	0.1877
N-C10	0.3	0.40359	0.00493	0.01222
Sum Mol. Frac	1.0	1.0	1.0	
Moles: gmol	1.0000	0.74018	0.25982	
Mol. Weight: g/gmol	65.137	81.216	19.286	
Z-Factor:		0.4645	0.9261	
Density (g/cc):		0.5638	0.06715	

$$n \cdot z_i = n_v \cdot y_i + (n - n_v) x_i$$

$$F_v \equiv n_v / n$$

$$\Rightarrow z_i = F_v \cdot y_i + (1 - F_v) x_i \quad \leftarrow$$

$$n-C_5: z_i, y_i, x_i$$

⇒ Solve for F_v

Because
 $n=1$

$$F_v = \frac{z_{C5} - x_{C5}}{y_{C5} - x_{C5}} = 0.25982 = \eta_v$$

$$F_L = 1 - F_v = 0.74018 = \eta_L$$

$$K_i = \frac{y_i}{x_i}$$

Ca. 4:

$$\rho = \frac{pM}{RTz}$$

p [bar]

M [kg/kmol]

T [K]

ρ [kg/m³]

$$T = 100^\circ\text{C} + 273 \\ = 373 \text{ K}$$

$$R = 0.08314 \\ \text{App. A}$$

$$z_g = 0.9261$$

$$\Rightarrow \rho_g = 67.15 \text{ kg/m}^3 = 0.06715 \text{ g/cm}^3 \\ \text{g/cc}$$

$$z_o = 0.4645$$

$$M_o = 81.2$$

$$\Rightarrow \rho_o = 563.8 \text{ kg/m}^3 = 0.5638 \text{ g/cc}$$

Problem 2: Using results from Problem 1 and Table 2, answer the following:

- a. Pressure at 900 m below sea level.
- b. Pressure at 1200 m below sea level (WOC).
- c. Initial surface gas in Reservoir Gas Zone, IGIP(RG).
- d. Initial surface oil (“condensate”) in Reservoir Gas Zone, IOIP(RG).
- e. Initial surface gas in Reservoir Oil Zone, IGIP(RO).
- f. Initial surface oil in Reservoir Oil Zone, IOIP(RO).

Assuming an idealized surface process, where “surface gas” is C1 and “surface oil” is (n-C5 + n-C10), calculate and compare with values in Table 2:

- g. Initial solution OGR (r_s) in Reservoir Gas Zone.
- h. Initial gas formation volume factor (B_{gd}) in Reservoir Gas Zone.

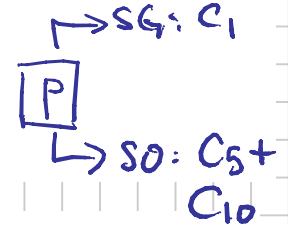
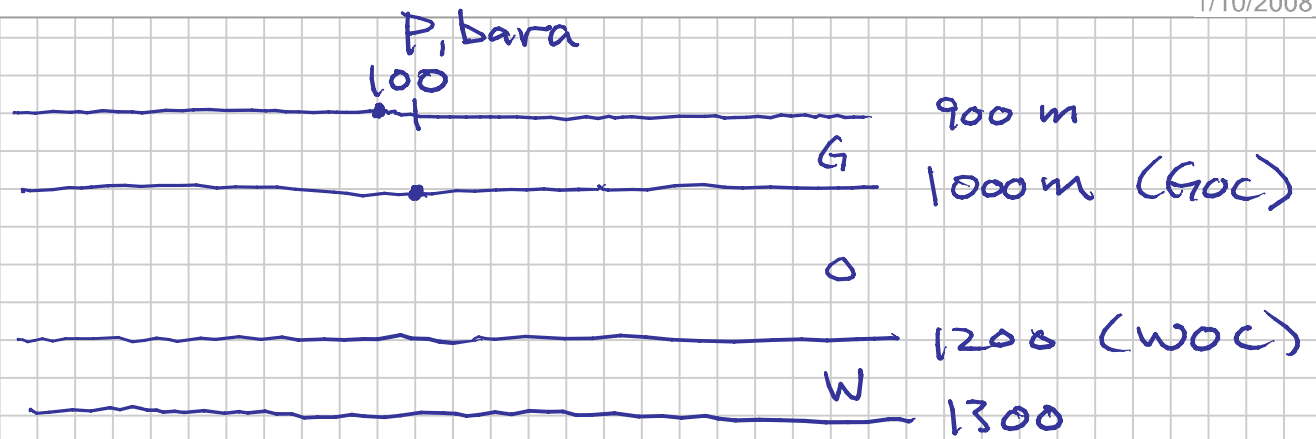


TABLE 2 – Problems 1&2 – Gas-Oil Reservoir.

Initial Reservoir Pressure (bara) at Gas-Oil Contact	100
Initial Reservoir Temperature (°C)	100
Gas-Oil Contact (m below sea level)	1000
Water-Oil Contact (m below sea level)	1200
Top Gas Reservoir Zone (m below sea level)	900
Bottom Water Zone (m below sea level)	1300
Hydrocarbon Pore Volume, Reservoir Gas (m ³)	1E8
Hydrocarbon Pore Volume, Reservoir Oil (m ³)	1E8
Initial solution OGR (r_s) in Reservoir Gas Zone (Sm ³ /Sm ³)	3.6173E-5
Initial solution GOR (R_s) in Reservoir Oil Zone (Sm ³ /Sm ³)	94.3
Initial gas formation volume factor (B_{gd}) in Reservoir Gas Zone (m ³ /Sm ³)	0.01222
Initial oil formation volume factor (B_o) in Reservoir Oil Zone (m ³ /Sm ³)	1.434

} Real Process



a. Gas Density:

$$P_{900} = P_{1000} - \rho_g \cdot g \cdot (100)$$

$$= 100 - \underbrace{67 (9.8) (100)}_{\text{Pa}} \cdot (10^{-5} \frac{\text{bar}}{\text{Pa}})$$

$$P_{900m} = \underline{99.34 \text{ bara}}$$

b. Oil Density

$$P_{1200} = P_{1000} + \rho_o \cdot g \cdot (200) (10^{-5})$$

$$= 100 + 564 (9.8) (200) (10^{-5})$$

$$\underline{P_{1200} = 111 \text{ bara}}$$

$$c. \text{IGIP (RG)} = \frac{HCPV(RG)}{B_{gdi}} = \frac{10^8}{0.01222} = \underline{8.19 \cdot 10^9 \text{ Sm}^3}$$

$$d. \text{LOIP (RG)} = \text{IGIP (RG)} \cdot r_{si} = \underline{2.96 \cdot 10^5 \text{ Sm}^3}$$

$$e. \text{IGIP (RO)} = \text{LOIP (RO)} \cdot R_{si} = \underline{6.576 \cdot 10^9 \text{ Sm}^3}$$

$$f. \text{IOP}(RO) = \frac{HCPV(RO)}{B_{oi}} = \underline{\underline{6.974 \cdot 10^7 \text{ Sm}^3}}$$

g.

$n_g = n_{ci} = y_{ci} = 0.94748 \text{ kmol}$
 $n_o = n_{cs} + n_{co} = y_{cs} + y_{co} = \underline{\underline{0.05252 \text{ kmol}}}$

$$V_g = \frac{RT_{sc}}{P_{sc}} \cdot n_g = 23.64$$

$$M_o = \frac{y_{cs} M_{cs} + y_{co} M_{co}}{y_{cs} + y_{co}} = 78.57 \text{ kg/kmol}$$

$$V_o = \frac{M_o}{\rho_o} = n_o \cdot \frac{M_o}{\rho_o}$$

$$\rho_o \approx \frac{y_{cs} M_{cs} + y_{co} M_{co}}{\frac{y_{cs} M_{cs}}{\rho_{cs}} + \frac{y_{co} M_{co}}{\rho_{co}}} = 652 \text{ kg/m}^3$$

Ideal Volume Mixing

$$r_{si} = \frac{V_o}{V_g} = \frac{0.05252 \left(\frac{78.57}{652} \right)}{23.64 (0.94748)} = 2.83 \cdot 10^{-4} \text{ Sm}^3/\text{Sm}^3$$

vs

$$3.61 \cdot 10^{-4} \text{ Sm}^3/\text{Sm}^3$$

$$h) B_{gd} = \frac{P_{sc}}{T_{sc}} \cdot \frac{ZT}{P} \cdot \frac{1}{y_g}$$

$$Z = 0.9261$$

$$T = 373 \text{ K}$$

$$p = 100 \text{ bar}$$

$$y_g = 0.94748$$

$$\underline{\underline{B_{gd} \approx 0.00991 \text{ m}^3/\text{Sm}^3}}$$

Problem 3: Based on information in Table 3, calculate the following at the end of plateau for two minimum flowing tubing pressures, 100 and 500 psia: *10 yr*

- a. Minimum number of wells needed to produce Plateau Field Gas Rate.
- b. Gas recovery factor. $137 \cdot 10^6 \text{ scf/D}$
- c. Average reservoir pressure.
- d. Flowing tubing pressure.

TABLE 3 – Problem 3 – Dry-Gas Reservoir.

z = 1

S.L. Gas M.B.

Assume Ideal Gas Law and Straight-Line Gas Material Balance ($M=c_w=c_f=0$)

Initial Reservoir Pressure (psia)	1500
Initial Gas in Place (scf)	1E12
Plateau Field Gas Rate (MMscf/D = 10^6 scf/day)	137
Plateau Period (years)	<u>10</u>
Gas Static Column Gravity Term ($p_{\text{reservoir}}/p_{\text{surface}}$)	1.1
Wellhead Backpressure Deliverability Equation* Constant C	400
Wellhead Backpressure Deliverability Equation* Exponent n	0.8

* $q_g = C(p_c^2 - p_t^2)^n$ with p(psia), q_g (scf/D) | For a single well

$$P_c = \frac{P_R}{1.1} \Rightarrow P_R = 1.1 \cdot P_c$$

$$\frac{P_R}{z} = \frac{P_i}{z_i} \left(1 - \frac{G_p}{G}\right) \Rightarrow P_R = P_i \left(1 - RF_g\right)$$

\uparrow
 RF_g

b.

$$(RF_g)_p = \frac{q_{gF} \cdot t_p}{1GIP} = \frac{137 \cdot 10^6 \cdot 10 \cdot 365}{10^{12}} = 0.5 \quad (50\%)$$

Independent of P_{tmin}

$$c. (P_R)_p = 1500(1-0.5) \\ = \underline{750 \text{ psia}} \text{ independent of } P_{tmin}$$

$$d. P_t \text{ @ end plateau} = P_{tmin}$$

100 psia

500 psia

$$a. (N_w)_p = \frac{q_{gF}}{(q_{gw})_{P_t = P_{tmin} \text{ @ end plateau}}}$$

$$q_{gw} = C \cdot (P_c^2 - P_t^2)^n$$

$$P_{tmin} = 100 \text{ psia}$$

$$q_{gw} = 400 \left(\left(\frac{750}{1.1} \right)^2 - 100^2 \right)^{0.8} = 13.4 \cdot 10^6 \frac{\text{scf}}{\text{D}}$$

$$\Rightarrow (N_w)_{P_{tmin}=100} = \frac{137 \cdot 10^6}{13.4 \cdot 10^6} = 10.2$$

$\Rightarrow 11$ wells

$$P_{\text{min}} = 500 \text{ psia}$$

$$(q_w)_p = 7.38 \cdot 10^6 \text{ ccf/D}$$

$$N_w = 18.x \Rightarrow \underline{19 \text{ wells}}$$